



Heat Transfer Analysis of 3-D Viscoelastic Nanofluid Flow Over a Convectively Heated Porous Riga Plate with Cattaneo-Christov Double Flux

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The impact of heat-absorbing viscoelastic nanofluidic flow along with a convectively

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Loganathan K, Alessa N and Kayikci S (2021) Heat Transfer Analysis of 3-D Viscoelastic Nanofluid Flow Over a Convectively Heated Porous Riga Plate with Cattaneo-Christov Double Flux. Front. Phys. 9:641645. doi: 10.3389/fphy.2021.641645 heated porous Riga plate with Cattaneo-Christov double flux was analytically investigated. The Buongiorno model nanofluid was implemented with the diversity of Brownian motion and thermophoresis. Making use of the transformations; the PDE systems are altered into an ODE system. We use the homotopy analysis method to solve these systems analytically. The reaction of the apposite parameters on fluid velocity, fluid temperature, nanoparticle volume fraction skin friction coefficients (SFC), local Nusselt number and local Sherwood number are shown with vividly explicit details. It is found that the fluid velocities reflect a declining nature for the development of viscoelastic and porosity parameters. The liquid heat becomes rich when escalating the radiation parameter. In addition, the nanoparticle volume fraction displays a declining nature towards the higher amount of thermophoresis parameter, whereas the inverse trend was obtained for the Brownian motion parameter. We also found that the fluid temperature is increased in viscoelastic nanofluid compared to the viscous nanofluid. When we change the fluid nature from heat absorption to heat generation, the liquid temperature also rises. In addition, the fluid heat is suppressed when we change the flow medium from a stationary plate to a Riga plate for heat absorption/generation cases.

Keywords: viscoelastic nanofluid, porous riga plate, bidirctional streching sheet, cattaneo- christov double flux, homotopy analysis method

1 INTRODUCTION

Many industries depend on fluids, because they play an indispensable role in the heating and cooling process. Regular fluids like oil, ethylene, water, and glycol normally have scant heat transfer (HT) attributes because of their lesser thermal conductivity. So enhancing the fluid thermal conductivity is essential to cut down the work time process and extend equipment work life. Adding metallic nanosized (1–100 mm) particles, like Cu, Fe, Ti, Ag, or their oxides to regular fluids can reinforce their thermal conductivity. Rana and Bhargava [1] conducted HT analysis of a nanofluidic flow over a non-linear stretching surface (SS). They detected that fluid heat develops in huge quantities in the Brownian motion (BM) parameter. Khan and Pop [2] formed a mathematical model of 2D boundary

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layer flow of a nanofluidic flow over an SS. They learned that the mass transfer gradient depresses when the thermophoresis values enlarge. Bachok et al. [3] studied the flow of nanofluid on a moving semi-infinite plate and discovered that there was a larger energy rate when the Prandtl number was smaller. Viscoelastic nanofluidic flow with velocity slip with the finite element method was scrutinized by Goyal and Bhargava [4]. They observed that fluid heat enriches with the rising values of velocity slip. Hassani et al. [5] derived the series solution of a nanofluid over an SS. It is identified that a smaller mass transfer rate is obtained in higher values of the BM parameter. The recent developments for this direction are found in the referenced works [6–9].

Recently, several researchers have tried to prevent the reduction of mechanical energy. One of the simplest ways is to reduce the drag force, which helps to increase the mechanical energy. A Riga plate (RP) is one of the external agents used to curtail the drag force and control the fluid flow. This phenomenon is adopted in many production processes, like, MHD power generators, solar energy devices, heat exchangers, thermal nuclear reactors, and energy recovery, etc. The Blasius fluid flow past an RP was inspected by Magyari and Pantokratoras [10]. The impact of thermophoresis and Brownian parameters of a nanofluidic flow at an RP was addressed by Adeel et al. [11]. They identified that skin friction coefficient (SFC) diminishes with a developing modified Hartmann number (MHN). Zero normal wall mass flux of tangent hyperbolic nanofluidic flow on an RP, including partial slip, thermal radiation, and a chemical reaction along with activation energy was inspected by Nayak et al. [12]. New attempts for the above concept are included in the referenced works [13-16].

