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Entropy generation investigation of MHD Ag- and $Au-H_2O$ nanofluid above an exponential porous stretchable surface with thermal radiation and stagnation point flow

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The current study presents an entropy generation investigation of magnetohydrodynamic Ag- and Au- H_2O nanofluid flows induced by an exponential stretchable sheet implanted in porous media accompanying suction/injection and heat radiation impact. Moreover, the stagnation point flow and silver and gold nanoparticles are considered. The consequences of ohmic heating and thermal radiation are also included as part of the heat transport examination. A physical process is transformed into a set of mathematical expressions using mathematical concepts, which can then be further simplified by using the necessary variables. Considering numerous physiological factors of interest, exact solutions for velocity and temperature profiles are calculated. Graphs and numerical tables are utilized to examine how different physical entities affect the distribution of velocity, temperature, and entropy. It is noted that enhancing the values of Ω reduces entropy inception. It is observed that the entropy inception field gains due to an increment in Ec_{rt} .

KEYWORDS

thermal radiation, entropy inception, ohmic heat, magnetic field, stagnation point flow

1 Introduction

Entropy is defined as a gauge of disorder inside a system and its surroundings or a measure of progress toward thermodynamic equilibrium under the scope of thermodynamics. Working with a thermodynamics process, an entropy generation investigation is essential since entropy calculates the effectiveness of every engineered thermofluid mechanism. The second law of thermodynamics determines the randomness of any system. According to current research, the second law of thermodynamics is a significant tool for calculating the entropy of any system. Entropy inception has considerable fascinating application in the engineering and chemical industry such as extrusion procedures, lubrication phenomena, and schemes of geothermal energy, thermal mechanisms, heat management, and power production (Abbasi et al., 2021). Bejan (1979) was the first to introduce the concept of entropy production inside the flowing fluid and heat exchange mechanism. Later on, many researchers discussed entropy generation inside fluid and heat transport frameworks. Abbasi et al. (2021) studied the significant entropy inception with ohmic heating and thermal radiation effects of a viscoelastic nanofluid on a lubricated disk. Entropy production inside the MHD flow between porous media was discussed by Rashidi and Freidoonimehr (2014). Hayat et al. (2021) described the entropy in Newtonian nanofluid flow provoked by a curved stretchable sheet. Entropy inception within a Casson nanoliquid by a stretched surface soaked in porous media considering many impacts was investigated by Mahato et al. (2022). Wang et al. (2022) studied the Darcy-Forchheimer nanofluid for irreversibility inception. The entropy production in the Darcy-Forchheimer fluid in the presence of ohmic heat was scrutinized by Khan et al. (2022). Tayebi et al. (2021) examined the entropy and thermo-economics inside a convective nanofluid with the MHD effect. Afridi et al. (2018) analyzed the consequences of frictional and ohmic heating to find the entropy inception inside the used problem. Sithole et al. (2018) investigated the irreversibility of MHD nanofluid flow provoked by a stretchable surface for viscous dissipation influence. The impact of entropy inception inside the nanofluid with several effects is addressed in Noghrehabadi et al. (2013); Bhatti et al. (2017); and Abd El-Aziz and Afify (2019).

Despite the fact that a variety of approaches are used to promote heat transport, low thermal quality is a significant barrier in development of energy-efficient heat transfer fluids, which are in high need for a variety of industrial applications. The thermal capabilities of energy-carrying liquids are accountable for boosting the exchange of heat in a system. As a result, insufficient thermal conductivity is a disadvantage of conventional fluids, such as glycol, oil, water, and ethylene, in promoting the properties and efficiency of various engineered electronic devices. Integrating a fraction of nanometal particles within ordinary fluids is a novel way to improve the thermal conductivity of traditional liquids, which are known as nanofluids. The first time a nanofluid was used by adding nano-sized metallic particles into a conventional fluid was in 1995 by Choi (1995). Such kinds of nanofluids significantly enhance heat transport properties. After that, many scientists investigated the heat exchange rate of a nanofluid with several impacts. Prasannakumara (2021) analyzed the MHD Maxwell nanofluid provoked by a stretched surface

by applying a numerical method. The influence of thermal radiation on the Casson nanofluid by shrinking/stretching walls was observed by Mahabaleshwara et al. (2022). The consequence of dissipation and radiation entities on an MHD bioconvective nanoliquid due to a stretching sheet was discussed by Neethu et al. (2022). B Awati et al. (2021) used the Haar wavelet method to study nanofluid flow with a nonlinear stretchable surface along with mass and energy transport. The impact of nanofluid flow provoked by a stretching sheet along with hydromagnetics is scrutinized by Manzoor et al. (2022). The impact of emerging entities on a nanofluid is presented in Oztop and Abu-Nada (2008); Khan and Pop (2010); Hamad (2011); Yacob et al. (2011); Noghrehabadi et al. (2012); Rohni et al. (2012).

