



Oxygen Reduction Activity and Stability of Composite Pd_x/Co-Nanofilms/C Electrocatalysts in Acid and Alkaline Media

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The morphology tuning of Pd and Pd-M nanoparticles is one of the significant strategies to control the catalytic activity toward oxygen reduction reaction (ORR). In this study, composite Pd_x/Co-nanofilms/C electrocatalysts of Pd nanoparticles implanted onto Co nanofilms were synthesized on an immiscible ionic liquid (IL)/water interface for ORR. The Pd nanoparticles implanted onto Co nanofilms show a marked distortion of crystal lattice and surface roughness. These Pd_x/Co-nanofilms/C electrocatalysts exhibit enhanced activity for ORR compared with Pd/C and PdCo/C catalysts in both acid and alkaline solutions, in which the Pd₃/Co-nanofilms/C catalyst displays the highest ORR mass activity. The superior ORR mass activities of the fabricated Pd_x/Co-nanofilms/C catalysts may be mainly attributed to their larger catalytic areas, which are conferred by the rough surface of Pd nanoparticles with a distorted crystal lattice, and the synergistic effect between the surface Pd atoms and the 2D Co nanofilm substrate. The relationship between ORR mass activity and Pd/Co atom ratio varies in different electrolytes. Furthermore, by using proper heat-treatment methods, the Pd_x/Co-nanofilms/C catalysts exhibit improved cycling stability compared with pure Pd/C catalyst after extended potential cycling.

Keywords: composite electrocatalysts, palladium nanoparticles, co nanofilms, oxygen reduction reaction, alkaline solution, acid solution

INTRODUCTION

Development of low-cost, efficient and stable electrocatalysts for oxygen reduction reaction (ORR) is one of the key factors to promote the commercialization of low-temperature fuel cells (Shao et al., 2016; He et al., 2017; Sui et al., 2017; Wang et al., 2018). Pd-based electrocatalysts have attracted considerable attention in research for non-Pt catalysts for ORR, because Pd has a similar structural characteristic to Pt, is relatively abundant on earth and displays the four-electron reduction of oxygen (Zhen et al., 2014; Doan et al., 2016; Zhang et al., 2016). So far, the most popular strategies including alloying Pd with various transition metals [e.g., Co (Wei et al., 2011; Rahul et al., 2014; Yun et al., 2015), Fe (Holade et al., 2016; Bampos et al., 2017), Au (Kuttiyiel et al., 2014; Wang Y. et al., 2016)] and Cu (Zheng et al., 2015; Wang G.W. et al., 2016) and choosing optimized support materials or heterostructural nanocomposites, such as carbon materials [e.g., XC-72, Graphene (G) and Reduced graphene oxide (RGO)] (Liu et al., 2015b; Yun et al., 2015; Zheng et al., 2015; Song et al., 2016), metal oxides (e.g., W₁₈O₄₉ and TiO₂) (Maheswari et al., 2013; Lu et al., 2014),

and transition metal carbides (e.g., Co₆Mo₆C₂, Co₃W₃C, and Fe₂MoC) (Li et al., 2014; Yan et al., 2015), have been applied to develop more active and durable ORR electrocatalysts. The enhanced ORR activities of these Pd-based electrocatalysts are believed to be due to the electronic structure modification of Pd by the alloying elements through the so-called strain and ligand effects or the electron transfer between the support materials and Pd nanoparticles named synergistic effect. For instance, alloying Pd with a transition metal with a smaller atom distance (e.g., Co, Ni, and Fe), the Pd–Pd interatomic distance decreases compared with pure Pd in the optimal alloy ratios (Wei et al., 2011; Rahul et al., 2014; Zhen et al., 2014; Yun et al., 2015; Bampos et al., 2017). Such a compressive strain of Pd–Pd causes a downshift of the d-band center of surface Pd, which consequently enhances the ORR activity through weakened bonding of oxygenated species, such as OH_{ads}. As well, the nanocomposites of Pd nanoparticles deposited on bimetallic carbide support materials (e.g., Co₆Mo₆C₂, GC-Fe₂MoC) show superior activity and stability for ORR in acid media. The excellent performance of Pd/bimetallic carbide catalysts may be attributed to the excellent electron-donating (synergistic effect) of bimetallic carbide to Pd, which not only facilitates the reduction of oxygen but also increases the linkage strength between Pd and bimetallic carbide (Li et al., 2014; Yan et al., 2015).

Recent studies have manipulated the morphologies and surface structure of Pd and Pd-M alloy nanoparticles to control the catalytic activity toward ORR (Xiao et al., 2009; Lu et al., 2014; Poon et al., 2014; Zhen et al., 2014; Srejjic et al., 2015). Lu et al. (2014) reported that strongly coupled Pd nanotetrahedron/tungsten oxide nanosheet hybrids exhibited not only surprisingly high activity but also superior stability for ORR in alkaline solutions. Such enhanced electrocatalytic activity and durability are associated with the increased number and improved catalytic activity of active sites, which is induced by the strong interaction between the Pd tetrahedrons and W₁₈O₄₉ nanosheet supports. Poon et al. (2014) showed that amorphous Pd nanoparticles synthesized by stepwise electroless deposition displayed superior ORR activity and stability compared with crystalline Pd nanoparticles and commercial Pt/C and Pd/C in KOH solution. Liu et al. (2015a) presented five-fold twinned Pd₂NiAg nanocrystals with a Ni-terminal surface, which demonstrated excellent electrocatalytic performance for ORR in alkaline media better than that of commercial Pt/C catalysts. Such, the morphology tuning of Pd and Pd-M nanoparticles are still one of significant strategies to control the catalytic activity toward ORR. It is worth noting that a considerable amount of studies has proven that the ORR activities of Pd and Pd-based nanomaterials are comparable to that of Pt/C in alkaline media (Poon et al., 2014; Rahul et al., 2014; Zhen et al., 2014; Yun et al., 2015; Doan et al., 2016; Zhang et al., 2016; Bampos et al., 2017). Furthermore, Pd or Pd-based electrocatalysts possess predominant stability in alkaline solution owing to a less corrosive environment for the catalysts and electrodes in alkaline fuel cells.