Many researchers are interested in examining the importance of convective boundary condition, because many engineering processes are based on these conditions. A few examples are, nuclear plants, thermal energy storage, transpiration cooling, geothermal energy extraction, laser pulse heating, petroleum processing, textile drying, and many others. Ahmad et al. [17] numerically examined nanofluidic flow on an RP with a convective heating (CH) condition. Their results speculate that temperature gradient reflects an inciting nature for strengthening the Biot number. Ramzan et al. [18] studied a radiative Williamson nanofluid on an RP with CH. They discovered that fluid heat develops when the value of the Biot number increases. Zaib et al. [19]. elucidated the flow of a blended convective micropolar fluid occupied by water/kerosene based Ti O₂ nanoparticles on a Riga surface. The impact of CH of a third-grade nanofluid flow over an SS with entropy features was discussed by Loganathan et al. [20]. They proved that entropy rate increases when the Biot number increases. Nanofluidic flow over a convectively heated surface was portrayed by Makinde and Aziz [21]. Their results show that the thermal boundary layer thickness becomes thicker when the Biot number increases. Notable studies of convective boundary conditions are seen in the referenced works [22-24].

The aforementioned inspection reveals that many authors are willing to divulge the analysis of HT and MT using the Cattaneo-Christov theory with different physical configurations. But nobody yet has investigated the above analysis with porous RP. So we investigate the viscoelastic nanofluidic flow over a convectively heated porous RP. The homotopy method was implemented for solving the physical governing equations and the computational results are reported via graphs and tables. In petroleum engineering, pore space is essential for finding the permeability and porosity of a reservoir rock. So, this property is necessarily needed for storage capacity and flow motion. Further, the fluid needs to have heat generating and absorbing characteristics because this property can change the temperature gradient in the flow field. Potential applications of this effect are semi-conductor wafers, electronic chips, and





TABLE 1 Homotopy Analysis Method order.					
Order	– f ^{′′} (0)	- g ^{''} (0)	-θ [′] (0)	φ [΄] (0)	
1	1.17000	0.35400	0.32089	0.16044	
5	1.20748	0.39798	0.32123	0.16062	
10	1.20927	0.40069	0.32114	0.16057	
15	1.20933	0.40080	0.32113	0.16057	
20	1.20933	0.40080	0.32113	0.16057	
25	1.20933	0.40080	0.32113	0.16057	
30	1.20933	0.40080	0.32113	0.16057	
35	1.20933	0.40080	0.32113	0.16057	
40	1.20933	0.40080	0.32113	0.16057	

combustion modeling. Also, these analyses are very useful in thermal engineering for designing thermal systems. Some other different computational methods and their utilizations are obtained in the referenced works [27–31].

2 MATHEMATICAL FORMULATION

We now look into the 3D flow of VENF flow in a stretchy RP at z = 0. The plate is fixed at z = 0 and the flow is restrained to $z \ge 0$. Let $u_w(x, y) = ax$ and $v_w(x, y) = by$ be the plate velocity in x & y directions. The plate has an invariable temperature T_w and nanoparticle concentration C_w . When $z \to \infty$, the free stream value of temperature and nanoparticle concentration is denoted by T_∞ and C_∞ . The HT and MT attributes are inspected along with CCDF. The base of the plate is convectively heated with hot fluid along with temperature T_f and this generates a HT coefficient $h_{\rm c}$ see **Figure 1**. The ruling boundary layer equations are taken from [25].

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$
(1)
$$\frac{\partial u}{\partial x} u + \frac{\partial u}{\partial y} v + \frac{\partial u}{\partial z} \widehat{w} = v \frac{\partial^2 u}{\partial z^2}$$
$$-\beta \left[\frac{\partial^3 u}{\partial x \partial z^2} u + \frac{\partial^3 u}{\partial z^3} w - \frac{\partial^2 u}{\partial z^2} \frac{\partial u}{\partial x} - \frac{\partial^2 w}{\partial z^2} \frac{\partial u}{\partial z} - 2 \frac{\partial^2 u}{\partial x \partial z} \frac{\partial u}{\partial z} - 2 \frac{\partial^2 u}{\partial z^2} \frac{\partial w}{\partial z} \right]$$
$$+ \frac{\pi J_0 M_0}{8\rho} \exp\left(\frac{-\pi y}{a}\right) - \frac{v}{k_1} u$$
(2)
$$\frac{\partial v}{\partial x} u + \frac{\partial v}{\partial y} v + \frac{\partial v}{\partial z} w = v \frac{\partial^2 v}{\partial z^2}$$

