



Diagnosing Stagnant Gas Bubbles in a Polymer Electrolyte Membrane Water Electrolyser Using Acoustic Emission

Maximilian Maier¹, Quentin Meyer², Jude Majasan¹, Rhodri E. Owen^{1,3}, James B. Robinson^{1,3}, James Dodwell¹, Yunsong Wu¹, Luis Castanheira⁴, Gareth Hinds⁴, Paul R. Shearing^{1,3} and Dan J. L. Brett^{1,3*}

¹Electrochemical Innovation Lab, Department of Chemical Engineering, UCL, London, United Kingdom, ²School of Chemistry, UNSW, Sydney, NSW, Australia, ³The Faraday Institution, Quad One, Harwell Science and Innovation Campus, Didcot, United Kingdom, ⁴National Physical Laboratory, Teddington, United Kingdom

The use of acoustic emission as a low-cost, non-destructive, and *operando* diagnostic tool has been demonstrated for a range of electrochemical energy conversion and storage devices, including polymer electrolyte membrane water electrolysers (PEMWEs) and fuel cells. In this work, an abrupt change in acoustic regime is observed during operation of a PEMWE as the current density is increased from 0.5 to 1.0 A cm⁻². This regime change is marked by a sudden drop in the number of acoustic hits, while hit duration, amplitude, and energy increase significantly. It is found that the change in acoustic regime coincides with a significant extension of the stagnant bubble region in the flow channels of the PEMWE, observed with high-speed optical imaging. These results demonstrate that acoustic emission can be used effectively as an operando diagnostic tool to monitor bubble formation (two-phase flow conditions) in PEMWEs, facilitating rapid testing or prototyping, and contributing to operational safety.

Keywords: acoustic emission, polymer electrolyte membrane water electrolyser, operando diagnostics, mass transport, flow channels, flow regime, gas bubble

INTRODUCTION

Polymer electrolyte membrane water electrolysers (PEMWEs) represent one of the most promising approaches to the production of "green" hydrogen and large-scale energy grid stabilization. The technology is likely to replace the widely commercially used alkaline electrolysis due to advantages including lower voltage at equal current density, lower gas crossover, compact build, and the possibility of high-pressure operation (Carmo et al., 2013). While currently more expensive than the alternative alkaline technology, the capital cost of a typical PEMWE system is dropping (Saba et al., 2018) and plants rated up to 6 MW are in operation (Buttler and Spliethoff, 2018).

Water flooding has been shown to be a major mass transport limitation occurring in polymer electrolyte membrane fuel cells (PEMFCs) at high current densities, particularly at high humidity when water condenses at the cathode forming droplets which coalesce. This leads to water blocking the flow channels and occupying the gas diffusion layer (GDL), causing a consequent increase in pressure drop and decrease in performance (Tüber et al., 2003; Spernjak et al., 2007; Hussaini and Wang, 2009). Similarly to water accumulation in a PEMFC, which eventually leads to flooding, product gas can accumulate in polymer PEMWEs leading to bubbles blocking the flow channels. This occurs if the gas production from the catalyst sites exceeds the

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*Correspondence:

Dan J. L. Brett d.brett@ucl.ac.uk

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1



gas removal capacity of the flow channels, which is mainly determined by the cross-sectional area and the flow rate of water through the channels. The effects of bubble blockage on performance, pressure drop, and life-time of a PEMWE have not yet been investigated, but it is expected that prolonged bubble blockage results in local water starvation, causing a non-uniform current distribution over the active area and a decrease in performance (Sun et al., 2015).

Acoustic emission (AE) is a non-destructive, *operando* diagnostic tool traditionally used in civil engineering, e.g., for monitoring crack propagation in steel (Roberts and Talebzadeh, 2003) or the stability of bridges (Nair and Cai, 2010). It uses a piezoelectric sensor to detect mechanical perturbations emitted by an object and has been applied to a range of electrochemical energy storage devices. It has been used to monitor particle fracture and morphological changes in battery electrodes during charge and discharge (Ohzuku et al., 1997; Rhodes et al., 2010; Villevieille et al., 2010), has been found to be sensitive to Li-ion intercalation and formation of the solid electrolyte interphase (Kircheva et al., 2011; Kircheva et al., 2012) in Li ion batteries, and has also been applied to PEMFCs (Legros et al., 2009; Legros et al., 2010; Bethapudi et al., 2019).

Two-phase systems, such as the water-gas mixture in the flow channels of the PEMWE analyzed in this work, are also readily analyzed using AE. This includes the calculation of bubble size distribution (Pandit et al., 1992), recognition of different flow patterns by analyzing AE data with neural networks (Yen and Lu, 2002), and observing the formation and collapse of single bubbles (Husin et al., 2013). Hence, AE is a valuable alternative diagnostic tool to other techniques for the investigation of two-phase dynamics (Huguet et al., 2011; Maiyalagan and Saji, 2017; Dastafkan et al., 2020). In previous work, the authors demonstrated the ability of AE to detect changes in the number and size of bubbles passing through the flow channel of a PEMWE. This enabled the prediction of the change from bubbly to slug flow and showed that AE is a valuable *operando* tool for PEMWE diagnosis (Maier et al., 2019). Here, we demonstrate that AE signal changes dramatically when, rather than normal two-phase flow, stagnant bubbles are located within the vicinity of AE sensor. This feature can be used to detect and locate bubble "blockage" (channel dehydration) in PEMWEs, for *operando* monitoring or design optimization.