Transition metal Co or Co-decorated catalysts have recently attracted considerable attention because of their low cost and promising applications in oxygen electrode (Cheng et al.,

2017a,b; Su et al., 2017; Gong et al., 2018; Li et al., 2018). The Pd-Co alloy catalysts, in which the addition of transition metal Co could facilitate the dissociation of the O–O bonds (O₂) and thereby the produced Co–O_{ads} species might transfer to the Pd site to promote the electrochemical reduction of oxygen, have been reported to enhance the activity for ORR through adjusting the amount of Co alloyed, the Pd-Co particle size and the morphology (Wei et al., 2011; Arroyo-Ramírez et al., 2013; Antolini, 2014; Rahul et al., 2014; Yun et al., 2015; Huang et al., 2017). In the present study, Pd nanoparticles are implanted onto Co nanofilms to form Pd_x/Co-nanofilms/C composite electrocatalysts on an immiscible ionic liquid (IL)/water interface through a sequential reduction approach. The assembly of Pd atoms is affected by 2D Co nanofilm substrate, and the Pd nanoparticles exhibit a distorted crystalline structure and surface roughness. Thus, prepared Pd_x/Co-nanofilms/C catalysts have enhanced ORR catalytic activity in both acid and alkaline media. The designed Pd_x/Co-nanofilms/C catalysts exhibit superior stability compared to Pd/C catalyst in alkaline media after proper heat-treatment. And the structure–activity relationship between the ORR mass activity and the structure of Pd/Co-nanofilms was discussed.

EXPERIMENTAL

Materials Preparation and Physical Characterization

Pd_x/Co-nanofilms/C electrocatalysts were synthesized including the use of an immiscible imidazolium-based IL to achieve controllable metal nanostructured materials (Pd nanoparticles, Co nanofilms) (Chen et al., 2014) on the immiscible IL/water interface and a two-step reduction procedure (Chen et al., 2016). Firstly, a mixture of IL (6.00 g) and KBH₄ aqueous solution (20 mL, 50 mM) was stirred uniformly by ultrasonic assisted to form a highly dispersed, superfine IL/water interface solution and heated to 60°C. Another mixture of Co(Ac)₂ aqueous solution (20 mL, 5 mM) and certain amount of XC-72 (mass ratio of Co+Pd to XC-72: 1/4) pre-mixed ultrasonically for 30 min was then added into the solution drop by drop. The reacting solution was stirred continuously for another 40 min to prepare Co-nanofilms/C. Secondly, the deposition of Pd nanoparticles onto Co nanofilms was reduced under 40°C with KBH₄ (molar ratio of KBH₄/PdCl₂ = 10/1) as a reducing agent after rinsing PdCl₂ (atom ratio of Pd/Co: 3:1 or 2:1) for 30 min in Co-nanofilms/C colloid system. The reacting solution was then cooled down to room temperature after stirring continuously for 3 h. The whole process was carried out under a N₂ atmosphere. Finally, the resulting black powders were isolated by centrifugation and washed 3–4 times with ethanol. Thus-prepared catalysts were then dried at 30°C in a vacuum oven and stored for use. For comparison, Pd/C and Pd_xCo/C alloy catalysts were prepared in the same synthesis system. Differently, After the first step to form the IL/water interface solution, the mixture of precursor salt aqueous solution (PdCl₂ or Co(Ac)₂ and PdCl₂) and certain amount of XC-72 pre-mixed ultrasonically for 30 min was added to the solution drop by drop and stirring

continuously for 3 h under 60°C. Pd and Pd_xCo nanoparticles are deposited on XC-72 directly reduced by KBH₄. The molar ratio of KBH₄/PdCl₂ (or KBH₄/PdCl₂+Co(Ac)₂) = 10/1. IL: 1-octyl-3-methylimidazolium hexafluorophosphate [C₈min]PF₆.

The morphological features of the prepared samples was measured using a JEOL JEM-2100FEF transmission electron microscope (TEM) operating at a 200 kV accelerating voltage. Power samples for TEM were dispersed in ethanol by ultrasonic dispersion for 30 min and a drop of suspension was deposited on copper grids coated with thin carbon film. The data of X-ray photoelectron spectroscopy (XPS) was obtained on A Kratos Ltd. XSAM-800 spectrometer and fitted using the software XPSPEAK41 (Shirley function as baseline, Gauss–Lorentzian linearity fitting).

Electrochemical Measurements

Electrochemical measurements were performed on a CHI760A potentiostat with a three-electrode configuration. The as-prepared electrode, a Pt foil and a saturated calomel electrode (SCE) were applied as the working electrode, counter electrode and reference electrodes, respectively. The working electrode was prepared by coating the catalyst ink onto a glassy carbon rotating disk electrode (RDE, geometric area: 0.196 cm²), in which accurately 5 mg catalyst was introduced into 1 mL solution of Nafion in isopropyl alcohol (0.05 wt%) sonicated for 30 min to form uniform ink.

The cyclic voltammogram (CV) test was conducted in Ar-saturated 0.5 M H₂SO₄ or 0.1 M NaOH solution at a scan rate of 50 mV/s. The steady-state polarization curves for ORR were recorded in O₂-saturated electrolyte at a scan rate of 5 mV/s

and a rotation rate of 1,600 rpm. The working electrode was first cleaned by potential cycling between 0.042 and 1.342 V in 0.5 M H₂SO₄ solution or 0.0103–1.5103 V in 0.1 M NaOH at 500 mV/s and the reproducible CVs should be obtained before each electrochemical test. Usually, the cyclic voltammograms (CVs) in the first few cycles change significantly. Even, the electrochemical areas gradually increase along with the potential scans. After 10–20 cycles of 500 mV/s, the successive cycling would give relatively reproducible CVs. It should be pointed out that “reproducible” here does not mean “no change.” Such an electrochemical polish is necessary to get rid of the surface contaminations of catalyst particles and this fast electrochemical activation cannot alter the original structure of samples. The stability is evaluated by measuring the cumulative change loss of their electrochemical surface area after long-term continuous cycling under accelerated potential region in Ar-saturated electrolyte with a scanning rate of 50 mV/s. The measurements were carried out at room temperature (27 ± 1°C). All potentials are reported with respect to RHE and the current densities in the CVs are normalized by the Pd loading of the electrode.

