



# Air-Sea Trace Gas Fluxes: Direct and Indirect Measurements

Christopher W. Fairall<sup>1\*</sup>, Mingxi Yang<sup>2</sup>, Sophia E. Brumer<sup>3</sup>, Byron W. Blomquist<sup>1,4</sup>, James B. Edson<sup>5</sup>, Christopher J. Zappa<sup>6</sup>, Ludovic Bariteau<sup>1,4</sup>, Sergio Pezoa<sup>1</sup>, Thomas G. Bell<sup>2</sup> and Eric S. Saltzman<sup>7</sup>

<sup>1</sup> National Oceanic and Atmospheric (NOAA) Administration, Department: Physical Science Laboratory, Boulder, CO, United States, <sup>2</sup> Plymouth Marine Laboratory; Department: Marine Biogeochemistry and Observations, Plymouth, United Kingdom, <sup>3</sup> Laboratoire d'Océanographie Physique et Spatiale, UMR 6523, CNRS-IFREMER-IRD-UBO, IUEM, Plouzané, France, <sup>4</sup> Cooperative Institute for Research in Environmental Sciences, University of Colorado Boulder, Boulder, CO, United States, <sup>5</sup> Applied Ocean Physics & Engineering, Woods Hole Oceanographic Institution, Woods Hole, MA, United States, <sup>6</sup> Lamont-Doherty Earth Observatory of Columbia University, Palisades, NY, United States, <sup>7</sup> Department of Earth System Science, University of California, Irvine, CA, United States

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### \*Correspondence:

Christopher W. Fairall  
chris.fairall@noaa.gov

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The past decade has seen significant technological advance in the observation of trace gas fluxes over the open ocean, most notably CO<sub>2</sub>, but also an impressive list of other gases. Here we will emphasize flux observations from the air-side of the interface including both turbulent covariance (direct) and surface-layer similarity-based (indirect) bulk transfer velocity methods. Most applications of direct covariance observations have been from ships but recently work has intensified on buoy-based implementation. The principal use of direct methods is to quantify empirical coefficients in bulk estimates of the gas transfer velocity. Advances in direct measurements and some recent field programs that capture a considerable range of conditions with wind speeds exceeding 20 ms<sup>-1</sup> are discussed. We use coincident direct flux measurements of CO<sub>2</sub> and dimethylsulfide (DMS) to infer the scaling of interfacial viscous and bubble-mediated (whitecap driven) gas transfer mechanisms. This analysis suggests modest chemical enhancement of CO<sub>2</sub> flux at low wind speed. We include some updates to the theoretical structure of bulk parameterizations (including chemical enhancement) as framed in the COAREG gas transfer algorithm.

**Keywords:** gas transfer velocity, chemical enhancement, bubble mediated transfer, COARE gas flux parameterization, Dimethylsulfide (DMS), carbon dioxide (CO<sub>2</sub>), bulk algorithm, direct observation

## 1 INTRODUCTION

The exchange of gases between the atmosphere and ocean is an important process in global budgets of many gases with significant implications in climate, biogeochemical cycles, oceanic ecosystems, and pollution. Because of its importance to global carbon budgets, biology, and climate, carbon dioxide (CO<sub>2</sub>) tends to dominate our interest in the subject but many gases including oxygen (O<sub>2</sub>), carbon monoxide (CO), dimethylsulfide (DMS), ozone (O<sub>3</sub>), and sulfur dioxide (SO<sub>2</sub>) to name a few, are also relevant - see Johnson (2010) for a list of 79 gases. The exchange of non-reactive gases are usually expressed as vertical fluxes which are principally driven by wind speed and the sea-air concentration difference of the gas. Gas fluxes may be measured directly from ships with bow-

mounted eddy correlation systems or estimated from mean concentrations using so-called bulk flux relationships (Fairall et al., 2000; Wanninkhof et al., 2009). Arrays of *in situ* measurements are not practical for global or regional budget closure, so some combination of satellite, reanalysis, and data assimilation synthesis is needed (Cronin et al., 2019; Shutler et al., 2020). These approaches rely on the bulk relationships. Thus, the principal application of direct measurements [including deliberate dual tracer techniques, Ho et al. (2011)] is in determining the appropriate bulk scaling variables and coefficients. It turns out this is a complex issue that involves similarity theory, chemistry, laboratory studies, process models such as direct numerical and large eddy simulations (DNS and LES), and a variety of experimental approaches in the field (see Garbe et al., 2014, for an overview).

The mass flux of some scalar variable,  $x$ , can be directly estimated from measurements of turbulent correlations in the near-surface atmosphere with the direct covariance (a.k.a. eddy correlation) technique:

$$F_x = \rho_{ad} \overline{w'r_x'} \cong \overline{w'x'} \quad (1)$$

Here  $\rho_{ad}$  is the density of dry air,  $r_x$  the mixing ratio of  $x$  (mass of  $x$  per dry mass of air),  $w'$  and  $x'$  are turbulent fluctuations of vertical velocity and dry air mole fraction of  $x$ , respectively. More often though, the air-sea flux is computed using the bulk method:

$$\overline{w'x'} = C_x S_z (X_s - X_z) = c_x^{1/2} u_* (X_s - X_z) \quad (2)$$

where  $X$  is the mean concentration of  $x$  and the subscripts  $s$  and  $z$  refer to the value at the air-ocean interface and height  $z$ , respectively.  $S$  is the mean wind speed,  $C_x$  is the transfer coefficient for the mass flux of  $x$ ,  $c_x^{1/2}$  is the scalar transfer component specific to  $x$  and  $u_* = \sqrt{C_d} U_{10}$  is the friction velocity where  $C_d$  is the drag coefficient and  $U_{10} = \sqrt{U^2 + V^2}$  is the vector average wind speed for mean components  $U$  and  $V$  at reference height  $z = 10$  m. Note mean wind *speed* is distinct from the mean vector wind components and is defined as  $S^2 = (U + u')^2 + (V + v')^2$ , where the capitals and primes denote of the mean and turbulent fluctuations of the horizontal wind components. Differences between the mean wind speed, and vector-averaged winds are associated with gustiness (Fairall et al., 1996; Fairall et al., 2003).

The essence of bulk parametrizations is captured in specification of the transfer coefficient,  $C_x$ , which is obtained directly by measuring  $\overline{w'x'}$ ,  $S_z$ ,  $X_s$ , and  $X_z$  and applying (2). Note  $C_x$  will depend on  $z$  and buoyancy forcing as defined in Monin-Obukhov similarity theory (MOST – see e.g., Fairall et al. (1996)). Bulk algorithms have a long and successful history in meteorology; in this paper we will focus principally on the COARE family of flux codes (Fairall et al., 2011) where COAREG defines codes for gas transfer. There are certainly other products to choose from for gas transfer purposes, e.g., FluxEngine (Goddijn-Murphy et al., 2016; Shutler et al., 2016) or FuGas (Vieira et al., 2020).