$$-\beta \left[\frac{\partial^3 v}{\partial y \partial z^2} v + \frac{\partial^3 v}{\partial z^3} w - \frac{\partial^2 v}{\partial z^2} \frac{\partial v}{\partial y} - \frac{\partial^2 w}{\partial z^2} \frac{\partial v}{\partial z} - 2 \frac{\partial^2 v}{\partial y \partial z} \frac{\partial v}{\partial z} - 2 \frac{\partial^2 v}{\partial z^2} \frac{\partial w}{\partial z} \right] - \frac{v}{k_1} v$$
(3)

TABLE 2 Illustrating the disparity of $-f''(0)$ and $-g''(0)$ with c when $K = Q = \Lambda = 0.0$ from Qa	ayyum et al. [25] and Li et al. [26].
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с		- f ″ (0)			- g ^{′′} (0)		
-	Present	Reference [25]	Reference [26]	Present	Reference [25]	Reference [26]	
0.0	1.00000	1.000000	1.000000	0.00000	0.000000	0.000000	
0.1	1.02026	1.020259	1.020259	0.06685	0.066847	0.066847	
0.2	1.03950	1.039495	1.039495	0.14874	0.148736	0.148736	
0.3	1.05795	1.057954	1.057954	0.24336	0.243359	0.243359	
0.4	1.07579	1.075788	1.075788	0.34921	0.349208	0.349208	
0.5	1.09309	1.093095	1.093095	0.46521	0.465204	0.465204	
0.6	1.10995	1.109946	1.109946	0.59053	0.590528	0.590528	
0.7	1.12640	1.126397	1.126397	0.72453	0.724531	0.724531	
0.8	1.14249	1.142488	1.142488	0.86668	0.866682	0.866682	
0.9	1.15825	1.158253	1.158253	1.01654	1.016538	1.016538	
1.0	1.17371	1.173720	1.173720	1.17371	1.173720	1.173720	

TABLE 3 | Skin friction coefficients, local Nusselt number, and Local Sherwood number for different values of K, Q, and Λ .

к	На	Λ	$Cf_{\widehat{x}}$	$Cf_{\widehat{y}}$	Nu/ $\sqrt{\text{Re}}$	Sh/ $\sqrt{\text{Re}}$
0.0	0.3	0.2	-1.00195	-0.28096	0.45340	0.08097
0.1	_	_	-1.44476	-0.38462	0.45178	0.08068
0.2	_	_	-2.00748	-0.55310	0.449580	0.08028
0.3	_	_	-2.87497	-0.99095	0.44580	0.07961
0.2	0.0	0.2	-2.32521	-0.54489	0.44708	0.07983
_	0.3	_	-2.00748	-0.55310	0.44958	0.08028
_	0.5	_	-1.79030	-0.55819	0.45117	0.08057
_	0.8	_	-1.45495	-0.56533	0.45348	0.08098
_	1.0	_	-1.22404	-0.56979	0.45498	0.08125
0.2	0.3	0.0	-1.79757	-0.48352	0.45159	0.08064
_	_	0.3	-2.10575	-0.58525	0.44867	0.08011
_	_	0.5	-2.29118	-0.64526	0.44700	0.07982
_	_	0.8	-2.54649	-0.72670	0.44483	0.07943
_	-	1.0	-2.70513	-0.77650	0.44356	0.07921

with

$$u = u_w(x) = ax, \quad v = v_w(y) = by, \quad w = 0 \quad at \quad z = 0$$

$$u \to 0, v \to 0 \quad as \quad z \to \infty$$
(4)

The energy and concentration expressions are taken from [31].