RESULTS AND DISCUSSION

Physical Characterization

The fabrication of Pd_x/Co-nanofilms/C catalysts in this study relies on an interfacial synthesis technique by the use of an immiscible IL/water interface to achieve controllable metal nanostructured materials (Pd nanoparticles, Co-nanofilms) (Chen et al., 2014) and a sequential reduction process to implant

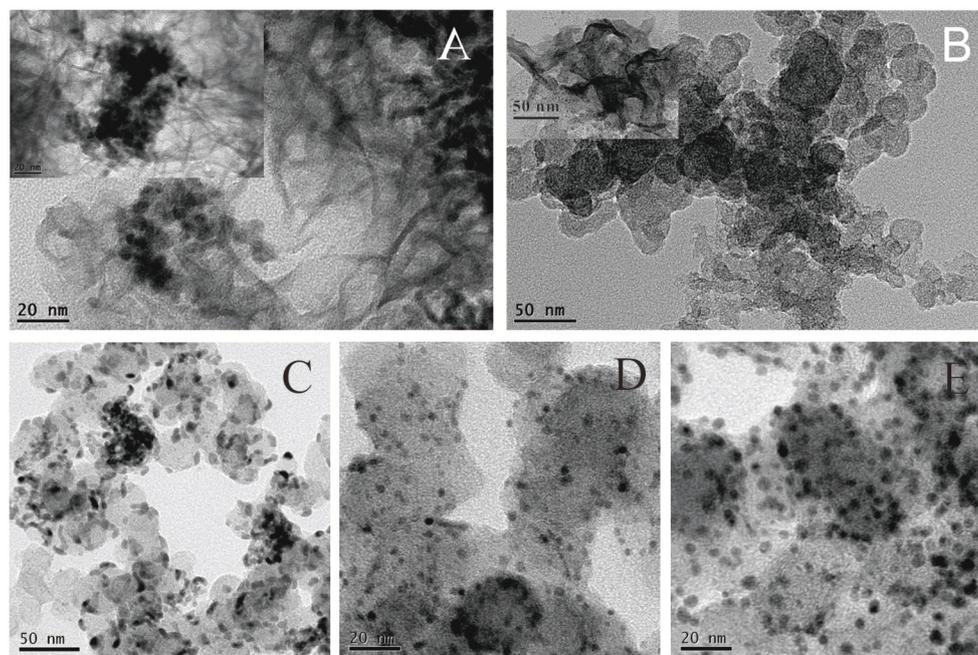


FIGURE 1 | Representative TEM images of the prepared (A) Pd/Co-nanofilms materials, (B) the Co-nanofilms/C; TEM images of the prepared catalysts of (C) Pd/C, (D) Pd₂Co/C, and (E) Pd₂/Co-nanofilms/C.

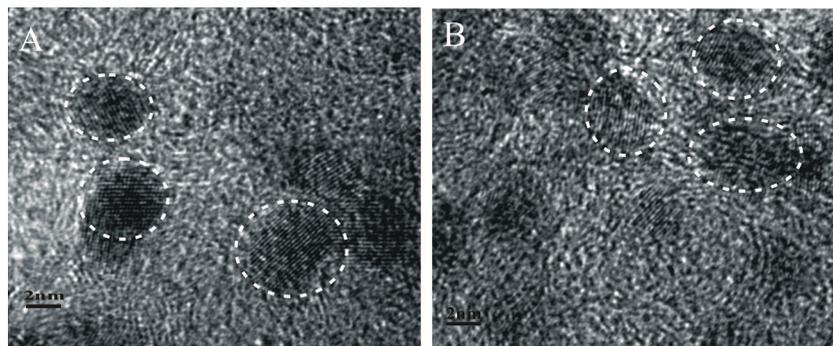


FIGURE 2 | Representative HRTEM images of the catalyst particles of (A) Pd₂Co/C and (B) Pd₂/Co-nanofilms/C.

Pd nanoparticles onto Co nanofilms (Chen et al., 2016). The representative TEM images of the non-carbon supported Pd/Co-nanofilms show that Co atoms assemble to Co-nanofilms with edges curled into nanotubes, and almost all Pd nanoparticles, which are seriously aggregated, are preferentially implanted onto the Co-nanofilms (**Figure 1A**; also see references Chen et al., 2014, 2016). To obtain highly dispersed Pd_x/Co-nanofilms/C catalysts, the treatments including pre-mixing Co salt and XC-72 support uniformly by ultrasonic and rinsing Pd precursors for 30 min in the second reduction process, respectively, are applied to conquer aggregation through the onsite reduction to deposit Co nanofilms on the XC-72 support and heterogeneous nucleation to implant Pd nanoparticles preferentially onto the Co nanofilms evenly. The **Figure 1B** give the TEM image of the Co-nanofilm/C materials, the Co nanofilms are difficult to be identified in the most TEM images except for very few edges. The TEM images in **Figures 1C–E** show that all of the prepared Pd, Pd₂Co, and Pd₂/Co-nanofilms particles have an average size of 5 nm and are relatively uniformly dispersed on carbon supports. High-resolution TEM (HRTEM) images of the selective catalyst particles of Pd₂Co/C and Pd₂/Co-nanofilms/C catalysts are shown in **Figure 2**. The composite materials of Pd₂/Co-nanofilms exhibit a marked distortion of crystal lattice and a rough surface, which are different from the Pd₂Co alloy particles mostly possessing a relatively fine crystalline structure with a smooth surface (observed in the particles signed by dashed circles). The Co nanofilms are also difficult to distinguish from the TEM and HRTEM images of Pd₂/Co-nanofilms/C catalysts, possibly because that the existence of XC-72 supports destroy long-range IL/water interface, correspondingly that the Co atoms cannot form continuously complete nanofilms and the Co nanofilms may instead break into pieces (also see reference Chen et al., 2016). The XRD responses of Pd/C, Pd_xCo/C and Pd_x/Co-nanofilms/C catalysts indicate that the diffraction peaks of Pd nanoparticles on Co nanofilms become broader compared with those of the Pd/C and Pd₂Co/C catalysts and the diffraction peaks of separated Co nanofilms are not resolved on the XRD patterns of Pd_x/Co-nanofilms/C catalysts (Chen et al., 2016). The XRD results confirmed that the

pre-deposited 2D Co nanofilms affect the assembly of Pd atoms and Pd nanoparticles with more complex crystalline are formed onto Co-nanofilms/C, correspondingly to modulate the electronic properties or geometric structure of surface Pd atoms.