While (2) is commonly used to estimate fluxes of sensible heat and moisture, the gas transfer community more often uses a

formulation based on a transfer velocity,  $k_x$ ,

$$F_x = \alpha_x k_x (X_w / \alpha_x - X_a) = \alpha_x k_x \Delta X \quad (3)$$

where  $\alpha_x$  is the dimensionless solubility of the gas  $x$  in seawater,  $k_x$  the transfer velocity for the gas  $X$ ,  $X_w$  and  $X_a$  the mean concentrations of  $x$  at some depth in water and some height in air, and we use  $\Delta X$  to denote the sea-air difference in  $X$  taking solubility into account. Note that, compared to (2), expression (3) has the additional complexity of solubility. Superficially,  $k_x$  is equivalent to  $C_x S_z = c_x^{1/2} u_*$  in (2). Because  $C_x$  for heat and moisture is approximately constant with the friction velocity or wind speed, we might infer that  $k_x$  is roughly proportional to wind speed. Would that it was so simple. To illustrate the variability in transfer with the properties of trace gases, Fairall et al. (2011) recast (3) as

$$F_x = \alpha_x k_x \Delta X = \left[ \frac{\alpha_x k_x}{u_*} \right] [u_* \Delta X] = \text{CP}_x [u_* \Delta X] \quad (4)$$

with CP being interpreted as characterizing the chemical variability and  $u_* \Delta X$  characterizing the physical forcing. Figure 1 in Fairall et al. (2011) shows CP varying by 4 orders of magnitude with small values ( $2 \times 10^{-6}$ ) for the highly insoluble gas neon, increasing with solubility to about 0.03 for  $\alpha_x = 100$  (e.g., ethanol) and then leveling off with increasing solubility. This leveling off for highly soluble gases is well understood to be the limit imposed by transfer in the atmosphere – i.e., similar to water vapor, which is unconstrained by transfer resistance on the ocean side,  $\text{CP}_v = c_v^{1/2} \approx 0.035$ . Both  $\text{CO}_2$  (solubility on the order of 0.5) and DMS (solubility on the order of 15) are intermediate to these extremes.

Early wind tunnel measurements (Liss and Merlivat, 1986) and analysis of  $^{14}\text{C}$  in the ocean (Wanninkhof, 1992) found the transfer velocity of  $\text{CO}_2$  (i.e.,  $k_{\text{CO}_2}$ ) to be non-linear in wind speed. Woolf (1993) argued that the stronger wind speed dependence of  $\text{CO}_2$  was due to enhancement by bubbles generated by breaking waves. Because the enhancement was solubility dependent, Woolf predicted that more soluble gases would have a more linear wind speed dependence – a prediction that has been borne out by observations of DMS transfer velocity (e.g., Blomquist et al., 2006).

Ocean surface waves are an essential component in air-sea fluxes. The fluxes of momentum and kinetic energy from the atmosphere to the ocean are driven by a direct input to the ocean currents *via* viscous stress and input to waves *via* the pressure-wave slope correlation known as *form drag*. Viscous stress dominates the exchange at low wind speeds. As the winds increase, the dominant mechanism for exchange transfers to the form drag imposed primarily by wind waves with some modulation due to longer waves and swell. The action of the form drag grows waves which transfer their momentum and energy to ocean currents and turbulence initially through micro-breaking (Edson et al., 2013). The transition is complete once the waves become fully rough; a condition often associated with the onset of visible wave breaking around  $7 \text{ m s}^{-1}$ . At this point, bubble-mediated processes begin to gain importance (Woolf,

1993) and breaking of longer waves plays an increasingly important role in momentum and, particularly, energy exchange (Melville, 1996).

The simplicity of bulk flux relations (2) and (3) is somewhat misleading because complexity may be hidden in the transfer coefficients. The simplest forms contain little complexity, with power law dependence on wind speed at some reference height, typically 10m.

$$k_x = c_{1x} U_{10}^2 \quad (5)$$

where the coefficient  $c_{1x}$  depends on the gas and  $U$  in  $\text{m s}^{-1}$  ( $k_x$  in  $\text{cm hr}^{-1}$ ). For  $\text{CO}_2$   $c_{1x}$  is on the order of 0.25 (Wanninkhof, 2014). However, there is debate about the power law with up to 3<sup>rd</sup>-order polynomials in wind speed being used (Wanninkhof et al., 2009). The temperature dependence of  $k_x$  is usually captured through a temperature-dependent Schmidt number  $Sc_x = \nu/D_x$ , where  $D_x$  is the oceanic molecular diffusivity and 660 is the reference value of  $Sc_{\text{CO}_2}$  at 20°C (although the 1/2 exponent may not hold in all conditions).

$$k_{660x} = c_{1x} U_{10}^2 (Sc_x/660)^{1/2} \quad (6)$$

Since the bulk gas and water concentrations are measured well away from the interface, mixing processes in both media must be considered. This has led to the development of physically-based parameterizations that attempt to capture the relevant processes in a unified mathematical structure (e.g. Liss and Slater, 1974; Fairall et al., 2011; Goddijn-Murphy et al., 2016). If this is successful, it is not necessary to measure  $c_{1x}$  for each gas of interest. This is the approach for the COAREG gas flux parameterizations where both atmospheric and oceanic interfacial forcing are framed within surface-layer turbulent scaling theory. In the ocean, turbo-molecular mixing and bubble mediated transfer are treated as parallel processes.

While wave processes are important in almost all aspects of air-sea interactions, it is interesting that many very successful parameterizations do not explicitly include wave properties. This is because wave properties are highly correlated with wind speed. Thus, simple representations in the drag coefficient,  $C_d$ , or  $k_x$  are done with wind speed alone. Ironically, decades of experimental and theoretical effort (see Brumer et al., 2017a) have yet to yield wave-based parameterizations for  $C_d$ , or  $k_x$  that give significantly better RMS fits to direct observations over the open ocean. This is partly due to the large sampling noise of the observations and partly the noisy and uncertain nature of characterizations of the wave field. However, that is not the complete story because wind-only parameterizations essentially characterize transfer for a mean wave climatology associated with that wind speed. We expect that when the waves depart significantly from that mean, then air-sea fluxes may be affected. For example, in a coastal region offshore winds may yield quite different fluxes compared to onshore winds at the same wind speed, as has been observed for sea spray (Yang et al., 2019). Regardless of our ability to explicitly include wave variables in a parameterization, separating near-surface turbulent and bubble-mediated processes in physically-based treatments of gas transfer is useful.

In this paper we will further discuss air-sea fluxes – principally gas transfer and its forcing mechanisms – in the context of the COARE algorithms. We will not attempt a detailed attack on all issues (e.g., discussion in Johnson et al., 2011; Woolf et al., 2019), but focus on specific topics where significant progress has been made through observations, theory, or numerical modeling. The principal scaling variables for  $k_x$  are solubility, Schmidt number, friction velocity, and whitecap fraction. The last two variables may be estimated with wind-only formulae or with formulae that add some wave information. We begin with a discussion of theoretical background, then sketch the formulation of COARE [taking from detail provided in Fairall et al. (2011)]. We will briefly describe direct observations and focus on three recent field programs. We will discuss wave-based parameterizations and the difficulty of determining them with observations alone. Because of their more than one order of magnitude solubility differences, simultaneous DMS and  $\text{CO}_2$  observations can be analyzed to separate the turbo-molecular and bubble-mediated components. To do this, we will also have to deal with chemical enhancement of  $\text{CO}_2$  flux (Wanninkhof, 1992; Luhar et al., 2018; Jørgensen et al., 2020). The turbo-molecular transfer is found to be quite linear with the *tangential* component of the stress. The bubble component is approximately linear with either whitecap fraction or air-entrainment rate of breaking waves but there is still some uncertainty in characterizing those quantities which will be discussed.