Motivated by the aforementioned studies and interesting applications, entropy inception is calculated inside the magnetohydrodynamic nanofluid flow by incorporating Ag and Au nanoparticles on an exponentially stretchable surface with stagnation point flow, porous wall, and ohmic heating. Furthermore, the Bejan number and energy transport investigation are carried out along with thermal heating. The closed form solutions are acquired by utilizing hypergeometric functions to visualize the impact of numerous emerging parameters on the velocity field, temperature field, local skin friction, Nusselt number, and the chaos due to different effects in the used problem. Additionally, numerical tables and graphs are displayed.

2 Problem statement

A two-dimensional, laminar, incompressible, steady flow of an Ag/Au-water MHD nanofluid provoked by an exponentially stretchable surface immersed in porous media with different body forces has been carried out. The impact of ohmic heating and thermal radiation is also considered part of the heat transfer study. The extending sheet is placed along the *x*-axis in the flow path, whereas the *y*-axis is assumed normal to the sheet. **Figure 1** shows that the fluid is in the $y \ge 0$ space. Considering a velocity of $u = u_{re}e^{x/L_c}$, the surface is pulled throughout the *x* dimension. In addition, the magnetic field (B_0) is introduced toward the flowing fluid in a normal direction. The basic equations that regulate the used fluid flow are as shown as follows (Rashidi and Freidoonimehr, 2014):

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial v}{\partial y} = \frac{\mu_{sf}}{\rho_{sf}}\frac{\partial^2 u}{\partial y^2} + u_{sp}\frac{\partial u_{sp}}{\partial x} - \frac{\sigma_{sf}B(x)^2}{\rho_{sf}}\left(u - u_{sp}\right) - \frac{\mu_{sf}}{\rho_{sf}k}\left(u - u_{sp}\right), \quad (2)$$

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in which B(x) = magnetic entity; u, v denote the velocity portions in the *x* and *y* directions, respectively, $\rho_{sf} =$ density; μ_{sf} is the dynamic viscosity; the thermal diffusivity is expressed by α_{sf} ; the specific heat capacitance is $= (\rho c_p)_{sf}$; and v_{sf} is the kinematic viscosity of the nanofluid. The thermal conductivity can be expressed as follows (Rashid et al., 2017):

$$\begin{pmatrix} \rho c_{p} \end{pmatrix}_{sf} = +\phi (\rho c_{p})_{sf} + \left(\left(\rho c_{p} \right)_{hf} \cdot 1 - \left(\rho c_{p} \right)_{hf} \phi \right), \\ \alpha_{sf} = \frac{k_{sf}}{(\rho c_{p})_{sf}}, \quad \mu_{sf} = \frac{\mu_{hf}}{(1 - \phi)^{2.5}}, \\ \rho_{sf} = \phi (\rho_{sf}) + (1\rho_{hf} - \rho_{hf}\phi), \quad v_{sf} = \frac{\mu_{sf}}{\rho_{sf}}, \\ \frac{\sigma_{sf}}{\sigma_{hf}} = \frac{\left(3\frac{\sigma_{sf}}{\sigma_{hf}}\phi - 3\phi \right)}{\left(\phi - \frac{\sigma_{sf}}{\sigma_{hf}}\phi \right) + \left(\frac{\sigma_{sf}}{\sigma_{hf}} + 2 \right)} + 1, \\ k_{sf} = \frac{\left(k_{hf}k_{sf} + 2k_{hf}^{2} \right) - 2\left(k_{hf}^{2}\phi - k_{sf}k_{hf}\phi \right)}{\left(k_{sf} + 2k_{hf} \right) + \left(k_{f}\phi - k_{sf}\phi \right)},$$

$$(3)$$

In Eq. 5, k_{sf} =thermal conductivity; σ_{sf} =electrical conductivity; $(\rho c_p)_{hf}$ and ρ_{hf} are the effective heat capacity and density, respectively; and ϕ is the nanoparticle volume ratio of the nanofluid. k_{hf} =thermal conductivity and σ_{hf} =electrical conductivity of the host fluid. The appropriate boundary criteria of the aforementioned model are as follows (Bilal et al., 2017):

$$\begin{array}{l} u = u_{re} e^{x/L_c}, \quad v = v_{wmt} \quad \text{at} \quad y = 0, \\ u \to u_{sp} = u_{re} e^{x/L_c} \quad \text{as} \quad y \to \infty. \end{array} \right\}.$$

$$(4)$$

The accompanying similarity variables have been established to non-dimensionalize the basic equations and boundary





conditions (Bilal et al., 2017):

$$\eta = y \left(\frac{u_{rf}}{2v_{hf}L_c} \right)^{1/2} e^{x/2L_c}, v = -\left(\frac{u_{rf}v_{hf}}{2L_c} \right)^{1/2} e^{x/2L_c} (f + \eta f'), u = u_{re} e^{x/L_c} f'.$$
 (5)







