

# SUPPLEMENTAL INFORMATION

## The Blood-Brain Barrier: An Engineering Perspective

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### Appendix 1: TEER - resistance of blood plasma

Blood plasma makes up 55 - 60% of the total volume of blood. It is about 90% water by volume and contains various ionic and proteins:

<b>Ion</b>	<b>Concentration (mM)</b>
Sodium	135 - 145
Potassium	3.7 - 5.1
Chloride	95 - 105
Calcium	2.1 - 3.7
Carbonate	23 - 31
Phosphate	0.7 - 1.4

<b>Protein</b>	<b>Concentration (mg mL<sup>-1</sup>)</b>
Albumin	35 - 50
IgG	5 - 7
other	10 - 15

The conductivity of blood plasma can be estimated from the molar conductivity using the Debye-Huckel-Onsager equation:

$$\Lambda = \Lambda^\circ - (A \Lambda^\circ + B) \sqrt{c} \quad (\text{A1.1})$$

The molar conductivity at infinite dilution ( $\Lambda^\circ$ ) for NaCl is 161 cm<sup>2</sup> Ω<sup>-1</sup> mol<sup>-1</sup> at 37 °C.<sup>1</sup> Taking  $A = 1489 \text{ cm}^{5/2} \Omega^{-1} \text{ mol}^{-1/2}$  and  $B = 6.83 \text{ cm}^{3/2} \text{ mol}^{-1/2}$  at 37 °C, the molar conductivity ( $\Lambda$ ) for a 140 mM NaCl solution is 130 cm<sup>2</sup> Ω<sup>-1</sup> mol<sup>-1</sup>.

The resistivity can then be calculated from:

$$\rho_{\text{pl}} = \frac{1}{\kappa} = \frac{1}{\Lambda c} \quad (\text{A1.2})$$

The resistivity for a 140 mM NaCl solution at 37 °C is 54.8 Ω cm, in good agreement with the experimentally measured resistance of blood plasma (54 - 62 Ω cm).<sup>2</sup>

The resistivity of whole blood depends on the fraction hematocrit:

$$\rho_{bl} = \frac{\rho_{pl}(1 + \xi h)}{1 - h} \quad (A1.3)$$

where  $\rho_{pl}$  is the resistivity of the blood plasma,  $h$  is the fraction hematocrit, and  $\xi$  is a form factor dependent on the shape of the red blood cells.<sup>3</sup>

## Appendix 2: 2D transport

The net flux of a solute  $J$  (mole  $s^{-1}$ ) across a barrier is the difference between the input and output fluxes:

$$J = \frac{dN}{dt} = k_{in}c_{in} - k_{out}c_{out} \quad (A2.1)$$

where  $N$  is the number of moles of solute in the output side,  $k_{in,2D}$  and  $k_{out,2D}$  are the first order rate constants ( $cm^3 s^{-1}$ ),  $c_{in}$  and  $c_{out}$  (mole  $cm^{-3}$ ) are the solute concentrations on the input and output sides, respectively.<sup>4-6</sup>

For diffusive transport it is seen that:<sup>4-6</sup>

$$J = \frac{dN}{dt} = -DA \frac{dc}{dx} \quad (A2.2)$$

where  $D$  is the diffusion coefficient ( $cm^2 s^{-1}$ ) and  $A$  is the area ( $cm^2$ ). The solute permeability is defined as the flux through unit area for unit concentration gradient:

$$P_{2D} = \frac{J}{A\Delta c} \quad (A2.3)$$

From Fick's first law the permeability coefficient can be related to the diffusion coefficient:

$$P_{2D} = \frac{D}{\Delta x} \quad (A2.4)$$

The flux can be written as:

$$J = \frac{dN}{dt} = -P_{2D}A\Delta c \quad (A2.5)$$

where  $\Delta c = c_{out} - c_{in}$ . Note that  $N = c_{out}(t)V$ , where  $V$  is the volume of the output side, and hence:

$$\frac{dc}{dt} = -\frac{P_{2D}A}{V}(c_{out}(t) - c_{in})J \quad (A2.6)$$

Rearranging:

$$\frac{dc}{c_{in} - c_{out}(t)} = \frac{P_{2D}A}{V} dt \quad (A2.7)$$

Integrating:

$$c_{\text{out}}(t) = c_{\text{in}} \left( 1 - \exp \left( -\frac{P_{2D}A}{V} t \right) \right) \quad (\text{A2.8})$$

$$\text{or } N(t) = V c_{\text{in}} \left( 1 - \exp \left( -\frac{P_{2D}A}{V} t \right) \right) \quad (\text{A2.9})$$