EXPERIMENTAL

Polymer Electrolyte Membrane Water Electrolyser Cell

The electrolyser used in this work (Figure 1) had a 9 cm² active area and consisted of transparent Perspex end-plates, parallel titanium flow-fields, a titanium sinter liquid-GDL on the anode side, a Toray H-060 carbon paper as the GDL on the cathode side, and a catalyst coated membrane, which was based on Nafion 115 with 0.6 mg cm⁻² platinum on the cathode and 3.0 mg cm⁻² iridium/ruthenium oxide on the anode (ITM Power, United Kingdom). The flow-field consisted of nine parallel channels, with a length of 3 cm and a land and channel width of 1.76 mm. The electrolyser was run at ambient pressure with a deionized water inflow temperature of 50°C and a water inflow rate of 10 ml min⁻¹ at the anode and cathode. Electrochemical testing was performed between 0.0 and 2.0 A cm⁻² using a potentiostat (Gamry Reference 3,000 Galvanostat/Potentiostat with a Gamry 30k Booster; Gamry Instruments, USA).



Acoustic Emission

AE was measured with a cylindrical piezoelectric sensor (S9208, Mistras NDT, United Kingdom), with a diameter and height of 25 mm. The sensor was placed in the center of the flow-field on the anode side; data acquisition lasted 1 min during galvanostatic operation of the PEMWE. Due to the nature of sound transmission, no clear area can be defined within which acoustic data is collected. Whether a mechanical perturbation is detected by the sensor is contingent on the location and intensity of the perturbation, with the intensity necessary for detection increasing with the distance between acoustic source and sensor. Therefore, detection of stagnant bubbles is increasingly likely as they are located closer to the sensor (bubbles "grow" from the top end of the channel toward the center). Data were processed using the software AEWin (Physical Acoustics, USA). The sensor produces a continuous voltage/time signal, with strong mechanical perturbations producing high voltage values. After filtering and preamplification by 26 dB, acoustic hits exceeding a noise threshold of 37 dB were extracted from the continuous signal. An acoustic hit is defined as an acoustic event initiated by AE signal exceeding the noise threshold and ending when the signal falls back below that threshold (Figure 2). Strong acoustic activity is marked by a high number of separate acoustic hits (events). The number of hits per unit time (hit rate H), the maximum of each waveform averaged over all hits (average hit amplitude A), the averaged time from exceeding the threshold until falling back below it (average hit duration D) and the average hit energy E were recorded. The hit energy was determined by integrating the area under the waveform with respect to time. Further details on AE data analysis can be found in previous work (Maier et al., 2019).

High-Speed Imaging

To visualize the movement of bubbles and the effect of increasing current density on the rate of removal of bubbles in the flow channels, high-speed imaging was employed. A Photron FASTCAM SA1 high-speed camera with a Tokina MACRO 100 F2.8 D lens was used to image the full flow-field on the anode side (1024 \times 1024 pixel resolution, 2,000 frames per second, 5.46 s acquisition). The transparent end-plates allowed for direct optical access to the flow-field (Dedigama et al., 2014; Majasan et al., 2018).

RESULTS AND DISCUSSION

The bubble evolution as a function of the current density has been captured with high-speed imaging experiments, which are shown as a function of increasing current density (Figure 3). As the cross-sectional area of the flow channels is finite and as all bubbles have to leave the flow-field through the manifold at the top end of the flow channels, the ability of the PEMWE cell to remove product gas is limited. This leads to bubbles blocking the top end of the flow channels at high current densities. For a given flow rate, the length of channel that contains stagnant bubbles at the top end of the flow channel increases significantly with current density. Here, a stagnant bubble is defined as a bubble which does not change its location, and particularly a bubble at the top end of the channel not entering the combining manifold, but remaining at the top end of the flow channel. The location of the largest stagnant bubble in each image in Figure 3 is marked in red. The amount of oxygen produced at the anode increases as a function of current density (Faraday's law); hence, a growth in the length of stagnant bubbles is expected with increasing current density. At a current density of 0.3 A cm^{-2} (Figure 3A) the top end of each channel is almost free of stagnant bubbles, while a clear growth of these bubbles can be observed at 0.6 A cm^{-2} (Figure 3B). At 1.0 A cm^{-2} (Figure 3C), bubble blockage covers more than a quarter of the channel length.