$$\frac{\partial T}{\partial x}u + \frac{\partial T}{\partial y}v + \frac{\partial T}{\partial z}w + \Omega_T = \alpha \left(1 + \frac{16\sigma^* T_{\infty}}{3KK^*}\right)\frac{\partial^2 T}{\partial z^2} + \tau \left[D_B \frac{\partial T}{\partial z}\frac{\partial C}{\partial z} + \frac{D_T}{T_{\infty}}\left(\frac{\partial T}{\partial z}\right)^2\right] + \frac{Q}{\rho C_p}\left(T - T_{\infty}\right) + \frac{\partial C}{\partial x}u + \frac{\partial C}{\partial y}v + \frac{\partial C}{\partial z}w + \Omega_C = D_B \frac{\partial^2 C}{\partial z^2} + \frac{D_T}{T_{\infty}}\left(\frac{\partial^2 T}{\partial z^2}\right)$$
(6)

where

$$\Omega_{T} = \frac{\partial^{2} T}{\partial x^{2}} u^{2} + \frac{\partial^{2} T}{\partial y^{2}} v^{2} + \frac{\partial^{2} T}{\partial z^{2}} w^{2} + \left(\frac{\partial u}{\partial x}u + \frac{\partial u}{\partial y}v + \frac{\partial u}{\partial z}w\right)\frac{\partial T}{\partial x}$$

$$+ \left(\frac{\partial v}{\partial x}u + \frac{\partial v}{\partial y}v + \frac{\partial v}{\partial z}w\right)\frac{\partial T}{\partial y} + \left(\frac{\partial w}{\partial x}u + \frac{\partial w}{\partial y}v + \frac{\partial w}{\partial z}w\right)\frac{\partial T}{\partial z}$$

$$+ 2\frac{\partial^{2} T}{\partial x \partial y} uv + 2\frac{\partial^{2} T}{\partial y \partial z} vw + 2\frac{\partial^{2} T}{\partial x \partial z} uw \qquad(7)$$

$$\Omega_{C} = \frac{\partial^{2} C}{\partial x^{2}} u^{2} + \frac{\partial^{2} C}{\partial y^{2}} v^{2} + \frac{\partial^{2} C}{\partial z^{2}} w^{2} + \left(\frac{\partial u}{\partial x}u + \frac{\partial u}{\partial y}v + \frac{\partial u}{\partial z}w\right)\frac{\partial C}{\partial x}$$

$$+ \left(\frac{\partial v}{\partial x}u + \frac{\partial v}{\partial y}v + \frac{\partial v}{\partial z}w\right)\frac{\partial C}{\partial y} + \left(\frac{\partial w}{\partial x}u + \frac{\partial w}{\partial y}v + \frac{\partial w}{\partial z}w\right)\frac{\partial C}{\partial z}$$

$$+ 2\frac{\partial^{2} C}{\partial x \partial y} u v + 2\frac{\partial^{2} C}{\partial y \partial z} vw + 2\frac{\partial^{2} C}{\partial x \partial z} uw$$
(8)

TABLE 4 | Variation of $\theta(\eta)$ for various combinations of Ha, R, and Hg for VENF and NF.

На	Rd	VENF		NF		
_	_	Hg = -0.3	Hg = 0.3	Hg = -0.3	Hg = 0.3	
0.3	0.0	0.341801	0.566542	0.334881	0.503372	
_	0.3	0.387789	0.693752	0.379921	0.607053	
_	0.5	0.412705	0.767952	0.404436	0.670709	
_	0.8	0.444218	0.865097	0.435574	0.757369	
_	1.0	0.462376	0.921645	0.453587	0.809522	
0.0	0.0	0.34644	0.627145	0.338425	0.536566	
_	0.3	0.393138	0.771438	0.384076	0.656213	
_	0.5	0.418363	0.852970	0.408874	0.727462	
_	0.8	0.450175	0.957019	0.440306	0.822149	
-	1.0	0.468456	1.016220	0.458451	0.877948	

$$-k\frac{\partial T}{\partial z} = -h_c (T - T_f), \quad \frac{D_T}{T_{\infty}} \frac{\partial T}{\partial z} + D_B \frac{\partial C}{\partial z} = 0 \quad at \quad z = 0$$
$$T \to T_{\infty}, \quad C \to C_{\infty} \quad as \quad z \to \infty$$
(9)