The chemical states of Pd and Co on the catalytic surface were examined by XPS. **Figure 3** presents the XPS responses of the prepared Pd/C, Pd₂Co/C and Pd₂/Co-nanofilms/C catalysts. The Pd states for all studied samples consist of Pd metal (Pd⁰) as well as Pd oxide (Pd²⁺) by fitting the Pd 3d in the binding energy region between 330 and 352 eV using Gauss–Lorentzian fitting methods (**Figures 3A–C**) (Oishi and Savadogo, 2013; Stefanov et al., 2015; Yun et al., 2015). Different from Pd₂Co/C catalyst with higher binding energy 336.06 eV for Pd 3d_{5/2} with respect to the value 335.96 eV for Pd/C as a result of the effect of alloying Pd with Co (Stefanov et al., 2015; Yun et al., 2015), the binding energy for Pd 3d_{5/2} of the prepared Pd₂/Co-nanofilms/C catalyst was 336.02 eV medially. The corresponding peak areas can be used to estimate the relative Pd⁰/Pd²⁺ atom ratios in the near-surface region of each catalyst. The estimated near-surface Pd⁰/Pd²⁺ ratios are ~0.91 and 0.89 for the Pd₂Co/C and Pd₂/Co-nanofilms/C catalysts, respectively, which are much higher than the 0.55 ratio for Pd/C. These observations confirm the Co nanofilms-induced modification of electronic properties or geometric structure of Pd nanoparticles. The Co 2p_{3/2} XPS peaks in **Figures 3D,E** show that Co states of the exposed Co atoms consist of Co metal (Co⁰) and Co oxides (Co²⁺) (Ali et al., 2014; Yun et al., 2015). After the two shakeup satellite peaks associated with the Co (2p) line of Co²⁺ are taken into account (Xiao et al., 2015), the major Co 2p_{3/2} XPS peaks with the typical binding energy around 782 eV correspond to Co²⁺ oxides. This result suggests that a majority of the exposed Co atoms have been oxidized during post-processing. The alloying effect including the addition of an easily oxidized metal (e.g., Co or Ni), which can preferentially combine with oxygen to prevent the oxidation of noble metals, may explain the higher Pd⁰/Pd²⁺ ratios for Pd₂Co/C and Pd₂/Co-nanofilms/C catalysts calculated by XPS peak areas (Chen et al., 2011; Jiang et al., 2015). Although the Co nanofilm substrate cannot be resolved from the responses of TEM and XRD of the carbon supported

sample, the measured results of Co nanofilms (**Figure 1A**, also see Chen et al., 2016) and the Co XPS profile of the Pd₂/Co-nanofilms/C catalyst verify the successful fabrication of Co nanofilms.

Cyclic Voltammetric Measurement

A clean surface is important to study the characteristic and catalytic active area of an electrocatalysts. We tested the CVs repeatedly in the different potential regions by changing the cathodic scan potentials. Take the Pd-Co samples for example (**Figure 4**), the H adsorption/desorption reaction on the surface of Pd₃Co/C and Pd₃/Co-nanofilms/C catalysts under cathodic potential (0.0103 V (Vs RHE) becomes the main reaction in 0.1 M NaOH solution, in which H absorption peak cannot take place. Similarly, H absorption peak is suppressed under cathodic potential [0.042 V (Vs RHE)] in 0.5 M H₂SO₄. And the H absorption become the main process along with reducing the cathodic potentials, covering the adsorption/desorption peaks (seen the red and blue lines in **Figure 4**). Sun et al. studied the CVs on the nm-Pd film formed by the 6 nm Pd crystal and compared with those of the bulk Pd metal electrode in 0.5 M H₂SO₄ solution (Cai et al., 1999, **Figures 4, 6** in the reported paper). The H adsorption/desorption reaction on the surface of nm-Pd electrode take place under lower cathodic potential [0.032 V (Vs RHE)] without H absorption. However, on the bulk Pd metal, the adsorption/desorption current peaks could be obviously observed under high cathodic scan potential [(0.172 V (Vs RHE)]. When the cathodic potential was reduced to [0.032 V (Vs RHE)], the H absorption becomes the main process covering the adsorption/desorption peaks. The fact that H dissolution into Pd causes larger peak in the hydrogen potential region is discussed in reported paper (Zhang et al., 2007; Lee et al., 2015). As for the CV scans in our measurement, the CV characteristics are consistent with those results reported. And the H adsorption/desorption reaction and H absorption process can be resolved clearly under different cathodic potential regions. Those results indicate a clean surface of Pd-based catalysts in our experiment.