Expression Eq. 5 reduces Eq. 2 into a dimensionless form and is given as

$$f''' + \chi_1 \chi_2 f f'' + 2\chi_1 \chi_2 A_{vr}^2 - 2\chi_1 \chi_2 f'^2 - \chi_1 M_{egn} f' + (K_{pr} A_{vr} - K_{pr} f') = 0, \quad (6)$$

(S < 0)1.9 $A_{vr} = 0.1$ S = -0.3= 0.1 φ 1.8 $M_{egn} = 0.0, 0.3, 0.5$ -f "(0) 1.7 1.6 Solid line: Ag-Water Dashed line: Au-Water 0.1 0.2 0.3 0.4 0.7 0.5 0.6 0 K FIGURE 7 Outcome of M_{egn} on -f''(0).

and the boundary conditions are

$$\begin{cases} f(\eta) = S, & f'(\eta) = 1, & \text{at} \quad \eta = 0, \\ f'(\eta) \to \frac{u_{sp}}{u_{re}} = A_{vr} & \text{as} \quad \eta \to \infty. \end{cases}$$

$$(7)$$



Outcome of suction/injection on -f''(0).



In Eqs. 6, 7,

$$\chi_{2} = \left(1 - \phi + \phi \frac{\rho_{sf}}{\rho_{hf}}\right), \quad S = -\left(\frac{2L_{c}}{u_{re}v_{hf}}\right)^{1/2} e^{-x/2L} v_{w},$$

$$M_{egn} = \frac{2u_{rf}\sigma B_{0}^{2}}{\rho},$$

$$\chi_{1} = (1 - \phi)^{2.5}, \quad K_{pr} = \frac{u_{re}k_{0}}{L_{c}v_{hf}}, \quad u_{sp}$$
the stagnation – point flow velocity.
$$\left.\right\}$$
(8)

the stagnation – point flow velocity,

 \boldsymbol{u}_{re} the reference velocity,





where K_{pr} is the permeability parameter and M_{egn} = the Hartmann number. The closed form solution of such a kind of equation was introduced by Chakrabarti and Gupta, (1979):

$$f(\eta) = \lambda_1 + \lambda_2 e^{-\Psi \eta}.$$
 (9)

By solving Eqs. 7, 8,

$$f(\eta) = \left(\frac{1 - e^{-\Psi\eta}}{\Psi}\right) + S.$$
 (10)







$$\Psi = \frac{1}{2}\chi_1\chi_2S + \frac{1}{2}\sqrt{\chi_1^2\chi_2^2S^2 - 8A_{vr}^2\chi_1\chi_2 - 4A_{vr}\chi_1M_{egn+\xi}},$$
 (11)

$$\lambda_1 = \frac{1}{\frac{1}{2}\chi_1\chi_2 S + \frac{1}{2}\sqrt{\chi_1^2\chi_2^2 S^2 - 8A_{vr}^2\chi_1\chi_2 - 4A_{vr}\chi_1M_{egn+\xi}}} + S, \quad (12)$$





$$\lambda_{2} = -\frac{1}{\frac{1}{2}\chi_{1}\chi_{2}S + \frac{1}{2}\sqrt{\chi_{1}^{2}\chi_{2}^{2}S^{2} - 8A_{vr}^{2}\chi_{1}\chi_{2} - 4A_{vr}\chi_{1}M_{egn+\xi}}},$$
(13)

$$\xi = -4A_{vr}4K_{pr} + 8\chi_1\chi_2 + 4\chi_1M_{egn} + 4K_{pr}, \qquad (14)$$

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where Ψ , λ_1 , and λ_1 are constants with $\Psi > 0$. After substituting **Eqs. 11–13** in **Eq. 9**, the solution of the velocity filed is found as

$$f(\eta) = \left(\frac{1}{\frac{1}{2}\chi_{1}\chi_{2}S + \frac{1}{2}\sqrt{\chi_{1}^{2}\chi_{2}^{2}S^{2} - 8A_{\nu r}^{2}\chi_{1}\chi_{2} - 4A_{\nu r}\chi_{1}M_{egn+\xi}}}{\left(1 - e^{\frac{1}{2}\chi_{1}\chi_{2}S + \frac{1}{2}\sqrt{\chi_{1}^{2}\chi_{2}^{2}S^{2} - 8A_{\nu r}^{2}\chi_{1}\chi_{2} - 4A_{\nu r}\chi_{1}M_{egn+\xi}\eta}}\right) + S,$$
(15)