## 2 THEORETICAL BACKGROUND

In this section we describe a simple 1-dimensional theoretical framework for describing the flux-profile relationships for trace gas transport between the atmosphere and ocean. The approach has its roots in observations from wind tunnels and flat Kansas plains, so application over the ocean requires a certain skepticism. It is known that wind speed does not strictly obey the conventional log-layer behavior within the wavy boundary layer. Furthermore, distortions by wave motions on the ocean side occur on scales that are greater than the normal ‘10% of the mixed layer depth’ usually ascribed to the surface layer where ‘law of the wall’ scaling is appropriate. Our justification for using this approach for gas transfer applications is based on the small scale of the molecular sublayer and the transition to the turbulent sublayer – this occurs at mm scales where local dominant wave-induced slopes are negligible. This theoretical approach allows us to conceptualize the balance of the processes and to create a scaling structure that can be tuned to observations with only a few universal parameters.

### 2.1 Fluxes, Solubility, Similarity and Turbo-Molecular Transport

In the absence of significant *in situ* sources or sinks, the vertical flux of some scalar variable,  $x$ , in either fluid can be defined as the sum of molecular and turbulent diffusivities

$$F_x = -D_x \frac{\partial X}{\partial z} + \overline{w'x'} \quad (7)$$

In the case where  $z$  is height or depth, the flux is positive directed away from the interface. Near the surface the turbulent flux can be represented in terms of the local gradient and a turbulent eddy diffusivity,  $K(z)$ , so that

$$F_x = -[D_x + K(z)] \frac{\partial X}{\partial z} \quad (8)$$

We can integrate (8) from the surface to some reference height (depth),  $z_r$ , to obtain the total change of  $X$  between the surface (subscript  $s$ ) and  $z_r$ ,

$$(X_s - X_r) = \Delta X_r = \int_0^{z_r} \frac{F_x dz}{[D + K(z)]} = F_x \int_0^{z_r} \frac{dz}{[D + K(z)]} \quad (9)$$

If we define an air-side transfer velocity of  $x$ ,  $k_{xa}$ , as acting between the surface and some reference height in the atmosphere,  $z_{ra}$ , then

$$F_{xa} = k_{xa}(X_{sa} - X_{zra}) = k_{xa} \Delta X_{ra} \quad (10)$$

Thus, (9) and (10) imply

$$k_{xa}^{-1} = \int_0^{z_{ra}} \frac{dz}{[D + K(z)]} \quad (11)$$

Similarly, we can define a turbo-molecular flux on the water side

$$F_{xw} = k_{xw}(X_{sw} - X_{zrw}) = k_{xw} \Delta X_{rw} \quad (12)$$

While temperature is continuous across the interface, gas concentrations are not so we must account for the discontinuity by defining the solubility,  $\alpha_x$  as

$$\alpha_x = X_{sw}/X_{sa} \quad (13)$$

If we assume the atmospheric flux is continuous with the oceanic flux (applicable to a gas not undergoing rapid chemical reactions), then we can derive (4) where

$$k_x^{-1} = k_{xw}^{-1} + \alpha_x k_{xa}^{-1} \quad (14)$$

We use Monin-Obukhov Similarity (MOS) to describe the turbulent diffusivity (Fairall et al., 2000, hereafter F00): MOS defines surface turbulent flux scaling parameters  $u_*$  and  $x_*$  in terms of turbulent conditions sufficiently far from the interface that fluxes of momentum or of a scalar  $x$  (i.e. trace gases) are completely carried by turbulent covariance

$$\overline{w'u'} = -u_*^2 \quad (15a)$$

$$\overline{w'x'} = -u_* x_* \quad (15b)$$

The profile of a dynamical variable can be described *via* a dimensionally consistent combination of the scaling parameters,  $z$ , and a dimensionless function of  $z/L$ , where  $L$  is the MOS buoyancy length scale. This leads to a simple specification of turbulent diffusivity

$$K(z) = \kappa z u_* / \phi(z/L) \approx \kappa z u_* \quad (16)$$

where  $\phi$  is an empirical function that characterizes the enhancement of diffusion in convective conditions or suppression in stratified conditions and  $\kappa$  is the von Karman constant,  $\kappa \approx 0.4$ . Stability effects may be substantial but for dealing with near-surface and interfacial aspects of gas transfer, we can assume  $\phi = 1$ .

F00 discuss solutions to (9) and (11) using an approximation for  $K(z)$  that accounts for the suppression of turbulence near the interface which occurs in the sublayer

$$z < \delta_u = \lambda v / u_* \quad (17)$$

Where  $\lambda$  is a coefficient on the order of 10. This is done by expressing  $K(z)$  as

$$K(z) = \kappa z u_* / (1 + \delta_u / z) \quad (18)$$

The form of (18) produces a smooth transition from molecular-dominated diffusion to turbulent diffusion and has the effect of extending the depth of the molecular layer. The analytical solution to (9) produces a near-surface linear profile (molecular sublayer) that transitions to a logarithmic profile (turbulent sublayer)

$$\frac{\Delta X_s(z)}{F_{xs}} = \frac{1}{2c} \log(G/a) + \frac{2[\delta_u - \frac{b}{2c}]}{d} \left[ \arctan\left(\frac{b + 2cz}{d}\right) - \arctan\left(\frac{b}{d}\right) \right] \quad (19)$$

where  $a = D_x \delta_u$ ,  $b = D_x$ ,  $c = \kappa u_{*w}$ ,  $d = [4D_x \delta_u \kappa u_{*w} - D_x^2]^{1/2}$   $G = a + bz + cz^2$ .

In principle, this solution applies to vertical transfer of dissolved gas within the ocean in the absence of chemical reactions. The analytical profile in the turbulent layer can be approximated

$$\frac{\Delta X}{F_x} = \frac{\Delta X_m}{F_x} + \frac{1}{\kappa u_*} \log\left(\frac{z}{5 \delta_u}\right) \quad (20)$$

where  $5\delta_u$  is the maximum extent of the molecular sublayer (Züllicke, 2005) and  $\Delta X_m$  characterizes the total change in  $X$  over that layer. Using  $\lambda = 10$ , the analytical solution gives

$$\frac{u_* \Delta X_m}{F_x} = \frac{1}{\kappa} \left[ \frac{\pi}{2} (\lambda \kappa S_{c_x})^{1/2} + \log\left(5 \left(\lambda \kappa S_{c_x}\right)^{1/2}\right) \right] = 7.8 S_{c_x}^{1/2} + 2.5 \log(10 S_{c_x}^{1/2}) \quad (21)$$

The logarithmic form is an idealization because of the distortions of the wave motions. At heights well above the significant wave height, atmospheric logarithmic profiles are observed over the ocean (e.g. Edson et al., 2004). In the ocean, wave induced displacements are a significant fraction of the mixed layer depth and an idealized log-layer may not exist (Zheng et al., 2021). However, we still expect the idealized solution to reasonably describe the main aspects of the profile at cm scales.