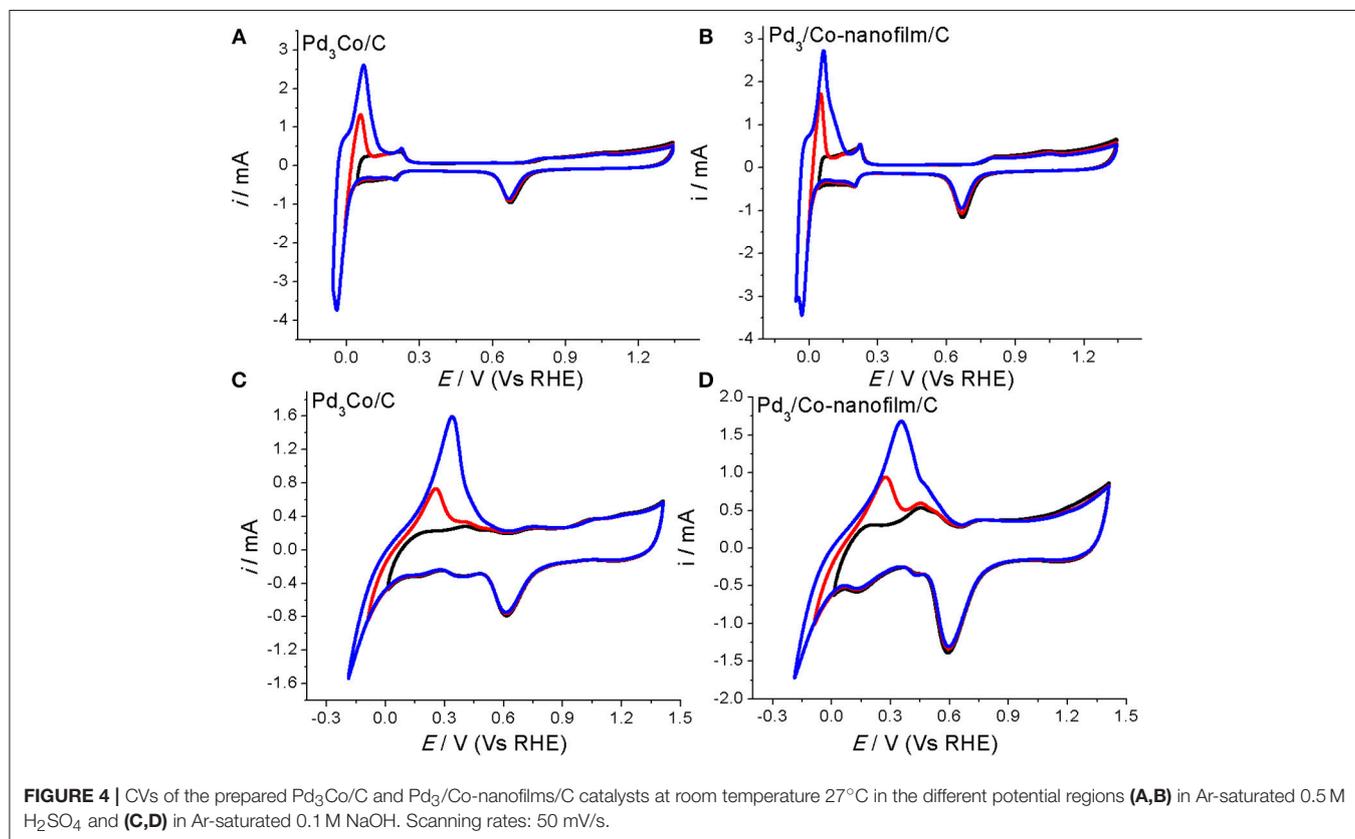
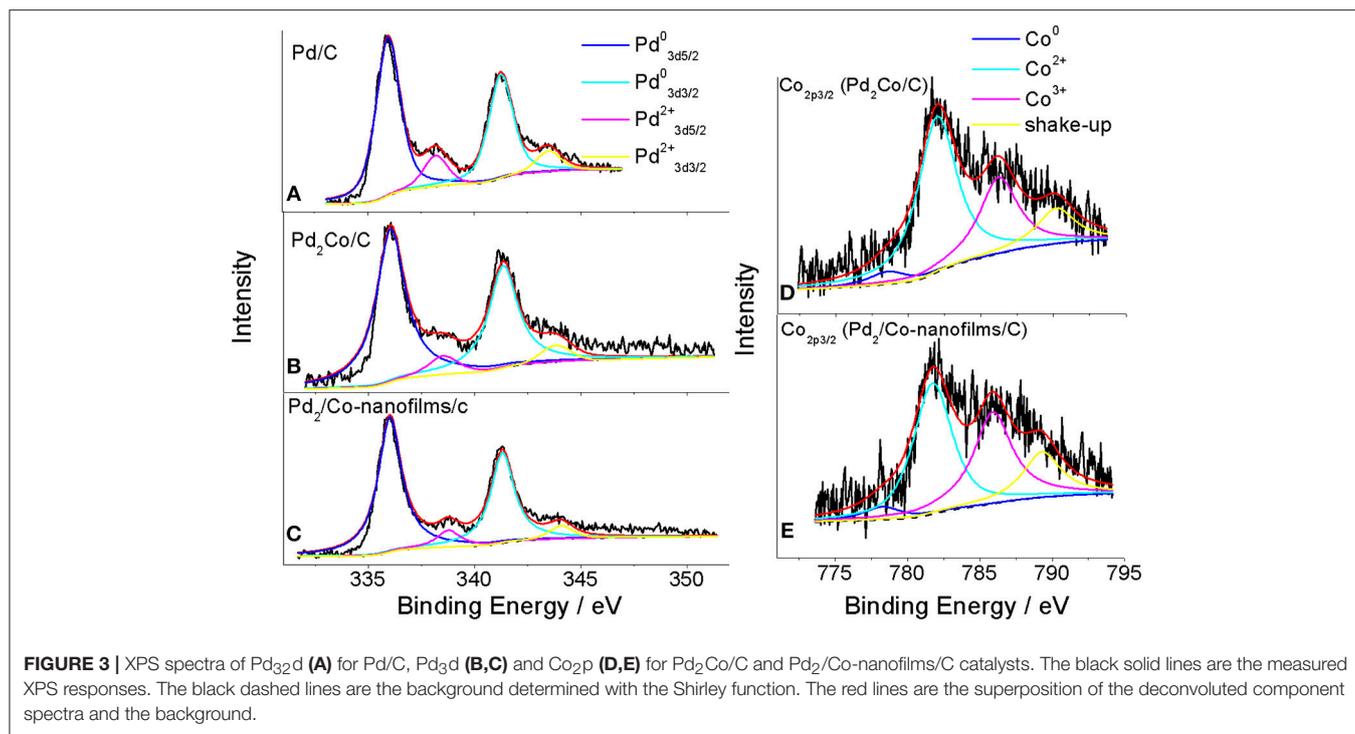
Figure 5 gives the cyclic voltammograms (CVs) and the corresponding voltammetric peaks associated with the reduction desorption of the oxygenated adsorbates of the prepared Pd/C, Pd_xCo/C, and Pd_x/Co-nanofilms/C catalysts in argon-saturated H₂SO₄ solution (**Figure 5A**) and NaOH solution (**Figure 5B**). It can be seen that the composite Pd_x/Co-nanofilms/C catalysts exhibit evidently larger electrochemical areas compared with the Pd_xCo/C catalysts of the same Pd/Co ratios, particularly in alkaline media. The enlarged catalytic areas of Pd_x/Co-nanofilms/C catalysts are attributed to the rough surface of Pd nanoparticles with a distorted crystal lattice measured from HRTEM and XRD (**Figures 2, 3**). In H₂SO₄ solution, the electrochemical areas increase with the addition of Pd content both for the Pd_xCo/C alloy and Pd_x/Co-nanofilms/C catalysts. However, in NaOH solution, the Pd_xCo/C alloy catalysts cannot release all of the active sites and the catalytic areas are not absolutely dependent on Pd content, such as more difference of electrochemical areas