u, v, & w are the "fluid speed components," x, y & z are the "direction co-ordinates," v is the "kinematic viscosity," β is the "material parameter of fluid," k1 is the "permeability of the porous medium," a is the" width of magnets and electrodes," J₀ is the "applied current density of the electrodes," M₀ is the "magnetization of the permanent magnets," p is the "fluid density," T is the "fluid temperature," $\Omega_T \; \Omega_C$ are the "relaxation time of heat and mass fluxes," a is the "thermal diffusivity," Cp is the "specific heat capacity," σ^* is the "Stefan Boltzmann constant," k is the "fluid thermal conductivity," k* is the "mean absorption coefficient," Q is the "heat absorption/generation coefficient," D_B is the "mass diffusivity," C is the "fluid concentration," τ is the "ratio of the effective heat capacity of the nanoparticle material and the base fluid," T_∞ & C_∞ are the "free stream temperature and concentration," and $D_{\rm T}$ is the "thermophoretic diffusion coefficient."

The instigation of dimensionless are taken from [31].

$$u = f'(\eta)xa, v = g'(\eta)ya, w = -\sqrt{\nu a}(g(\eta) + f(\eta))$$

$$\eta = \sqrt{\frac{a}{\nu}}z, \theta(\eta) = \frac{T - T_{\infty}}{T_f - T_{\infty}}, \phi(\eta) = \frac{C - C_{\infty}}{C_w - C_{\infty}}$$
(10)

$$f''' + gf'' + ff'' - [f']^2 + Kgf^{iv} + Kff^{iv} - Kg''f'' + Kf''f''$$

$$-2Kg'f''' - 2Kf'f''' - \Lambda f' + Hae^{-\beta\eta} = 0.$$
 (11)

$$g''' + gg'' + fg'' - [g']^2 + Kgg^{i\nu} + Kfg^{i\nu} + Kg''g'' - Kf''g'' - 2Kg'g''' - \Lambda g' = 0.$$
(12)

$$\theta''\left(1+\frac{4}{3}Rd\right) + Prg\theta' + Prf\theta' - Pr\Gamma\{\theta''\left[g+f\right]^2 + \theta'\left[g+f\right]^2\right] + f'\left[g'+f'\right] + PrN_b\phi'\theta' + PrN_t\theta^2 + PrHg\theta = 0, \quad (13)$$

$$\phi^{\prime\prime} + Scg\phi^{\prime} + Scf\phi^{\prime} - Sc\Gamma_{c}\{\phi^{\prime\prime}[g+f]^{2} + \phi^{\prime}[g+f][g^{\prime}+f^{\prime}]\} + \frac{N_{t}}{N_{b}}\theta^{\prime\prime} = 0.$$
(14)

with the condition that

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$$f(0) = 0, f'(0) = 1, g(0) = 0, g'(0) = c, \theta'(0) = -Bi[1 - \theta(0)], Nb\phi'(0) + Nt\theta'(0) = 0, (15) f'(\infty), g'(\infty), \theta(\infty), \phi(\infty) \to \infty$$

where $K = \frac{\beta a}{\nu}$ is the "viscoelastic parameter" (VEP), $\Lambda = \frac{\nu}{k_1 a}$ is the "porosity parameter," $Hm = \frac{\pi l_0 M_0}{8 \rho a^2 x}$ is the "modified Hartmann number" (MHN), $Rd = \frac{4\sigma_0^2 T_{co}^2}{k_k}$ is the "radiation parameter" $Pr = \frac{\nu}{a}$ is the "Prandtl number," $\Gamma =$ Ω_{Ta} is the "non-dimensional thermal relaxation time parameter," $\Gamma_c = \Omega_C a$ is the "non-dimensional nanoparticle relaxation time parameter," $Hg = \frac{Q}{\rho C_p a}$ is the "heat generation/ absorption parameter," $Sc = \frac{\nu}{D_B}$ is the "Schmidt number," $c = \frac{b}{a}$ is the "stretching ratio," $Nb = \frac{\tau D_B (C_w - C_{co})}{\nu}$ is the "Brownian motion parameter" (BM), $Nt = \frac{\tau D_T (T_f - T_{co})}{\nu T_{co}}$ is the "thermophoresis parameter," and $Bi = \frac{h_c \sqrt{\frac{2}{k}}}{k}$ is the "Biot number."