The skin friction at the sheet is calculated as follows:

$$C_f = \frac{\tau_w}{\rho u_w^2} = \frac{f^{\prime\prime}(0)}{R e_x^{1/2} \chi_1}, \quad R e_x^{-1/2} \chi_1 C_f = f^{\prime\prime}(0).$$
(16)

Here, the Reynolds number is shown by $Re_x = \frac{xu_w}{v}$, and the stress over the wall $= \tau_w = \mu_n f\left(\frac{\partial u}{\partial y}\right)_{v=0}$.

3 Heat transfer analysis

Heat transport analysis is carried out in this portion. Additionally, ohmic heating and thermal radiation are considered, which are presented by the following governing equation:

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha_{sf}\frac{\partial^2 T}{\partial y^2} + \frac{\sigma_{sf}B(x)^2}{\left(\rho C_p\right)_{sf}}u^2 - \frac{1}{\left(\rho C_p\right)_{sf}}\frac{\partial q_{rad}}{\partial y},\qquad(17)$$

where

$$q_{rad} = -\frac{\sigma^*}{3k^*} \frac{\partial T^4}{\partial y}.$$
 (18)

Here, σ^* is the Stefan–Boltzmann constant, k^* expresses the mass absorption coefficient, and the specific heat = $(C_p)_{sf}$. Expression **Eq. 16** takes the following form after substituting **Eq. 17** in it (Rashid et al., 2017):

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha_{nf}\frac{\partial^2 T}{\partial y^2} + \frac{1}{3(\rho C p)_{nf}}\frac{16\sigma^* T_{\infty}^3}{k^*}\frac{\partial^2 T}{\partial y^2} + \frac{\sigma_{nf}B(x)^2}{\left(\rho C_p\right)_{nf}}u^2.$$
(19)

The suitable boundary conditions are

$$T = T_w = T_{\infty} + T_{re} e^{x/L_c} \quad \text{at} \quad y = 0, \\ T \to T_{\infty} \quad \text{as} \quad y \to \infty, \end{cases}$$
(20)

where T_w is the temperature of the sheet, the characteristic length = L_c , T_{re} is the reference temperature, and T_{∞} is the free stream temperature. The temperature field similarity variable is specified as follows (Rashid et al., 2017):

$$\theta(\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}}.$$
(21)

The energy equation takes the following dimensionless form by utilizing Eqs. 5, 20:

$$\kappa\theta^{\prime\prime} - 2Prf^{\prime}\theta + Prf\theta^{\prime} + \frac{PrM_{egn}}{\chi_4}Ec_{rt}f^{\prime\prime2} = 0, \qquad (22)$$

where

$$\begin{split} \kappa &= \left(\frac{\chi_3}{\chi_4}\right) \left(1 + \frac{4}{3N_{tr}\chi_3}\right), \ Ec_{rt} = \frac{u^2}{(T_w - T_\infty) Cp}, \ Pr = \frac{v_{hf}}{\alpha_{hf}}, \\ N_{tr} &= \frac{K^* K_{hf}}{4\sigma^* T_\infty^3}, \\ \chi_3 &= \frac{(k_{sf} + 2k_{hf}) - (k_{hf}2\phi - k_{sf}2\phi)}{(k_{sf} + 2k_{hf}) + (k_{hf}2\phi - k_{sf}2\phi)}, \\ \chi_4 &= \left(\phi \frac{(\rho Cp)_{sf}}{(\rho Cp)_{hf}} - \phi + 1\right). \end{split}$$
(23)



Here, Pr is the Prandtl number, N_{tr} is the radiation parameter, and Ec_{rt} is the Eckert number. The boundary conditions are

$$\begin{array}{ccc} \theta(\eta) = 1 & \text{at} & \eta = 0, \\ \theta(\eta) \to 0 & \text{as} & \eta \to \infty. \end{array} \right\}.$$
 (24)

Now, using Eq. 9 in Eq. 21,

$$\kappa \theta'' - 2Pre^{-\Psi\eta}\theta + Pr\left(S + \frac{1}{\Psi}\left(\frac{1 - e^{-\Psi\eta}}{\Psi}\right)\right)\theta' + \frac{PrM_{egn}}{\chi_4}$$
$$Ec_{rt}\left(e^{-\Psi\eta}\right)^2 = 0. \tag{25}$$

introduces the following new variable to convert **Eq. 24** into Kummer's ordinary differential equation:

$$\beta = -\frac{Pre^{-\Psi\eta}}{\kappa\Psi^2}.$$
(26)

Applying the new variable, Eq. 24 becomes as expressed below:

$$\beta \frac{\partial^2 \theta}{\partial \beta^2} + (Q - \beta) \frac{\partial \theta}{\partial \beta} + 2\theta = -\frac{PrM_{egn}}{\chi_4} Ec_{rt} \left(e^{-\Psi \eta}\right)^2, \quad (27)$$

where Q = (1 - H), and $H = \frac{Pr}{\kappa \Psi} \left(\frac{1}{\Psi} + S\right)$.