between the Pd_xCo/C and the Pd_x/Co-nanofilms/C catalysts with the same Pd/Co atom ratios and the Pd₃Co/C catalyst exhibits the smallest active area. These characteristics may be related to the existence form of Co atoms in Pd-based materials and the electrolyte properties. In alkaline media, exposed Co atoms are oxidized in the electrochemical scans. The Co oxidation near Pd in Pd_xCo alloy may cover some active sites of surface Pd, corresponding to the reduced active areas. However, in the designed composite structure of Pd/Co-nanofilms, the oxidation of segregated Co nanofilm substrate may almost not affect the surface active centers of Pd nanoparticles. The variation in peak potentials for the reduction desorption of the oxygenated adsorbates (E_o) is inconsistent in acid and alkaline media, indicated by the dashed dividing lines through the peak position of Pd/C. The results predict the different regular patterns of ORR activity in acid and alkaline media.

ORR Activity and Stability Measurements

The electrocatalytic ORR performances of the prepared Pd_x/Co-nanofilms/C catalysts are investigated using a rotating disk electrode at a rotation rate of 1,600 rpm in O₂-saturated 0.5 M H₂SO₄ and 0.1 M NaOH electrolyte, respectively. We technically repeat the experiment 3–5 times to get consistent results. **Figures 6A,D** show the ORR polarization curves, in which the curves for the prepared Pd/C and Pd_xCo/C alloy catalysts are also given for comparison. The Pd specific area and mass activities, which are acquired by normalizing the kinetic current (I_k) by the electrochemical surface area of Pd (ECSA, determined from the oxygen discharges in CVs given in **Figure 5**) and by the Pd loading on the electrode, are presented in **Figures 6B,C,E,F** (the inset). The I_k was calculated from the steady-state polarization curves (**Figures 6A,D**) using Koutecky–Levich equation ($I_k = I \times I_L / (I_L - I)$), where I and I_L are the measured current and the corresponding limiting diffusion current, respectively.

The steady-state polarization curves display a diffusion-limiting current region (from 0.242 to 0.742 V in H₂SO₄ solution and from 0.31 to 0.81 V in NaOH solution) and a mixed kinetic-diffusion control region (from 0.742 to 0.842 V in H₂SO₄ solution and from 0.810 to 1.010 V in NaOH solution). The half-wave potential ($E_{1/2}$) of the Pd₃/Co-nanofilms/C (0.799 V) is higher than that of Pd/C (0.782 V) and Pd₃Co/C alloy (0.788 V) catalysts in acid solution. This regular pattern is also found in alkaline solution with $E_{1/2}$ values of 0.910, 0.892, and 0.896 V for the Pd₃/Co-nanofilms/C, Pd/C, and Pd₃Co/C alloy catalysts, respectively. The Pd/C ORR activity is equal to that of reported paper (Wang et al., 2017). The Pd specific area activity profile in acid solution (**Figure 6B**) shows slightly enhanced activities of the Pd_x/Co-nanofilms/C catalysts compared with Pd_xCo/C catalysts. However, in alkaline solution (**Figure 6E**) the specific activities show the exact opposite regular. Maybe in the acid solution the surface Pd atoms exist in pure Pd along with accelerated Co dissolution. Such, the Pd_xCo/C alloy catalysts cannot display the enhanced specific activity. While, in alkaline solution the Pd_xCo/C alloying effect enhances Pd intrinsic



activity (Yun et al., 2015; Bampos et al., 2017). As indicated by the mass activity profiles (Figures 6C,F) and the corresponding comparison under given potentials among the prepared catalysts,

the Pd₃/Co-nanofilms/C catalyst shows the highest mass activity in both acid and alkaline solution. The results reveal that the Pd_x/Co-nanofilms/C catalysts possess a superior catalytic