Then, the dimensionless form of the skin friction coefficients $(C_{f_x} \& C_{f_y})$, local Nusselt number (Nu), and local Sherwood number (Sh) are defined as

$$\tau_{wx} = v \frac{\partial u}{\partial z} + k_1 \left[u \frac{\partial u}{\partial x \partial z} + v \frac{\partial u}{\partial y \partial z} + w \frac{\partial u}{\partial z^2} + \frac{\partial u}{\partial z} \frac{\partial u}{\partial x} + \frac{\partial v}{\partial z} \frac{\partial v}{\partial x} + 2 \frac{\partial w}{\partial z} \frac{\partial w}{\partial x} - \frac{\partial w}{\partial z} \frac{\partial u}{\partial z} \right]_{z=0}$$
(16)
$$\frac{\partial v}{\partial x} = \int_{z=0}^{z} \frac{\partial v}{\partial x} + 2 \frac{\partial v}{\partial z} \frac{\partial v}{\partial x} - \frac{\partial u}{\partial z} \frac{\partial u}{\partial z} \frac{\partial u}{\partial z} \frac{\partial v}{\partial z} \frac{\partial v}{\partial y} \frac{\partial v}{\partial z} \frac{\partial v}{\partial v} \frac{$$

$$\tau_{wy} = v \frac{\partial v}{\partial z} + k_1 \left[u \frac{\partial v}{\partial x \partial z} + v \frac{\partial v}{\partial y \partial z} + w \frac{\partial v}{\partial z^2} + \frac{\partial u}{\partial z} \frac{\partial u}{\partial y} + \frac{\partial v}{\partial z} \frac{\partial v}{\partial y} \right]_{z=0}$$
(17)

$$Nu = \frac{xk_T \left[\frac{\partial T}{\partial z}\right]_{Z=0}}{k_T \left(T_w - T_\infty\right)} \left[-\frac{4\sigma_0}{3k^*} \left(\frac{\partial T^4}{\partial z}\right)_{z=0}\right]$$
(18)

$$Sh = -\frac{x\left[\frac{\partial c}{\partial z}\right]_{Z=0}}{(c_w - c_\infty)}$$
(19)

$$\begin{split} C_{f_x}\sqrt{Re} &= f''(0) + 2Kf''(0)f'(0) - Kg(0)f'''(0) \\ &-Kf(0)f'''(0) + Kg'(0)f''(0) + Kf'(0)f'''(0), \\ C_{f_y}\sqrt{Re} &= g''(0) + 2Kg''(0)g'(0) - Kg(0)g'''(0) - Kf(0)g'''(0) \\ &+ Kg'(0)g''(0) + Kf'(0)g'''(0), \\ Nu/\sqrt{Re} &= -\left(1 + \frac{4}{3}Rd\right)[\theta'(0)], \quad Sh/\sqrt{Re} &= -[\phi'(0)]. \end{split}$$

3 HOMOTOPY ANALYSIS METHOD SOLUTIONS

The initial assumptions are $f_0(\eta) = 1 - e^{-\eta}$, $g_0(\eta) = c(1 - e^{-\eta})$, $\theta_0(\eta) = \frac{Bie^{-\eta}}{1+Bi}$, and $\phi_0(\eta) = -\frac{NiBie^{-\eta}}{Nb(1+Bi)}$.

The linear operators are $L_f = f''' - f'$, $L_g = g''' - g'$, $L_\theta = \theta'' - \theta$, and $L_\phi = \phi'' - \phi$. with the properties.

$$L_f \left[\omega_1 + \omega_2 e^{\eta} + \omega_3 e^{-\eta} \right] = 0$$
 (20)

$$L_{\sigma}[\omega_{4} + \omega_{5}e^{\eta} + \omega_{6}e^{-\eta}] = 0$$
 (21)

$$L_{0}[\omega_{7}e^{\eta} + \omega_{0}e^{-\eta}] = 0$$
 (22)

$$L_{\phi} \left[\omega_{9} e^{\eta} + \omega_{10} e^{-\eta} \right] = 0 \tag{23}$$

in which, ω_i , (i = 1–10) denote the arbitrary constants.