The boundary conditions are

$$\theta(\beta) = 1, \qquad \qquad \theta(0) = 0. \tag{28}$$

The closed form solution of Eq. 26 in the form of Kummer's function (Abramowitz and Stegun, 1972) is

$$\theta(\beta) = \begin{pmatrix} \frac{M\left(-2+\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right),1+\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right),\beta\right)\beta^{\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right)}}{M\left(-2+\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right),1+\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right),-\frac{P_r}{\kappa\Psi^2}\right)2\left(-\frac{P_r}{\kappa\Psi^2}\right)^{\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right)}} \end{pmatrix} \\ \times \begin{pmatrix} \frac{1}{\left(-2+\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right)\right)\kappa\Psi^2\chi_4} \end{pmatrix}} \\ + \left(\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right)^2+(-\beta-3)\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right)+\beta^2-2\right)} \\ \times \begin{pmatrix} -M_{egn}Ec_{rt}\kappa\Psi^2\frac{2\xi-1+\frac{P_r}{\kappa\Psi}\left(s+\frac{1}{\Psi}\right)}{2\chi_4P_r} + \frac{M_{egn}Ec_{rt}\kappa\Psi^2}{2\chi_4P_r}\left(s+\frac{1}{\Psi}\right)} \end{pmatrix} \end{pmatrix}, \quad (29)$$

where M is the confluent hypergeometric function (1st kind). The following is the solution to the energy equation:

				$P(kgm^{-3})$	$C_p(Jkg^{-1}k)$	⁻¹)	$K(Wm^{-1}.K^{-1})$
Host fluid		Water		1,000.52	4,181.8	4,181.8	
Nanoparticle		Silver (Ag)		10,500	235	235	
		Gold (Au)		19,320	128	128	
TABLE 2 Va	ariation of ϕ , A_{vr}	, M_{egn} and M_{egn} on	- <i>f</i> ^{′′} (0).				
φ	A_{vr}	M _{egn}	S	$K_{pr} = 1$	2	3	4
т		8		1			
	0.5	2	0.3	1.657481343	1.815082580	1.959005252	2.092292460
0			0.3	1.657481343 1.984443250	1.815082580 2.121805427	1.959005252 2.249833214	
0 0.12			0.3				2.370204875
0 0.12 0.19			0.3	1.984443250	2.121805427	2.249833214	2.370204875 2.414654530
0 0.12 0.19	0.5		0.3	1.984443250 2.035210788	2.121805427 2.170034896	2.249833214 2.296000878	2.370204875 2.414654530 2.900603636
0 0.12 0.19	0.5		0.3	1.984443250 2.035210788 2.333480582	2.121805427 2.170034896 2.538101852	2.249833214 2.296000878 2.725959990	2.370204875 2.414654530 2.900603636 2.680763159
0 0.12 0.19	0.5 0.1 0.3		0.3	1.984443250 2.035210788 2.333480582 2.204829536	2.121805427 2.170034896 2.538101852 2.375274746	2.249833214 2.296000878 2.725959990 2.533104229	2.370204875 2.414654530 2.900603636 2.680763159 2.542635502
¢ 0 0.12 0.19 0.13	0.5 0.1 0.3 0.4	2	0.3	1.984443250 2.035210788 2.333480582 2.204829536 2.112178384	2.121805427 2.170034896 2.538101852 2.375274746 2.265835379	2.249833214 2.296000878 2.725959990 2.533104229 2.408649271	2.092292460 2.370204875 2.414654530 2.900603636 2.680763159 2.542635502 2.853729822 2.959495757

TABLE 1 Thermophysical characteristics of water, Ag, and Au (Mahalakshmi and Vennila, 2020).

TABLE 3 Numerical values of $-\theta'(0)$ for $Ec_{rt} = 1$, Pr = 6.2, and $N_{tr} = 1.5$.