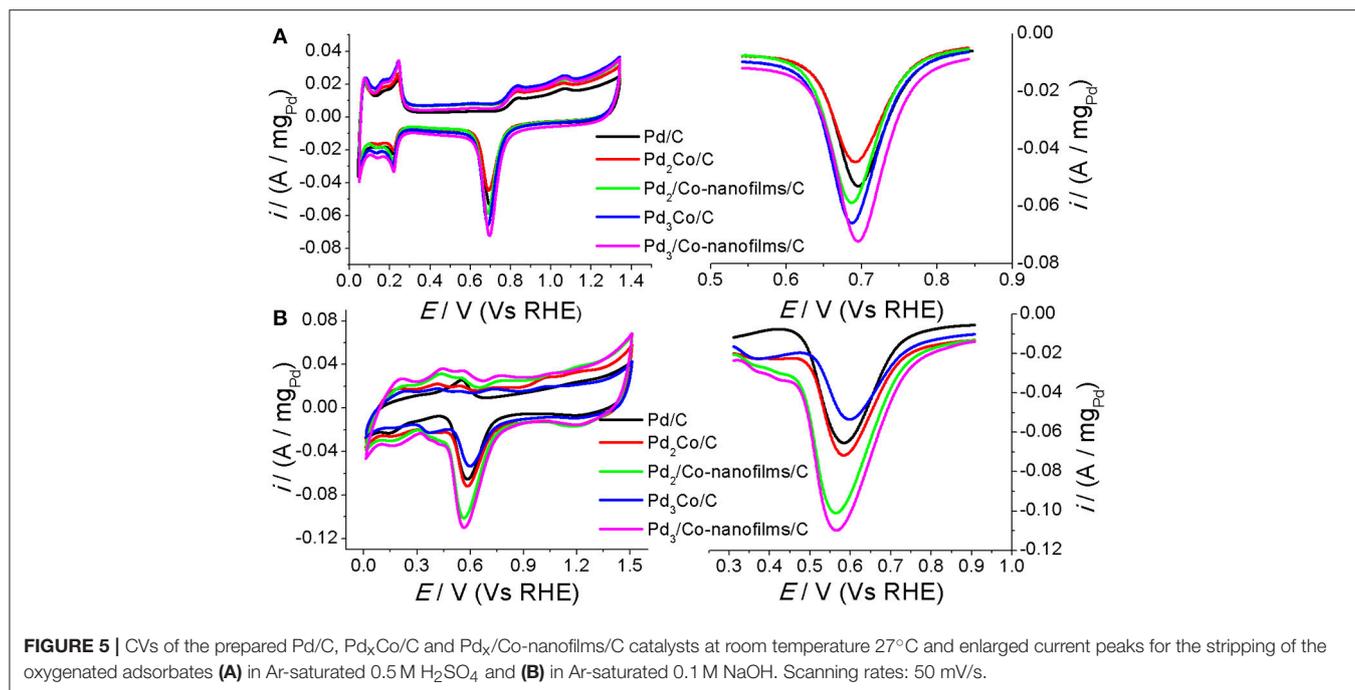


FIGURE 5 | CVs of the prepared Pd/C, Pd_xCo/C and Pd_x/Co-nanofilms/C catalysts at room temperature 27°C and enlarged current peaks for the stripping of the oxygenated adsorbates (A) in Ar-saturated 0.5 M H₂SO₄ and (B) in Ar-saturated 0.1 M NaOH. Scanning rates: 50 mV/s.

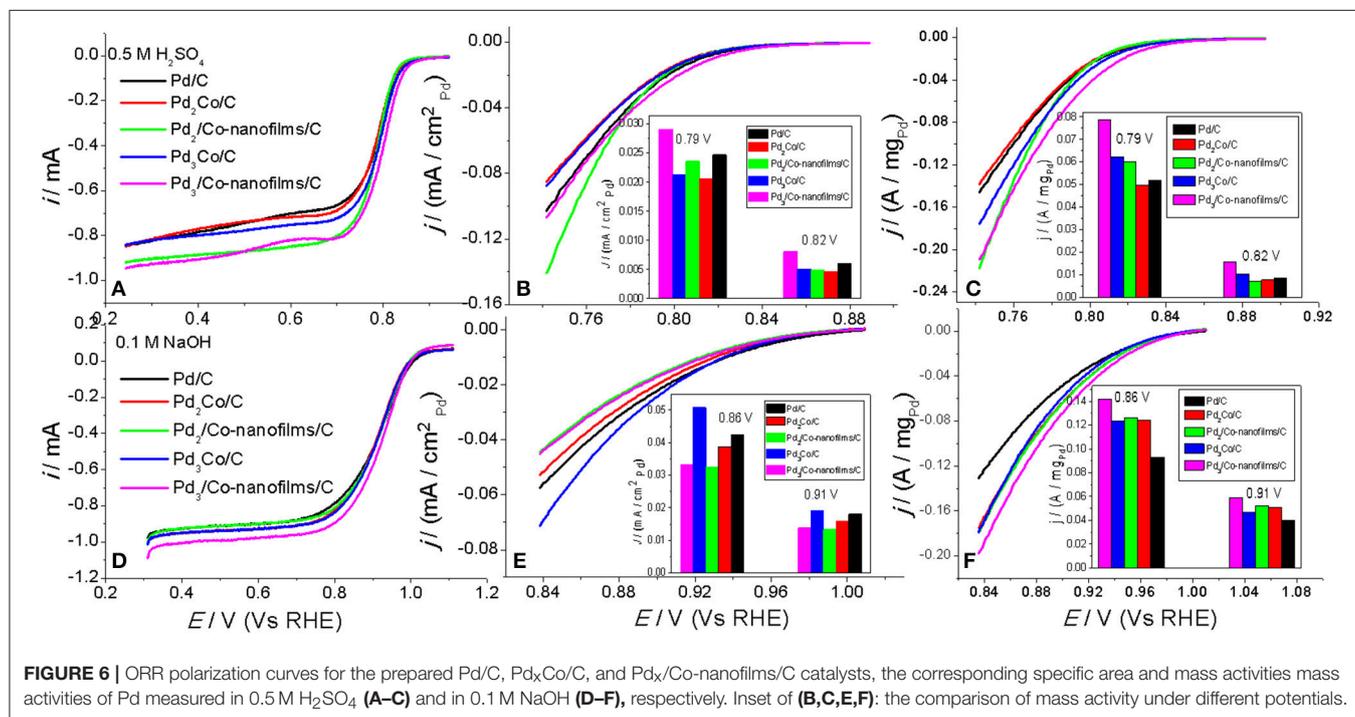


FIGURE 6 | ORR polarization curves for the prepared Pd/C, Pd_xCo/C, and Pd_x/Co-nanofilms/C catalysts, the corresponding specific area and mass activities mass activities of Pd measured in 0.5 M H₂SO₄ (A–C) and in 0.1 M NaOH (D–F), respectively. Inset of (B,C,E,F): the comparison of mass activity under different potentials.

performance. Previous theoretical and experimental works are focus on the methods to down-shift the d-band center of noble metals (e.g., Pd and Pt) by alloying a precious metal with the transition metal with a smaller interatomic distance (e.g., alloy structure, core-shell structure, and so on), thereby weakening the adsorption of oxygenated intermediates and being beneficial to improve ORR activity (Wei et al., 2011; Jiang

et al., 2015; Yun et al., 2015). In fact, it is well know that the catalytic process happens on the surface of the catalysts. Then a large specific surface area is an effective factor to reduce the amount of the precious metal. The significantly increased catalytic area of the Pd_x/Co-nanofilms/C catalysts (showed by CV scans in Figure 5) should be the reason why this structure exhibit enhanced ORR activity compared with Pd_xCo/C alloy