## 2.2 The Wavy Boundary Layer - Viscous Stress Versus Wave Stress

Waves add another complication because of their role in the momentum transfer and the friction velocity. The fluxes of momentum and kinetic energy from the atmosphere to the ocean are, except in light winds, dominated by input to waves *via* the pressure-wave slope correlation – the so called form drag. The action of the wind grows waves which, when they break, transfer their momentum and energy to ocean currents and turbulence. The wind is also subject to a viscous drag which directly drives surface currents and near-surface turbulence. Far from the interface, (but still within the surface layer of the marine boundary layer), the momentum flux from the atmosphere (surface stress) can be expressed as the covariance of atmospheric turbulent velocity fluctuations similar to (1)

$$\tau = \rho_a \overline{w'u'} = -\rho_a u_{*a}^2 \quad (22)$$

where  $u'$  represents fluctuations of wind speed in the in the mean wind direction (for simplicity, we ignore the crosswind stress component). Near the air-sea interface (even within the influence of surface wave disturbances) the momentum flux is the sum of viscous, turbulent, and wave-pressure components  $\tau_v$ ,  $\tau_t$ ,  $\tau_g$ . Thus, while the total stress may be assumed to be approximately constant in height, the turbulent  $\tau_t$  component is not constant in the wave boundary layer (Ortiz-Suslow et al., 2021). At the interface, turbulence is negligible, and so the momentum flux delivered to the ocean is the sum of viscous (subscript  $v$ ) and gravity wave drag (subscript  $g$ )

$$\begin{aligned} \tau &= \tau_v + \tau_t + \tau_g = \tau_{vs} + \tau_{gs} = -\rho_a \nu_a \left[ \frac{\partial U}{\partial z} \right]_s + \left[ p' \frac{\partial \eta}{\partial x_u} \right]_s \\ &= -\rho_a (u_{*av}^2 + u_{*ag}^2) \end{aligned} \quad (23)$$

Viscous (tangential) drag is the product of the air kinematic viscosity with the wind gradient at the surface (subscript  $s$ ), while the gravity wave drag is the correlation of 'pressure fluctuations,  $p'$ , and the wave slope'  $\rho$  is the symbol for density,  $p$  the symbol for pressure ( $\eta$  is the vertical displacement of the surface by waves) and  $x_u$  is the horizontal coordinate in the mean wind direction. Soloviev (2007) and Fairall et al. (2011) argue that, at scales less than 1 m near the interface,  $u_{*av}$  should scale with the turbulent diffusion because the wave-pressure correlation has reduced the turbulent momentum flux. This has been discussed in more detail by Cifuentes-Lorenzen et al. (2018) who suggest the wave stress component decays exponentially with a height scale of about 1 m. The partitioning suggested by (23) can be written

$$u_{*a}^2 = c_d U_{10}^2 = (c_{dv} + c_{dg}) U_{10}^2 = u_{*av}^2 + u_{*ag}^2 = u_{*av}^2 + \alpha_g u_{*a}^2 \quad (24)$$

Cifuentes-Lorenzen et al. (2018) use the parameter  $\alpha_g$  which is the fraction of wave stress to total stress so that

$$u_{*av} = u_{*a} \sqrt{1 - \alpha_g} \quad (25)$$

Fairall et al. (2011) give an estimate of the ratio of viscous to total stress as

$$u_{*av} = u_{*a} \sqrt{c_{dv}/c_d} \quad (26)$$

and provide a simple formulation [see Figure B1 in Fairall et al. (2011)]. **Figure 1** shows estimates of  $\alpha_g$  as a function of 10-m wind speed and wave age,  $c_p/U_{10}$  where  $c_p$  is the phase speed of the waves with frequency corresponding to the peak of the wave energy spectrum.  $\alpha_g$  is small at low winds and increases with wind speed; viscous and wave components of stress are comparable at wind speeds on the order of 12 m s<sup>-1</sup> (see **Figure 1**). Friction velocity on the ocean side is computed assuming the atmospheric viscous stress drives the oceanic viscous stress:

$$u_{*wv} = \sqrt{\frac{\rho_a}{\rho_w}} u_{*av} \quad (27)$$

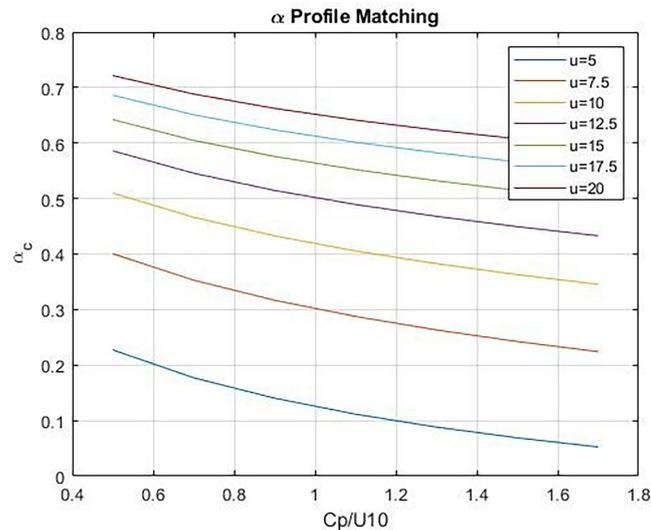
## 2.3 Atmospheric and Ocean Side Turbulent-Molecular Diffusion and Bubbles

On the atmospheric side of the interface, the behavior of  $k_{xa}$  is well-constrained by direct covariance flux measurements of water vapor [see **Figure 4** in Fairall et al. (2000)] and other trace gases of high solubility/reactivity (Yang et al., 2014; Yang et al., 2016; Porter et al., 2020). While (11) implies a sensitivity of  $k_{xa}$  to molecular diffusivity, it turns out that the variation of atmospheric diffusivity amongst trace gases of interest is not significant (Rowe et al., 2011). Direct flux measurements of soluble trace gases to date (Yang et al., 2016; Porter et al., 2020) have shown some departures from water vapor or heat, but the measurement techniques are probably not sufficiently accurate to reject a simple water vapor analogy representation. The importance of air-side transfer declines as solubility declines. For DMS (solubility on the order of 15)  $k_{xa}$  contributes about 5% to (14) while for CO<sub>2</sub> (solubility on the order of 0.5) it contributes about 0.2%. For solubility greater than 100,  $k_{xa}$  dominates (14) and  $k_x/u_{*a} \approx k_{xa}/u_{*a} \approx 0.03$ .