Silver (Ag)

ϕ	A_{vr}	M _{egn}	S	K _{pr}	1	2	3	4
0	0.3	1	1		2.821624541	2.815382505	2.808359278	2.800973518
0.12					2.396432529	2.386817656	2.377578170	2.368727743
0.19					2.165174717	2.155072352	2.145507700	2.136449386
Gold (Au	:)							
φ	А	M_{egn}	S	K _{pr}	1	2	3	4
0	0.3	1	1		2.821624541	2.815382505	2.808359278	2.800973518
					2.344189203	2.335774423	2.327801131	2.320228978
0.12								

$$\theta(\eta) = \begin{pmatrix} e^{-\Psi \frac{Pr}{K\Psi} \left(S + \frac{1}{\Psi}\right) P\eta} M \left(-2 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right), 1 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right), -\frac{Pr}{\kappa\Psi^2} e^{-\Psi\eta} \right)}{2M \left(-2 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right), 1 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right), -\frac{Pr}{\kappa\Psi^2} \right)} \end{pmatrix} \\ \times \left(\frac{1}{\left(\kappa\Psi^2\chi_4\right) \left(-2 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right)\right)} \right)} \\ + \left(\frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right)^2 + \left(-\frac{Pr}{\kappa\Psi^2} e^{-\Psi\eta} - 3\right) \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right) + \left(\frac{Pr}{\kappa\Psi^2} e^{-\Psi\eta}\right)^2 - 4 \frac{Pr}{\kappa\Psi^2} e^{-\Psi\eta} + 2 \right)} \\ \times \left(\frac{M_{egn}Er_{fr} \kappa\Psi^2}{2\chi_4 Pr \left(-2 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right)\right)} - M_{egn}Er_{fr} \kappa\Psi^2 \frac{2\xi - 1 + \frac{Pr}{\kappa\Psi} \left(S + \frac{1}{\Psi}\right)}{2\chi_4 Pr} \right). \end{cases}$$

$$(30)$$

$$\theta_{\eta}(0) = \left. \begin{array}{l} \frac{Pr^{2} \left(s + \frac{1}{\Psi^{2}} \right)^{2} \lambda_{3} \left(2\chi_{4}Pr \Psi \left(s + \frac{1}{\Psi} \right) - 4\chi_{4}\Psi^{2} \kappa - M_{eggn}Ec_{rt} Pr \right)}{2\kappa^{2} a\chi_{4}\Psi^{2} \left(-2 + P \right)} \\ + \left(\frac{Pr \left(s + \frac{1}{\Psi} \right) \left(\lambda_{4} - \lambda_{3} \right) \left(2\chi_{4}Pr \Psi \left(s + \frac{1}{\Psi} \right) - 4\chi_{4}\Psi^{2} \kappa - M_{eggn}Ec_{rt} Pr \right)}{\kappa^{2} \lambda_{3}\chi_{4}\Psi} \right) \\ - \left(\frac{1}{2a\chi_{4}\Psi^{2}\kappa} \left(- \left(\lambda_{5} - \lambda_{4} \right) \left(-1 + \frac{Prs}{K^{4}} + \frac{Pr}{R^{2}} \right) \Psi + \left(\lambda_{4} - \lambda_{3} \right) \right) \right) \left(-2\xi + \frac{Prs}{K^{4}} + \frac{Pr}{\kappa^{4}} \right) \Psi \\ \times \left(2\chi_{4}Pr \Psi \left(s + \frac{1}{\Psi} \right) - 4\chi_{4}\Psi^{2}\kappa - M_{eggn}\Psi^{2}\kappa + \frac{1}{\kappa} \right) \\ + \left(\frac{\left(\frac{-2Pr}{\kappa^{2}\Psi} \left(s + \frac{1}{\Psi} \right) + \frac{4Pr}{\kappa} \right) EcM_{eggn}\Psi^{2} \kappa}{\chi_{4}Pr \left(-2 + \frac{Pr}{\kappa^{\Psi}} \left(s + \frac{1}{\Psi} \right) \right)} + \frac{Ec_{rt} M_{eggn}\Psi^{2}}{\chi_{4}} \right),$$

$$(31)$$

where

$$\begin{split} \lambda_3 &= M \bigg(\frac{Pr}{\kappa \Psi} \bigg(S + \frac{1}{\Psi} \bigg) - 2, \frac{Pr}{\kappa \Psi} \bigg(S + \frac{1}{\Psi} \bigg) + 1, -\frac{Pr}{\Psi^2 \kappa} \bigg), \\ \lambda_4 &= M \bigg(\frac{Pr}{\kappa \Psi} \bigg(S + \frac{1}{\Psi} \bigg) - 1, \frac{Pr}{\kappa \Psi} \bigg(S + \frac{1}{\Psi} \bigg) + 1, -\frac{Pr}{\Psi^2 \kappa} \bigg), \\ \lambda_5 &= M \bigg(\frac{Pr}{\kappa \Psi} \bigg(S + \frac{1}{\Psi} \bigg), \frac{Pr}{\kappa \Psi} \bigg(S + \frac{1}{\Psi} \bigg) + 1, -\frac{Pr}{\Psi^2 \kappa} \bigg), \\ \Psi &= \frac{1}{2} \chi_1 \chi_2 S + \frac{1}{2} \sqrt{\chi_1^2 \chi_2^2 S^2 - 8A_{\nu r}^2 \chi_1 \chi_2 - 4A_{\nu r} \chi_1 M_{egn+\xi}}. \end{split}$$