Finally, the general solution of equations (52)-(55) can be written as.

$$f_m(\eta) = f_m^*(\eta) + \omega_1 + \omega_2 e^{\eta} + \omega_3 e^{-\eta}$$
(24)

$$g_m(\eta) = g_m(\eta) + \omega_4 + \omega_5 e^{\eta} + \omega_6 e^{-\eta}$$
(25)

$$\theta_m(\eta) = \theta_m(\eta) + \omega_7 e^{\eta} + \omega_8 e^{-\eta}$$
(26)

$$\phi_m(\eta) = \phi_m^*(\eta) + \omega_9 e^{\eta} + \omega_{10} e^{-\eta}$$
(27)

here particular solutions are denoted as $f_m^*(\eta)$, $g_m^*(\eta)$, $\theta_m^*(\eta)$, and $\phi_m^*(\eta)$.

The use of control variables $(h_{f_2}, h_g, h_{\theta_0}, h_{\varphi})$ play a significant role in the convergence of the series. Hence **Figures 1A,B** displays the h-curves. It is observed that the acceptable

values of h_f , $h_{\tilde{g}}$, $h_{\tilde{\theta}}$, h_{ϕ} are $-1.8 \le h_f$, $h_g \le -0.5$, $-1.4 \le h_{\theta}$, and $h_{\phi} \le -0.2$, see **Figures 2A,B**. For a more accurate solution, we choose -1 as the $h_f \& h_g$ values and -0.8 for $h_{\theta} \& h_{\phi}$. The HAM order of approximation is portrayed in **Table 1** and we proved that the 15th order is enough for all profiles. **Table 2** shows the evaluation of -f'(0) for different c values from Qayyum et al. [25] and Li et al. [26]. From this table, we conclude that our outcomes have high accuracy.

4 Correlation Analysis

To analyze the performance of the thermal system design, correlation equations are crucial. The obtained numerical values are used to derive the correlation equations with the help of linear regression analysis. The correlation equations of the Nusselt number and Sherwood number are derived as



here Ha $\in \{0, 0.3\}, \Lambda \in [0, 0.4]$, and R $\in [0, 1]$ with maximum error is 0.0076.

5 RESULTS AND DISCUSSION

The impact of the distinguished variables on the velocities, temperature, NPVF, SFCs, LNN, and LSN are interpreted in this section. **Table 3** establishes the significance of K, Ha, and Λ on Cf_x , Cf_y , Nu/\sqrt{Re} , and Sh/\sqrt{Re} . It is found that the SFCs, LNN, and LSN become smaller with higher values of K

and A. In addition, the HT and MT gradients form an enhancing behavior and SFCs form a decaying behavior with the rising values of MHN. The significance of fluid temperature $(\theta(\eta))$ for various combinations of Ha, Rd, and Hg is exhibited in **Table 4**. We noted that fluid heat heightens as the value of Rd increases for all cases. The maximum fluid temperature is attained with a heat generating VENF on an SP with a high presence of radiation. Also we found that fluid temperature decreases in RP with a heat absorbing NF and the absence of radiation. In the RP and VENF case, we change the fluid nature from heat absorption to heat generation; the minimum increase percentage (66%) is attained at Rd = 0 and the maximum enhancing percentage (99%) is obtained at Rd = 1. This analysis clearly shows that radiation plays an important role in rising



fluid temperature. In the SP and VENF fluid case, (81%) and (117%) are the smallest and highest enhance percentage of fluid heat with the absence and presence of radiation, respectively. In the RP and NF case, we change the fluid nature from heat absorption to heat generation, the lowest increase percentage (50%) is attained at Rd = 0 and the maximum rising percentage (79%) is obtained at Rd = 1. In the SP and NF case, (59%) and (92%) are the smallest and highest enhance percentage of fluid heat with the absence and presence of radiation, respectively. In the above observation, fluid is quickly heated in VENF compared to NF with an increasing radiation parameter. In addition, fluid temperature is suppressed when we change the flow medium from SP to RP for heat absorption/ generation cases.

The consequences of a viscoelastic parameter, porosity parameter, and stretching ratio parameter on both velocity profiles over a porous and non-porous RP are shown in **Figures 3A–F**. We proved that both direction velocities become smaller when escalating the values of K. Physically, a stronger viscoelastic effect creates a stronger resistive force and this force opposes fluid motion. Thereby the fluid velocity and its associative boundary layer (BL) thickness diminishes when the values of K are raised. In addition, the thickness of the momentum BL is high in viscous fluid (K = 0.0) compared to the viscoelastic fluid K \neq 0, see **Figures 3A,B**. We found that x-direction velocity declines against a higher quantity of c whereas the opposite behavior was attained for y-direction velocity. From these figures, we also found that the larger momentum BL thickness is obtained in NPRP for the x-direction and in PRP for the y-direction, see **Figures 3C,D**.