For short times:

$$1 - \exp \left( -\frac{P_{2D}A}{V} t \right) = \frac{P_{2D}A}{V} t \quad (\text{A2.10})$$

and hence:

$$c_{\text{out}}(t) = \frac{P_{2D}A}{V} c_{\text{in}} t \quad (\text{A2.11})$$

$$\text{or } N(t) = P A c_{\text{in}} t \quad (\text{A2.12})$$

### Appendix 3: resected vessel assay

We define  $N_{\text{bath}}$  as the number of moles of solute in the bath,  $N_{\text{cell}}$  as the number of moles of solute in the endothelium, and  $N_{\text{lum}}$  as the number of moles of solute in the lumen of the vessel. The concentration of solute in the bath is  $c_{\text{bath}} = N_{\text{bath}}/V_{\text{bath}}$  and in the lumen is  $c_{\text{lum}} = N_{\text{lum}}/V_{\text{lum}}$ . As long as  $V_{\text{bath}}$  and  $V_{\text{lum}} \gg V_{\text{cell}}$ , we can take show that:

$$\frac{dN_{\text{lum}}}{dt} = \frac{V_{\text{lum}} dc_{\text{lum}}}{dt} = k_{\text{in}} A c_{\text{bath}} - k_{\text{out}} A c_{\text{lum}} \quad (\text{A3.1})$$

Rearranging:

$$\frac{dc_{\text{lum}}}{k_{\text{in}} A c_{\text{bath}} - k_{\text{out}} A c_{\text{lum}}} = \frac{1}{V_{\text{lum}}} dt \quad (\text{A3.2})$$

Note that  $V_{\text{lum}}$ ,  $k_{\text{in}}$ ,  $k_{\text{out}}$ , and  $A$  are constants. We assume that  $V_{\text{bath}} \gg V_{\text{lum}}$ , and hence  $c_{\text{bath}}$  is approximately constant. Integrating equation (A3.2) and recognizing that  $c_{\text{lum}} = 0$  at  $t = 0$ , we obtain:

$$c_{\text{lum}}(t) = \frac{k_{\text{in}}}{k_{\text{out}}} \left( 1 - \exp \left( -\frac{k_{\text{out}} A}{V_{\text{lum}}} t \right) \right) c_{\text{bath}} \quad (\text{A3.3})$$

Substituting for  $k_{\text{in}}$  and  $k_{\text{out}}$ :

$$c_{\text{lum}}(t) = c_{\text{bath}} \left( 1 + \frac{k_{\text{pgp}}}{k_{\text{m}}} \right) \left( 1 - \exp \frac{t}{\frac{V_{\text{lum}}}{A k_{\text{m}}} \left( 2 + \frac{k_{\text{pgp}}}{k_{\text{m}}} \right)} \right) \quad (\text{A3.4})$$

At long times, the concentration in the lumen reaches a steady state value given by:

$$c_{\text{lum}}(\infty) = \frac{k_{\text{in}}}{k_{\text{out}}} c_{\text{bath}} = \left(1 + \frac{k_{\text{pgp}}}{k_{\text{m}}}\right) c_{\text{bath}} \quad (\text{A3.5})$$

Therefore, the time dependence of the concentration of solute in the lumen can be simplified as:

$$c_{\text{lum}}(t) = c_{\text{lum}}(\infty) \left(1 - \exp\left(-\frac{t}{\tau}\right)\right) \quad (\text{A3.6})$$

#### Appendix 4: in vivo transport

The net flux of a solute ( $J$ ) between the brain and plasma is the difference between the flux into and out of the brain, Where the flux in and out from one compartment to another may be described as the product of a first order rate constant,  $k_{\text{in},3\text{D}}$  and  $k_{\text{out},3\text{D}}$ , and its respective concentration,  $c_{\text{pl}}$  and  $c_{\text{br}}$ .

$$J = \frac{dQ_{\text{br}}}{dt} = k_{\text{in},3\text{D}} c_{\text{pl}} - k_{\text{out},3\text{D}} c_{\text{br}} \quad (\text{A4.1})$$

If we assume only a small amount of solute accumulates in the brain relative to the plasma ( $Q_{\text{br}}/V_{\text{br}} \ll c_{\text{pl}}$ ), then we can ignore the back flux ( $k_{\text{out},3\text{D}} c_{\text{br}} \approx 0$ ).<sup>7</sup>

$$\frac{dQ_{\text{br}}}{dt} \approx k_{\text{in},3\text{D}} c_{\text{pl}} \quad (\text{A4.2})$$

Integrating equation A4.2, assuming that the concentration of solute in plasma ( $c_{\text{pl}}$ ) is constant, we obtain

$$Q_{\text{br}} \approx k_{\text{in},3\text{D}} c_{\text{pl}} t \quad (\text{A4.3})$$

where  $t$  is the time of infusion, also known as the amount of time the brain is exposed to the drug. The net flux of solute into the brain can also be described by Fick's first law and related to the permeability coefficient ( $P_{3\text{D}}$ ):