On the ocean side of the interface the total transfer is assumed to be the sum of turbo-molecular,  $k_v$ , and bubble-mediated,  $k_b$ , processes:

$$k_w = k_v + k_b \quad (28)$$

The turbo-molecular part can be computed *via* (11) and (18) with the molecular sublayer part given by (21). The much smaller molecular diffusion coefficients in the ocean ( $Sc_x$  on the order of 1000 compared to 1 in the atmosphere) imply that most of the change in trace gas concentration on the ocean side occurs in the molecular transport sublayer. **Figure 2** contrasts the oceanic profiles for temperature ( $Sc_t = 5.9$ ) and CO<sub>2</sub> ( $Sc_w = 660$ ) at a water temperature of 20°C. The analytical solution is shown by the solid line and the log-layer portion by the dashed line. In this normalized form the log-layer slopes are the same but the offset caused by the molecular sublayer portion is relatively much

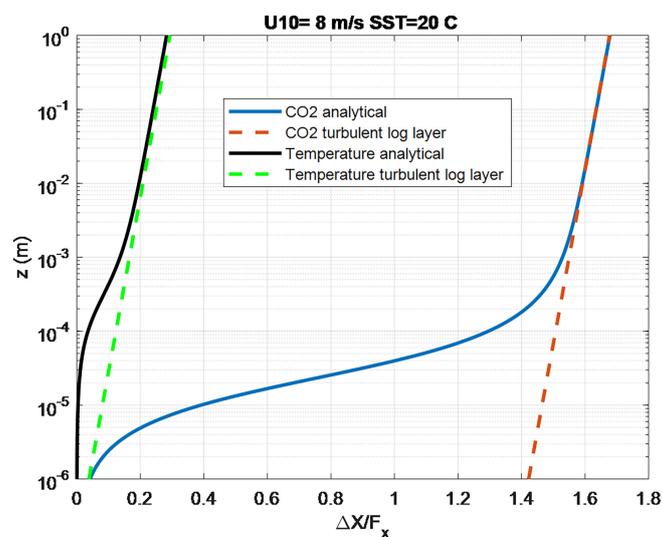


**FIGURE 1** | Wave stress fraction,  $\alpha_c$ , vs wave age,  $Cp/U_{10}$ , at different values of  $u = U_{10}$ . The lower curves correspond to lower wind speeds.

larger for  $CO_2$  – implying the computation of the flux for  $CO_2$  is much less sensitive to specification of the depth of the ocean side concentration measurement.

Bubble-mediated transfer is associated with air entrained by breaking waves. Wave breaking that entrains air rarely occurs in lighter wind regimes with a crude threshold of  $U_{10} \approx 5\text{--}8\text{ m s}^{-1}$ . Gas transfer enhancement by bubbles has been studied in laboratory experiments (Woolf, 1993; Rhee et al., 2007; Krall et al., 2019) and with numerical models (Woolf and Thorpe, 1991; Liang et al., 2013; Deike et al., 2017). The laboratory studies quoted here conflict somewhat on the importance of bubbles. The numerical model approach is based on injecting into the

ocean a numerical plume of bubbles with a spectrum of sizes. Gas transfer from the bubbles is computed for each bubble size as the plume rises and is vertically transported; total transfer is computed by integrating over the size spectrum. Turbulent mixing of the bubble plume may be neglected or can be very sophisticated (e.g., Liang et al. (2013) use a Large Eddy Simulation model). The variety of assumptions (injection depth, rise rate, bubble spectrum, bubble transfer rates, clean vs. dirty bubble, plume density, etc) lead to a variety of outcomes. Laboratory (Callaghan, 2013; Callaghan et al., 2016; Callaghan, 2018) and numerical modeling (Deike et al., 2016; Deike and Melville, 2018) have also advanced understanding of the



**FIGURE 2** | Normalized profiles of ocean temperature and  $CO_2$  concentration computed from the analytical solution (solid lines)  $K(z) = \kappa z u / (1 + \delta_s/z)$ . The dashed lines are using (21) to represent the turbulent log-layer part of the profile.

connection between wave breaking and dissipation, air entrainment, bubble populations, and whitecap coverage.

An example of a parameterization developed for bubble transfer can be found in Woolf (1993),

$$k_{xb} = BV_0 f_{wh} \alpha_x^1 [1 + (e\alpha_x Sc_{xw}^{1/2})^{-1/n}]^{-n} \quad (29)$$

where  $B$  is an empirical constant tuned to observations,  $V_0 = 2450 \text{ cm hr}^{-1}$  is the air volume entrainment flux per unit whitecap fraction,  $f_{wh}$  is the whitecap fraction,  $e = 14$ , and  $n = 1.2$ . This form is chosen so that the transfer velocity obeys the expected limits for low solubility (bubble mediated flux depends on the diffusion, but not on solubility) and high solubility (bubble mediated flux scales inversely with solubility). There is some debate about the scaling of the forcing in (29): should it be whitecap fraction, actively breaking fraction, air entrainment velocity ( $V$ ), or dissipation of wave breaking energy? The Woolf form assumes the scaling is  $V = V_0 f_{wh}$  with whitecap fraction scaling as  $U_{10}^{3.41}$  based on a fit to whitecap observations by Monahan (1971). Recent observations (Brumer et al., 2017b; Anguelova and Bettenhausen, 2019) have shown the Monahan formulation overestimates the wind-speed dependence which leads to overly large gas transfer estimates in high winds. Gas transfer versions of the COARE bulk transfer model, COAREG (Fairall et al., 2011), use (29) but Liang et al. (2013); Goddijn-Murphy et al. (2016), and Deike et al. (2017) offer viable alternatives to (29).

## 2.4 Chemical Enhancement

The COAREG models treat various gases with the assumption that they are conservatively transported. However, transfer of  $\text{CO}_2$  is complicated by carbonate chemical reactions on the water side – a phenomenon referred to as chemical enhancement. Hoover and Berkshire (1969) (hereafter HB69) express the chemical enhancement of  $\text{CO}_2$ , CE, as

$$\text{CE}(T) = \text{TT}/[(\text{TT} - 1) + \tanh(Q\delta)/(Q\delta)] \quad (30)$$

where, adapting the notation of Wanninkhof and Knox (1996), TT and Q depend on  $\text{CO}_2$ -carbonate reaction rate constants and diffusivity ( $D_{\text{CO}_2}$ ), and  $\delta = D_{\text{CO}_2}/k$  is diffusion layer thickness. Temperature dependence is explicit in TT and Q. Wind speed dependence is implied in  $\delta$  but no explicit functional form is given.

Wanninkhof (1992) (hereafter W92) considered this effect in the analysis of passive tracers to derive a formula for the enhanced transfer velocity for  $\text{CO}_2$   $k_{en660}$ . He uses a temperature-dependent but wind speed independent form for CE given by a polynomial fit,  $p(T)$ , to CE(T) at a constant  $k$  of  $1 \text{ cm hr}^{-1}$ .

$$k_{en660} = p(T) + 0.31 U_{10}^2 (Sc/660)^{1/2} \quad (31)$$

W92's formula gives  $p(T) = 3 \text{ cm hr}^{-1}$  in the tropics and  $2 \text{ cm hr}^{-1}$  for conditions relevant to the HiWinGS experiment (see Section 3.2). Wanninkhof and Knox (1996) define CE =  $k_{en}/k$  and examine the HB69 model with observations from several alkaline lakes and also estimate CE for the equatorial Pacific

Ocean. Note, this implies that as  $k_{en}/k$  approaches 1.0 with increasing winds, CE becomes small.