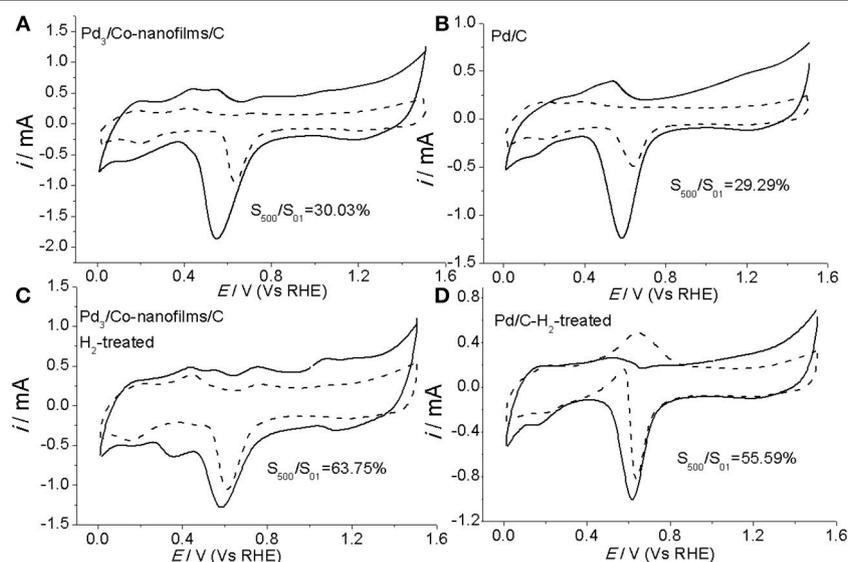


FIGURE 7 | CVs of Pd₃/Co-nanofilms/C (**A,C**) and Pd/C catalysts (**B,D**) before (solid) and after (dashed) accelerated by electrochemical degradation tests under repeating potential cycling in 0.1 M NaOH.

and Pd/C catalysts. Besides, Pd surface roughness and oxidation degree in the electrochemical process can modify the ORR activity.

As shown in **Figures 6C,F**, the mass activity of the Pd_x/Co-nanofilms/C catalysts exhibit different dependence on the Pd/Co atom ratios in acid and alkaline media. The Pd_xCo/C alloy catalysts also display the same behavior. In 0.5 M H₂SO₄ solution, the ORR mass activities of Pd improve remarkably with increasing the Pd/Co atom ratios. However, the mass activities are less dependent on the Pd/Co atom ratios in 0.1 M NaOH solution. These regular patterns predict that appropriate addition of Pd content is beneficial to improve ORR activity both in acid and alkaline media, particularly in former media.

Except for the catalytic activity, the long-term stability is another important parameter that determines the practical application of a specific ORR electrocatalyst. The stability of the prepared Pd₃/Co-nanofilms/C and pure Pd/C catalysts are evaluated by measuring their electrochemical surface areas from the desorption of the oxygenated adsorbates after extended potential cycling under the accelerated potential region between 0.0103 and 1.510 V (Vs RHE) in Ar-saturated 0.1 M NaOH with a scan rate of 50 mV/s. **Figure 7** gives the initial and final CVs after 500 cycles of the Pd₃/Co-nanofilms/C and Pd/C catalysts before and after heat-treatment in H₂ atmosphere. The stability of the Pd₃/Co-nanofilms/C catalyst is comparable with that of pure Pd/C catalyst before heat-treatment, in which self-existent Co-nanofilm substrate do not cause the violent degradation of the catalytic area (**Figures 7A,B**), owing to relatively lower corrosion of transitional metal (e.g., Co and Ni) in alkaline media and the enhanced effect by the surface Pd nanoparticles. After proper heat-treatment in H₂ atmosphere at 200°C, both Pd₃/Co-nanofilms/C and Pd/C catalysts exhibit decreased variations in potential CVs after long-time potential cycling. Moreover, the

Pd₃/Co-nanofilms/C catalyst exhibits greater cycling stability than pure Pd/C catalyst. One of the reasons for the relatively superior stability of the prepared Pd₃/Co-nanofilms/C after heat-treatment might be due to the higher coordination of surface Pd atoms. In addition, the heat-treatment promotes a little amount of Co atoms into Pd crystal lattice to increase atomic bond strength, which can further enhance stability of the Pd₃/Co-nanofilms/C catalyst.

CONCLUSION

Applying the interfacial synthesis technique on an immiscible ionic liquid (IL)/water interface, Pd nanoparticles with an average size of 5 nm are implanted onto 2D Co-nanofilm substrate to form the composite Pd_x/Co-nanofilms/C catalysts. The TEM (HRTEM), XRD, XPS, and CVs results suggest that the assembly of Pd atoms may be affected by the Co nanofilms, in which the Pd nanoparticles show a marked distortion of crystal lattice and surface roughness. These Pd_x/Co-nanofilms/C electrocatalysts exhibit enhanced activity for ORR compared with Pd/C and Pd_xCo/C catalysts in both acid and alkaline solutions, in which the Pd₃/Co-nanofilms/C catalyst displays the highest ORR mass activity. The superior ORR mass activities of the fabricated Pd_x/Co-nanofilms/C catalysts may be attributed to their larger catalytic areas, which are conferred by the rough surface of Pd nanoparticles with a distorted crystal lattice, and the synergistic effect between the surface Pd atoms and the 2D Co nanofilm substrate. Furthermore, by using proper heat-treatment methods, the Pd_x/Co-nanofilms/C catalysts exhibit improved cycling stability compared with pure Pd/C catalyst after extended potential cycling. This study can predict that deposition of Pd-M alloy nanoparticles onto 2D transition metal nanofilms would

further optimize the electrochemical activity and stability of Pd-based catalysts.

AUTHOR CONTRIBUTIONS

YC and BL designed experiments. LA carried out experiments. JS carried out the electrochemical experimental. YC, JC, and JY analyzed experimental results. LA and YC wrote the manuscript.

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Conflict of Interest Statement: The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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