AE parameters are strongly influenced by the current density (Figure 4). As illustrated above, current density leads to bubble blockage at the top end of the flow channels; hence, Figure 4 can be interpreted as the correlation between AE signal and the formation of stagnant bubbles. The acoustic hit rate drops from 80.0 s^{-1} to the limit of detection for AE system used in this work (1.0 s^{-1}) between 0.5 and 1.0 A cm⁻² (Figure 4A). The limit of detection is an artifact of the data acquisition, which cuts off any hit longer than 1.0 s, which means that from 1.0 A $\rm cm^{-2}$ onwards AE signal continuously exceeds the noise threshold, with no individual acoustic hits discernible. This significant decrease of acoustic hits highlights a dramatic change of two-phase flow within the flow channels. The relationship between the number of acoustic hits and the number of bubbles passing through the flow channels has been established in previous work (Maier et al., 2019), which found that the number of acoustic hits scales directly with the number of bubbles passing through the flow channels. Hence, a drop in the number of acoustic hits indicates a decrease in the number of bubbles generated and passing through the flow channels, which is likely due to the blocking of the flow





FIGURE 4 | Acoustic emission parameters as a function of current density for a water inflow rate of 10 ml min⁻¹. Acoustic hit rate (A), average hit amplitude (B), average hit duration (C), and average hit energy (D) are shown.

channel by a stagnant bubble. This stagnant bubble stops smaller bubbles from traveling upwards through the flow channels; instead the bubbles coalesce into the stagnant bubble. Hence, the drop in the number of acoustic hits between 0.5 and $1.0 \,\mathrm{A \, cm^{-2}}$ is likely caused by the extension of stagnant bubbles into the sensor area.

Further, the average hit amplitude (**Figure 4B**) increases steeply by around 50% between 0.5 and 1.0 A cm^{-2} , the same range within which the hit rate drops. The average hit duration increases from less than 0.1 m s to the cut off value of 1.0 s mentioned above (**Figure 4C**). For current densities above 1.0 A cm⁻², a constant signal is detected, indicating permanent contact between a bubble and the end-plate. Finally, an increase in hit duration and amplitude causes an increase in acoustic energy (**Figure 4D**). All these changes occur in a step-like manner between 0.5 and 1.0 A cm⁻².

The decreasing number of hits, while hit amplitude and contact time between bubble and end-plate increase, all suggest that the signal change is caused by the extension of the stagnant bubble region toward the sensor location in the current density range between 0.5 and 1.0 A cm⁻² (Figure 4). This is supported by the extension of the stagnant bubble region (Figure 3) observed via high-speed imaging, a major part of which occurs between 0.6 and 1.0 A cm⁻².

CONCLUSION

AE has been demonstrated as a useful technique for operando diagnosis of bubble blockage in PEMWEs. High-speed imaging of an optically-transparent PEMWE cell was used to visualize the bubble movement in the flow channels. The length of the part of the flow channel containing stagnant bubbles was found to increase with current density, eventually reaching the location of AE sensor. With increasing flow channel blockage, a dramatic change in acoustic activity was observed. The acoustic hit rate dropped from 80.0 to 1.0 s⁻¹, average hit amplitude increased from 32 to 50 dB, average hit duration from 0.1 m s to 1.0 s, and average hit energy from 0.004 to 3,400 aJ. These changes occurred abruptly between 0.5 and 1.0 A cm⁻², which coincides with a significant extension of the stagnant bubble region in the flow channels. This leads us to conclude that the change in acoustic activity is caused by the flow regime in the channels changing from two-phase flow to stagnant bubbles. The accumulation of gas in the flow channels occurs when gas production exceeds the capacity of the system for gas removal, which can affect the water distribution in the

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PEMWE. Insufficient water supply at the anode causes a voltage increase (Sun et al., 2015), hence lowers PEMWE efficiency and reduces hydrogen production at equal voltage. It is expected that AE can be used to detect local bubble blockage and insufficient water supply in specific areas of a PEMWE.

The use of this *operando* diagnostic tool has successfully been applied to a PEMWE, but could be extended to other applications. The accumulation of gas within a system or plant can cause inefficiencies or pose a hazard in many areas of chemical production and transport. Moreover, it has been shown that the change of two-phase flow regime influences the pressure drop (Cubaud and Ho, 2004; Choi et al., 2011). Hence, the technique presented in this work could be deployed to screen various flow-field configurations or monitor safe limits of operation, replacing less cost-effective or accessible diagnostic tools such as neutron or X-ray imaging (Panchenko et al., 2018; Majasan et al., 2019; Maier et al., 2020).

DATA AVAILABILITY STATEMENT

The raw data supporting the conclusions of this article will be made available by the authors, without undue reservation.

AUTHOR CONTRIBUTIONS

MM: conceptualization, methodology, formal analysis, investigation, writing—original draft, visualization. QM and YW: resources, conceptualization, writing—review and editing. JM: conceptualization, investigation, writing—review and editing. RW, JR, LC, and GH: conceptualization, writing—review and editing. JD: investigation, writing—review and editing. PS and DB: supervision, funding acquisition, writing—review and editing.

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Conflict of Interest: The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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6