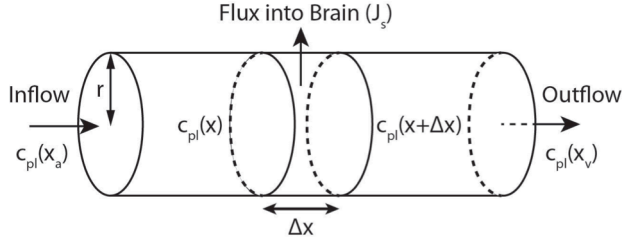
$$J = P_{3\text{D}} S (c_{\text{pl}} - c_{\text{br}}) \quad (\text{A4.4})$$

Assuming the concentration of solute in the brain ( $c_{\text{br}}$ ) is not significant over the duration of infusion ( $c_{\text{br}} \approx 0$ ):

$$J \approx P_{3\text{D}} S c_{\text{pl}} \quad (\text{A4.5})$$

where  $S$  is the normalized luminal surface area of vessels ( $\text{cm}^2 \text{ g}_{\text{br}}^{-1}$ ) in the brain. Consider the mass balance of solute entering a length of brain microvessel (Figure A4.1). The total amount of solute that enters through the arterial end ( $x_{\text{a}}$ ) is partitioned between diffusion out of a section of vessel with thickness  $\Delta x$ , and flow out of the venous end ( $x_{\text{v}}$ ). Assuming that the back flux is negligible, the inflow of total solute ( $\text{g}_{\text{s}} \text{ s}^{-1} \text{ g}_{\text{br}}^{-1}$ ) in plasma is equal to the sum of the flux into the brain parenchyma (equation A4) and the outflow of remaining solute in plasma ( $\text{g}_{\text{s}} \text{ s}^{-1} \text{ g}_{\text{br}}^{-1}$ ). Inflow and outflow can be described as the product of concentration ( $c_{\text{pl}}$ ) and flow rate ( $F$ ) into

and out of the vessel. The flux into the brain is related to the permeability coefficient and the surface area and concentration (equation A4.5).



**Figure A4.1. Illustration of solute mass balance.**

From mass balance:

$$Fc_{pl}(x) = P_{3D} 2\pi r \Delta x c_{pl}(x) + Fc_{pl}(x + dx) \quad (A4.6)$$

For small  $\Delta x$  ( $\text{cm g}_{br}^{-1}$ ):

$$-F \frac{c_{pl}(x + dx) - c_{pl}(x)}{\Delta x} \approx -F \frac{dc_{pl}(x)}{dx} = P_{3D} 2\pi r c_{pl}(x) \quad (A4.7)$$

Rearranging and integrating along the vessel from the arterial end ( $x_a$ ) to the venous end ( $x_v$ ) we obtain:

$$c_{pl}(x_v) = c_{pl}(x_a) \exp\left(-\frac{P_{3D}S}{F}\right) \quad (A4.8)$$

where  $\int_{x_a}^{x_v} 2\pi r dx = S$

The amount of solute that enters the brain ( $Q_{br}$ ) over an infusion time of  $t$  with a given flow rate  $F$  is:

$$Q_{br} = (c_{pl}(x_a) - c_{pl}(x_v)) Ft \quad (A4.9)$$

Substituting equation A4.8 into equation A4.9 yields:

$$\frac{Q_{br}}{t} = c_{pl}(x_a) \left[ 1 - \exp\left(-\frac{P_{3D}S}{F}\right) \right] F \quad (A4.10)$$

From equation A4.3, we see that:

$$k_{in,3D} \approx \frac{Q_{br} c_{pl}}{t_0} \quad (A4.11)$$

Substituting equation A4.10 into A4.11 we obtain the Crone-Renkin Equation,<sup>8,9</sup> which relates  $k_{in, 3D}$  to  $P_{3D}$ .

$$k_{in,3D} = F \left[ 1 - \exp \left( - \frac{P_{3D}S}{F} \right) \right] \quad (A4.12)$$

If  $P_{3D}S \gg F$ , then the exponential term can be linearized:

$$1 - \exp \left( - \frac{P_{3D}S}{F} \right) \approx \frac{P_{3D}S}{F} \quad (A4.13)$$

Combining equations A4.12 and A4.13, we obtain:

$$k_{in,3D} \approx P_{3D}S \quad (A4.14)$$

This equation is valid for short infusion periods over which back flux is negligible. Alternatively, equation A4.14 can be derived using equation A4.3 to approximate the net flux of solute into the brain:

$$J = \frac{Q_{br}}{t} \approx k_{in,3D}c_{pl} \quad (A4.15)$$

Combining equations A4.15 and A4.4 and simplifying yields equation A4.14.

## References

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