More recently, Fairall et al. (2007), hereafter F07, investigated air-sea transfer of ozone by considering the 1-dimensional conservation equation with a simple chemical reaction

$$-\frac{\partial}{\partial z} \left[ -D_x \frac{\partial X}{\partial z} + \overline{w'x'} \right] - a_r X = 0 \quad (32)$$

where flux is positive downward,  $X$  is the mean mass concentration and  $a_r = C_{xy}Y$  is the reactivity coefficient for the reaction of constituent  $X$  and constituent  $Y$  with a reaction rate constant of  $C_{xy}$ . F07 assumed ozone was completely destroyed in seawater and that the reactions are with unspecified oceanic chemicals in significantly large concentration such that the reaction is pseudo first-order in  $X$  and  $a_r$  is equivalent to a rate constant ( $s^{-1}$ ).

Here, we adapt this approach to  $\text{CO}_2$ . Following McGillis and Wanninkhof (2006), we assume the ocean mixed layer  $\text{CO}_2$  concentration,  $X_e$ , is in near equilibrium with carbonate chemistry. We assume that  $X_e$  is the result of a balance with total carbonate and alkalinity so that in the absence of significant temperature gradients it is essentially independent of depth. This is a more complex case than for ozone, but we again make the simplifying assumption that the reaction is pseudo first order in  $X_e$  and reactivity can be represented by a simple reactivity coefficient  $a_r$  ( $s^{-1}$ ) or time constant  $\tau_r = 1/a_r$  (s). The time constant is unknown but can be estimated from measurements. Thus, for a reactive gas in equilibrium like  $\text{CO}_2$ , (32) can be written

$$-\frac{\partial}{\partial z} \left[ -D_x \frac{\partial (X - X_e)}{\partial z} + \overline{w'x'} \right] - a_r (X - X_e) = 0 \quad (33)$$

The turbulent flux is represented in terms of turbulent diffusivity coefficient,  $K(z)$ , so that

$$-\frac{\partial}{\partial z} \left[ -(D_x + K(z)) \frac{\partial X'}{\partial z} \right] - a_r X' = 0 \quad (34)$$

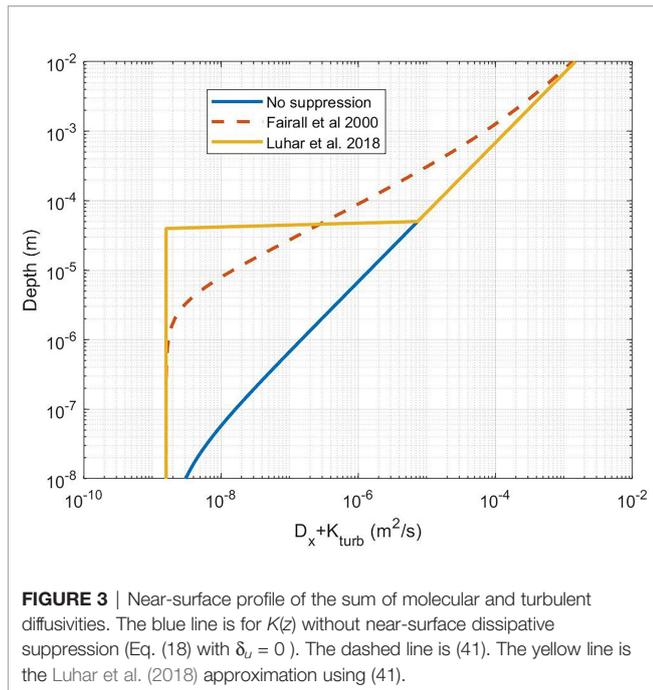
where  $X' = X - X_e$ . Following F07, we can use (34) to define a general flux variable,  $F_x$ , as

$$F_x = -[D_x + K(z)] \frac{\partial X'}{\partial z} - a_r \int_0^z X'(z') dz' \quad (35)$$

The gradient term expresses the sum of molecular and turbulent diffusion and the second term the gain or loss of  $X$  via chemical reaction. In steady state as expressed by (35),  $F_x$  is independent of depth and equal to the flux at the interface,  $F_x(0) = F_{xs}$ . For non-reactive gases, we can use (35) with  $a_r = 0$  to characterize the transport through the water

$$\frac{X'_s - X'(z)}{F_{xs}} = \frac{\Delta X_s(z)}{F_{xs}} = \int_0^z \frac{1}{D_x + K(z')} dz' = \frac{1}{k_{xw}} \quad (36)$$

Using the analytical solution (19) for the non-reactive case,  $k_{xw}$  represents the transfer velocity of  $x$  on the water side to some reference depth,  $z$ , on the order of 1 m. For  $a_r > 0$  an analytical solution corresponding to (34) with (18) does not exist.



**FIGURE 3** | Near-surface profile of the sum of molecular and turbulent diffusivities. The blue line is for  $K(z)$  without near-surface dissipative suppression (Eq. (18) with  $\delta_u = 0$ ). The dashed line is (41). The yellow line is the Luhar et al. (2018) approximation using (41).

Jørgensen et al. (2020) found solutions for (34) without the near-surface turbulence suppression. Another approach was developed by Luhar et al. (2018) who solved this problem by assuming that (18) could be approximated by setting the turbulent eddy diffusion coefficient to zero within some scale  $\delta_m$  of the surface (see **Figure 3**) and  $K(z) = \kappa z u_{*w}$  for  $z$  greater than  $\delta_m$ . Thus within a scalar molecular layer a stagnant (non-turbulent) film is assumed. If  $K(z)$  is set to 0 for  $z < \delta_m$ , the solutions of (34) with  $K(z) = 0$ , are exponentials. So the complete profile is given by

$$X = \begin{cases} A_1 \exp\left(\sqrt{\frac{a_r}{D_x}} z\right) + B_1 \exp\left(-\sqrt{\frac{a_r}{D_x}} z\right), & z \leq \delta_m \\ B_2 K_0(\xi), & z > \delta_m \end{cases} \quad (37a, 37b)$$

where  $A_1$ ,  $B_1$ ,  $B_2$  are constants and  $K_0$  is a modified Bessel function of order 0. Luhar et al. (2018) give an analytical expression for transfer velocity over some depth where chemical reactions become negligible

$$\frac{1}{k_{xw}} = \frac{1}{\sqrt{a_r D_x}} \left[ \frac{\psi K_1(\xi_\delta) \sinh(\lambda_m) + K_0(\xi_\delta) \cosh(\lambda_m)}{\psi K_1(\xi_\delta) \cosh(\lambda_m) + K_0(\xi_\delta) \sinh(\lambda_m)} \right] \quad (38)$$

where  $K_n$  are modified Bessel functions of order  $n$ ,  $\psi = [1 + \kappa u_{*w} \delta_m / D_x]^{1/2}$ ,  $\lambda_m = \delta_m (a_r / D_x)^{1/2}$ , and  $\xi_\delta$  is computed from

$$\xi_\delta^2 = \frac{4 a_r}{\kappa u_{*w}} \left( z + \frac{D_x}{\kappa u_{*w}} \right) \quad (39)$$

where  $z = \delta_m$  corresponds to the depth where the turbulent transport starts. Luhar et al. (2018) examined temperature dependent specifications for reactivity,  $a_r$ , and several candidates for  $\delta_m$ . Their final selections captured the modest temperature and weak wind speed dependencies of observed

ozone deposition velocity, but because ozone has very high reactivity they did not clearly delineate a value for  $\delta_m$ .