As a result, the non-dimensional wall temperature was generated by the aforementioned equation. The local Nusselt number is as follows:

$$Nu = \frac{-k_{sf}x\left(\frac{\partial T}{\partial y}\right)_{y=0}}{k_{hf}(\Delta T)} = -\frac{k_{sf}}{k_{hf}}Re_x^{1/2}\theta'(0) = \frac{k_{hf}}{k_{sf}}Nu_xRe_x^{-1/2}$$
$$= -\theta'(0).$$
(32)

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4 Second law analysis

The interchange of momentum, temperature, and magnetic effects inside the fluid and at the surfaces generates a continual entropy accumulation, resulting in a non-equilibrium condition. The following formula can be used to compute the volumetric entropy inception factor (S_{Gen}):

$$S_{Gen} = \frac{k_{sf}}{T_{\infty}^2} \left(1 + \frac{16T^3\sigma^*}{3k^*}\right) \left(\frac{\partial T}{\partial y}\right)^2 + \frac{\mu_{sf}u^2}{T_{\infty}k} + \frac{\sigma^*B_0^2u^2}{T_{\infty}}.$$
 (33)

The impact of three independent mechanisms generating entropy production is reflected in **Eq. 33**. The first term of **Eq. 33** shows the entropy inception provoked by heat transport along with a thermal impact, which is expressed by (E_{HT}) , the second term represents the entropy inception because of a magnetic impact (E_{MGN}) , and the entropy inception due to porous (E_{PM}) is described by the third term. Entropy is a measure of disordered in a system and its surroundings. The amount of non-dimensional entropy production $E_G = \frac{S_{GGR}}{S_{max}}$ is

$$\begin{split} E_G = & \chi_3 Re \left(1 + N_{tr} \right) \theta'(\eta)^2 + Br_{kmn} K_{pr} f'(\eta)^2 + Br_{kmn} \frac{M_{egn}}{\Omega} \\ f'(\eta)^2, \end{split} \tag{34}$$

where

$$S_{gen} = \frac{k_{hf}}{T_{\infty}^2 \left(\frac{\Delta T}{x}\right)^2}, Br_{kmn} = \frac{\mu_{sf} u_{re} x^2}{\Delta T k_{sf}}, \ \Omega = \frac{T_{\infty}}{\Delta T}, \text{ and}$$
$$M_{egn} = \frac{\sigma B_0^2 2 u_{re}}{\mu_{hf}}, \tag{35}$$

where Ω is the ratio of free stream temperature to the change in temperature. Bejan (1979) proposed an additional parameter, the Bejan number (Be), to find out the irreversibility field. The Bejan number (Be) is the ratio of heat exchange irreversibility to the total amount of irreversibility inside the process, expressed as

$$Be = \frac{E_{HT}}{E_{HT} + E_{MGN} + E_{PM}}.$$
(36)

5 Results and discussion

The influence of several emerging factors on the velocity, temperature, and entropy inception fields has been demonstrated in the current phase to examine the impact of these parameters. Furthermore, under the effect of suction/injection parameter (*S*), permeability parameter K_{pr} , and magnetic parameter M_{egn} , Ec_{rt} , ϕ , Br_{kmn} , Ω , and Rey, local skin friction, stream line, local Nusselt number, and Bejan (*Be*) number are presented. In this scenario, **Figures 2–18** are plotted and **Tables 1**, 2, 3 are shown. **Figures 2**, 3 show the trend of the velocity field as the magnitude

of ϕ is varied. It is to be noted that the velocity field is accelerated due to an increment in the magnitude of the nanoparticle volume friction in the case of Ag- and Au- water with S > 0 depicted in **Figure 2**. Physically, inter-molecular forces are increased in the presence of nanoparticles, which leads to a reduction in the velocity distribution. In the case of both Ag- and Au- water nanofluids with S < 0, the velocity distribution decreases due to an increase in ϕ as shown in **Figure 3**. The variation of nanoparticle friction on the temperature field is shown in **Figure 4**. An increment is observed in temperature distribution while gaining the magnitude of ϕ . Physically, the friction factor is enhanced with the existence of nanoparticles due to friction, and the overall internal temperature is accelerated in both Ag- and Au- and Au- water.