Figures 4A-F indicate the variations of temperature profile for distinct values of Γ, Rd, and Nt for PRP, NPRP, PSP, and NPSP. We detected that fluid heat decreases with larger values of Γ. Higher thermal BL thickness in both plates was attained only in the presence of porous medium, see Figures 4A,B. We noticed that the fluid temperature increases with rising values of Rd (Figures 4C,D). Physically, a larger quantity of the radiation parameter generates more heat in the fluid and enhances the thickness of thermal BL. The thickness of the thermal BL is almost the same for RP and SP. Also, we found that a lower fluid temperature occurs in the non-porous plate for both cases. In Figures 4A,E,F larger thermophoresis parameter relates to higher fluid thermal conductivity and this causes an increase in the temperature of the fluid. Also, we noted that a smaller thermal BL thickness was apparent in the non-porous plate for both cases.

Figures 5A-F describe the impact of Nt, Nb, and Γ_c on NPVF profile for PRP, NPRP, PSP, and NPSP. In **Figures 5A,B**,



we see that the large values of Nt lead to the enhancement of the NPVF. Also, we proved that the NPVF is a non-developing function of Nb (5 (c-d)). From **Figures 5E,F**, we report higher values of Γ_c as the NPVF increases near the plate, which decreases further away from the surface. In the above cases, BL thickness of the NPVF becomes thinner in the non-porous plate for both cases. The SFC (x- direction) for various values of c and Λ is displayed in **Figures 6A,B**. We noticed that the SFC is suppressed with improving values of c and Λ . We also note that a larger SFC is attained in RP compared to the SP. An opposite situation was obtained for y- direction SFC, see **Figures 6C,D**. Only small variations were found between RP and SP.

Figures 7A–D portray the variations of LNN for various combinations of Rd, Ha, Γ , Hg, Bi, and Λ . From **Figures 7A,B**, we noticed that the fluid temperature gradient was suppressed with enhancing values of Rd, Hg, and Λ . In the convective heating case, the rate of change of HT rate is enhanced with a small quantity of Rd and is suppressed with a higher quantity of Rd, see **Figure 7C**. On the other hand, the decreasing rate of the

HT gradient is small for a small amount of Rd and is high for a larger amount of Rd, see **Figure 7D**. **Figures 8A-D** demonstrate the influence of Rd, Ha, Γ , Hg, Bi, and Λ on LSN. We found that the LSN is depressed with the increasing values of Rd, Hg, and Λ and is boosted with the escalating values of Γ . In both HT and MT gradients, the RP plays a significant role.

6 CONCLUSION

The outcomes of the BL flow of a heat-absorbing viscoelastic nanofluid with CCDF and convective heating has been considered and the obtained key points are as follows:

- The momentum BL thickness becomes small with the presence of the viscoelastic parameter
- The thermal BL thickness increases with larger values of the thermal relaxation time parameter
- The NPVF is highly negatively correlated with the presence of the Brownian motion parameter



- The skin friction coefficient declined with a higher modified Hartmann number
- An increase in Hg gives a reduction in the mass transfer gradient

DATA AVAILABILITY STATEMENT

The original contributions presented in the study are included in the article/supplementary materials, further inquiries can be directed to the corresponding author.

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AUTHOR CONTRIBUTIONS

All authors listed have made a substantial, direct, and intellectual contribution to the work and approved it for publication.

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GLOSSARY

BM brownian motion CCDF cattaneo-christov double flux CH convective heating HT heat transfer HAM homotopy analysis method LNN local nusselt number LSN local sherwood number MT mass transfer MHN modified hartmann number
NPVF nanoparticle volume fraction
ODE ordinary differential equations
PDE partial differential equations
PRP porous riga plate
RP riga plate
SFC skin friction coefficient
SP stationary plate
SS stretching surface/sheet
VENF viscoelastic nanofluid