In order to choose the optimum value for  $\delta_m$ , we integrate (36) with the specified 2-layer  $K(z)$  profile with  $a_r = 0$  and select  $\delta_m$  to match the asymptotic form of the non-reactive analytical solution (21). This leads to

$$\delta_m = \delta_x = \frac{\pi}{2} \frac{\delta_u}{\sqrt{\lambda_u \kappa Sc}} = 0.79 \delta_u / Sc^{1/2} \quad (40)$$

In our view, this is a rigorous choice because it guarantees the same transfer velocity in the absence of chemical reactions.

We can use the 2-layer model to evaluate CE for  $\text{CO}_2$ . However, a more rigorous approach is a brute-force numerical solution to (34) with (18). One advantage of this approach is we can check and/or tune the 2-layer analytical model, which can give us an analytical function for CE in terms of the forcing and  $a_r$ . The numerical solutions are computed using MATLAB<sup>®</sup> differential equation solvers. With  $a_r = 0$ , the numerical solutions agreed with the non-reactive analytical solution (F00). Results for selected values of  $\tau_r$  are shown in **Figure 4** where we compute the enhancement ratio *via*

$$\frac{k_{en}}{k} = \frac{k(a_r)}{k(a_r = 0)} \quad (41)$$

The use of the ratio reduces the sensitivity to the calibration of  $k = k(a_r = 0)$ . We then compute CE as

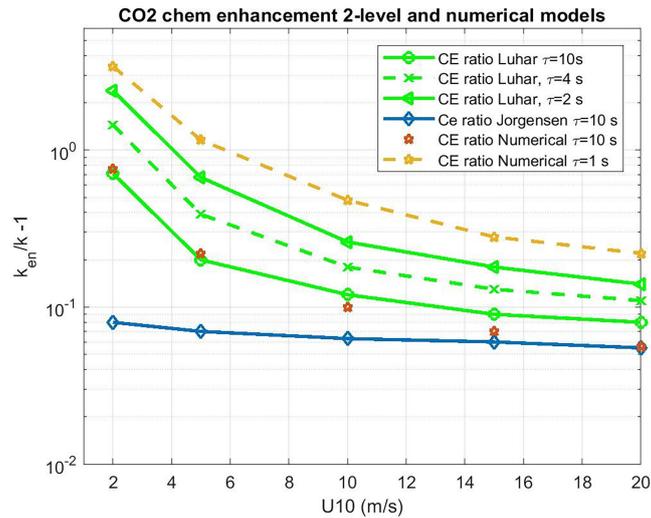
$$CE = \left( \frac{k_{en}}{k} - 1 \right) k_{c31x} \quad (42)$$

which is shown in **Figure 5**, where the COAREG 3.1 transfer velocity for gas  $x$ ,  $k_{c31x}$ , is the estimate for transfer without CE. The Luhar et al. (2018) analytical approximation is a good match with the numerical solution with our choice for  $\delta_m$ . This solution also works well for ozone. These calculations suggest CE of 3–5  $\text{cm hr}^{-1}$  for  $\text{CO}_2$  corresponding to a time constant,  $\tau_r$ , on the order of 3 s.

## 3 DIRECT OBSERVATIONS

### 3.1 Advances in DMS and $\text{CO}_2$ Flux Measurement

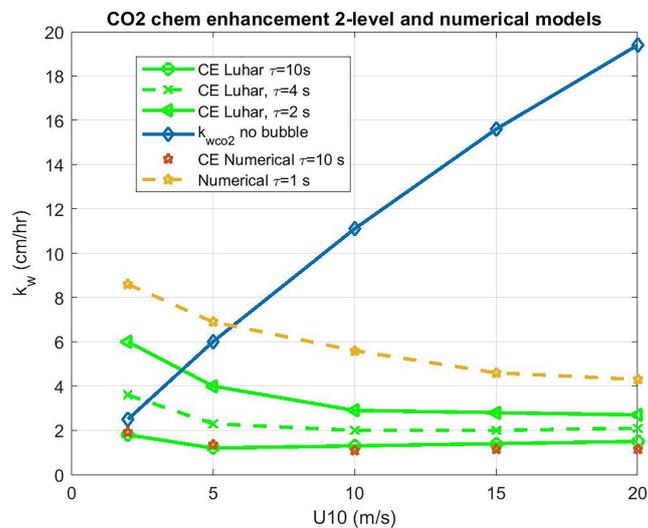
In this paper, we tune the latest revision of the model (COAREG 3.6) to direct gas exchange observations made with the eddy covariance (EC) method. The application of the EC method for measuring gas fluxes at sea requires high temporal resolution measurements of 1) vertical wind velocity, and 2) gas mixing ratio. The advent of the motion-correction method in late 1990s (Edson et al., 1998) enabled the derivation of the ambient vertical wind velocity from a moving platform. This method is subsequently refined by Miller et al. (2010); Landwehr et al. (2015), and Blomquist et al. (2017). Comparisons of momentum and heat fluxes between a buoy and a nearby fixed tower demonstrate that the bias due to the motion correction is within 6% (Flügge et al., 2016). For  $\text{CO}_2$ , we utilize fluxes



**FIGURE 4** | Water side transfer velocity (normalized to  $Sc = 660$ ) ratio of chemical enhanced to background value as a function of 10-m wind speed. Estimates of chemical enhancement (CE) via (42) for  $CO_2$  are shown with star symbols using a numerical integration of (34) and (19) and the analytical model (38) as green lines for different values of the  $CO_2$  carbonate reaction time constant,  $\tau_r$ . The results of the Jørgensen et al. (2020) are shown as diamonds.

measured using a closed-path instrument with a dryer. Deemed the best practice by Landwehr et al. (2014) and Blomquist et al. (2014), this approach avoids the water vapor cross-sensitivity in the  $CO_2$  measurement that likely confounded earlier flux measurements, especially using an open-path infrared analyzer [e.g., Edson et al. (2011)]. In particular, cavity ringdown analyzers (e.g., Picarro G2311-f) and closed-path infrared analyzers (e.g. Licor7200) are both well suited for measurements of air-sea  $CO_2$  flux. Recent works by Dong et al.

(2021) demonstrate that the random uncertainty in hourly  $CO_2$  flux is typically 30-50% (mostly a function of the flux magnitude), with sensor noise from both Picarro G2311-f and Licor7200 only contributing a minor fraction of the total flux uncertainty. Air-sea DMS flux measurement is made with a chemical ionization mass spectrometer operating at near atmospheric pressure. Hourly random uncertainty in DMS flux is on the order of 20-30% (Blomquist et al., 2010), thanks to the high signal-to-noise ratio in the DMS flux measurement.



**FIGURE 5** | Water side transfer velocity (normalized to  $Sc = 660$ ) as a function of 10-m wind speed. The basic COAREG non-bubble relationship for neutral conditions is shown in the blue diamonds. Estimates of chemical enhancement (CE) for  $CO_2$  are shown using a numerical model (stars) and an analytical model (green lines) for different values of the  $CO_2$  carbonate reaction time constant,  $\tau_r$ .