Figure 5 depicts the influence of Ec_{rt} on the temperature profile. As heat energy is produced in Ag- and Au- water nanofluids caused by friction heat, the temperature field is being augmented with an increasing value of Ec_{rt} . The impression of M_{egn} on the temperature field is shown in **Figure 6**. It is pointed out that the temperature distribution increases with a gain in M_{eqn} . In fact, the Lorentz effect has a considerable influence on M_{eqn} . A greater Lorentz force is associated with elevated M_{eqn} , whereas a smaller Lorentz strength is linked with lower M_{egn} . The larger Lorentz force creates more energy in both Ag- and Au- water, resulting in an increase in temperature change. The consequences of M_{egn} on -f''(0) are plotted in Figure 7. It is perceived that an augmentation in the magnetic entity escalates skin friction at the wall in both Ag- and Au- water. Moreover, Ag- water has a higher rate of skin friction than the Au- water nanofluid. Figure 8 shows the reaction of the wall mass transport entity on -f''(0). The magnitude of -f''(0) is stated to be reduced due to the decreasing amount of the wall mass transport entity (S) for both Ag- and Au- water. Additionally, Ag- water has a higher rate of skin friction than the Au- water nanofluid. The effects of Ec_{rt} and K_{pr} are shown in **Figures 9**, 10. The heat transport rate is seen to decrease with the magnitude of Ec_{rt} and K_{pr} for both Agand Au- water nanofluids. It is also noted that the heat exchange rate rapidly decreases in the occurrence of Au- water than in the Ag– water in **Figures 9**, 10. Physically, the magnitude of $-\theta'(0)$ decreases as the value of the permeability parameter decelerates. Physically, the existence of a porous structure restricts nanofluid flow, slowing fluid velocity and decreasing the heat transport rate at the wall.

Figures 11, 17 plot the influence of different parameters on the entropy inception E_G and Bejan *Be* number to visualize the system's chaos. **Figure 11** portrays the result of the Br_{kmn} number. It is expressed that entropy inception is decreased with an increase in Br_{kmn} . Additionally, more chaos is reported in the case of silver–water in the system than the gold–water nanofluid. Similar trends are shown in **Figures 12, 14** for *Rey* and M_{egn} , respectively The opposite behavior is observed in **Figure 13** for Ω . In **Figures 15, 17**, the variation of Ec_{rt} , ϕ , and Ω is investigated. It is perceived that *Be* is increased while increasing the value of Ec_{rt} , ϕ , and Ω . Physically, the Bejan *Be* number is, indeed, a non-dimensional quantity that shows the proportion of overall entropy creation that is generated by thermal dissipation. As a result, the Bejan number is a description of the entropy created by heat transmission and resistance to flow rather than a heat transport parameter.

Table 1 lists the thermophysical characteristics of H_2O , Ag, and Au. **Tables 2**, 3 are constructed for numerical values of -f''(0) and $-\theta'(0)$, respectively. **Figures 18A–**C, **Figures 19A–**C are plotted to provide insight into the flow pattern in the case of Ag– and Au– water (**Figure 16**).

6 Conclusion

The study presents an entropy inception investigation of magnetohydrodynamic Ag- and Au- H_2O nanofluid flows induced by an exponential stretching surface embedded in a porous medium with suction/injection and thermal conductivity. The investigation's principal conclusions have been summarized as follows:

- In both Ag- and Au-H₂O, the solid volume percentage has an accelerating effect on the velocity profile with suction/injection parameters.
- In both *Ag* and *Au*-*H*₂O, the *Ec*_{rt} and *M*_{egn} have an increasing impact on the temperature profile.
- It is perceived that an augmentation in the magnetic entity escalates skin friction at the wall in both *Ag* and *Au* water. Moreover, *Ag* water has a higher rate of skin friction than the *Au* water nanofluid.
- The heat transport rate is a decreasing function of Ec_{rt} and K_{pr} for both Ag- and Au- water nanofluids.
- It is also noted that the heat exchange rate rapidly decreases in the occurrence of *Au* water than in *Ag* water.
- The entropy inception is an increasing function of Br_{kmn} , *Rey*, and M_{egn} in both *Ag* and *Au* water.

• More chaos is observed in the case of *Ag*- water in the system than in the *Au*- water nanofluid.

Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material; further inquiries can be directed to the corresponding author.

Author contributions

IR initiated the fluid model and methodology. TZ, IR, and MA solved the model using software. JA completed the write-up and assisted in fluid model development.

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Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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