### 3.2 Recent Field Programs

The last decade has seen over a dozen field programs dedicated to EC gas flux measurements, with at least eight cruises and several near shore deployments. Long term EC measurements have been undertaken at two coastal sites. Östergarnsholm station is located in the Baltic Sea (57°27'N, 18°59'E) and has been providing CO<sub>2</sub> fluxes since 1995 (Rutgersson et al., 2020). Penlee Point Atmospheric Observatory (PPAO) was established in 2014 by the Plymouth Marine Laboratory in the Plymouth Sound on the south-west coast of the United Kingdom (50°19.08'N, 4°11.35'W). It provides CO<sub>2</sub>, CH<sub>4</sub> fluxes (<https://www.westernchannelobservatory.org.uk/penlee>, Yang et al. (2016)). A list of all recently collected and analysed EC field measurements is given in **Table 1** along with references to relevant publications.

In this paper we focus on results from three recent campaigns (Knorr11 in 2011, SOAP in 2012, HiWinGS in 2013), where simultaneous air-sea exchange measurements of CO<sub>2</sub> and DMS are available. Some published direct measurements of DMS  $k_{660}$  have shown unexpected decreases at higher wind speeds: GasEx08 (Blomquist et al., 2017), Knorr11 (Bell et al., 2013; Bell et al., 2017), and Sonne-234/235 (Zavarsky and Marandino, 2019). This was discussed in depth by Zavarsky and Marandino (2019) and explained in terms of flow separation using a wave reference Reynolds number,  $Re_{tr}$ . The argument is that flow separation (which occurs when  $Re_{tr} < 6.5E6$ ) suppresses the direct viscous transfer component and this affects DMS relatively more than CO<sub>2</sub> because the much larger bubble transfer for CO<sub>2</sub> masks the decrease. The basic idea has some logic, although Zavarsky et al. (2018) Figure 13 shows no dramatic decrease in DMS  $k_{660}$  for HiWinGS despite a large fraction of suppressed conditions for  $U_{10} > 12 \text{ m s}^{-1}$ . In our own analysis of HiWinGS

data, using their  $Re_{tr}$  criterion, we find no significant difference in  $k_{660}$  for DMS in suppressed vs. non-suppressed conditions, but CO<sub>2</sub>  $k_{660}$  is reduced by about 10 cm h<sup>-1</sup> during 'suppressed' conditions. It seems the sudden decrease in  $k_{660}$  DMS in strong winds observed in some field programs remains puzzling.

## 4 ANALYSIS OF OBSERVATIONS IN A COARE CONTEXT

### 4.1 Turbo-Molecular and Bubble-Mediated Drivers

The last public release of the COARE algorithm, version 3.1 (Fairall et al., 2011), does not include CE and gives a simple form for the transfer velocity (14) which captures the net transfer across water ( $w$ ) and atmospheric ( $a$ ) surface layers. We can separate the oceanic and atmospheric components as follows

$$k_w = \left(1 + \frac{\alpha_x k_w}{k_a}\right) k = k_v + k_b \quad (43)$$

From measurements of  $k$ , we can compute the oceanside value,  $k_w$ , which is made up of a turbulent-molecular term,  $k_v$ , and a bubble-mediated term,  $k_b$ . For HiWinGS the term multiplying  $k$  in (43) is an average of 1.054 for DMS and 1.008 for CO<sub>2</sub>. Following Appendix A of Fairall et al. (2011), we can convert  $k_w$  to  $k_{660}$  and write (43) as

$$k_{w\ 660} \cong k_{v\ 660} + k_{b\ 660} \\ = 37.5 A u_{*v} + \frac{B V_0 f_{wh}}{\alpha_x(20)} \gamma(T) G(T) \quad (44)$$

**TABLE 1** | Recent field campaigns.

Year	Program	Region	Gas Measured	Platform	References
2011-2012	FINO-2 tower	western Baltic	CO <sub>2</sub>	T	Ghobadian and Stammer (2019)
2011	Knorr11	North Atlantic	CO <sub>2</sub> , DMS	S	Bell et al. (2013, 2017); Esters et al. (2017)
2012	SOAP	southwest Pacific/Southern Ocean	CO <sub>2</sub> , DMS	S	Landwehr et al. (2018)
2013	HiWinGS	North Atlantic	CO <sub>2</sub> , DMS, methanol, acetone	S	Yang et al. (2014); Blomquist et al. (2017); Brumer et al. (2017a)
2014	Arctic fjords	Adventfjorden (flux tower)	CO <sub>2</sub>	T	Andersson et al. (2017)
	NBP-1210	MIZ, Southern Ocean (Punta Arenas to McMurdo)	CO <sub>2</sub>	S	Butterworth and Miller (2016)
	ACSE (SWERUS-C3)	(2 legs) Arctic MIZ at edge of the Siberian shelf: Kara, Laptev, East Siberian, and Chukchi Seas	CO <sub>2</sub>	S	Prytherch et al. (2017)
	NBP-1402	MIZ, Southern Ocean	CO <sub>2</sub>	S	Butterworth and Miller (2016)
	PPAO	south-west coast of the United Kingdom	CO <sub>2</sub> , CH <sub>4</sub>	T	Yang et al. (2016)
2014-2015	SPACES-OASIS (SO234-2/235)	western tropical Indian Ocean	CO <sub>2</sub> , DMS	S	Zavarsky et al. (2018); Zavarsky and Marandino (2019)
		Scripps Pier, La Jolla, California	SO <sub>2</sub>	P	Porter et al. (2018)
		Östergarnsholm + SAMI-CO <sub>2</sub>	CO <sub>2</sub>	T	Vieira et al. (2020)
2015		Duck USACE-FRF pier, North Carolina	SO <sub>2</sub>	P	Porter et al. (2020)
2017-2018	Östergarnsholm station	Baltic Sea	CO <sub>2</sub> , CH <sub>4</sub>	T	Gutiérrez-Loza et al. (2019)
2018-2019	AMT4OceanSatFlux	Atlantic Meridional Transect	CO <sub>2</sub>	S	
2018-2019	ice camp Arctic Ocean 2018	open lead close to North Pole	CO <sub>2</sub>	T	Prytherch and Yelland (2021)

Platforms: ship (S), tower (T), pier (P).

Here the first term on the right hand side represents tangential (interfacial) transfer, while the second term indicates bubble-mediated gas exchange (see Eq. 29).  $A$  and  $B$  are parameters tuned to fit the observations and the temperature- and gas-dependent factors are

$$\gamma(T) = \left[ \frac{Sc_w}{660} \right]^{1/2} \frac{\alpha_x(20)}{\alpha_x(T)} \quad (45a)$$

$$G(T) = [1 + (14 \alpha_x / Sc_w^{1/2})^{-1/n}]^{-n} \quad (45b)$$

with  $n = 1.2$ . In (44) we have neglected buoyancy effects on the first term, which become more important at wind speeds less than  $5 \text{ m s}^{-1}$ . Note that in COAREG,  $k_v$  is scaled by *viscous*, rather than total, friction velocity.

We can now consider the form of (44) for both  $\text{CO}_2$  (subscript  $c$ ) and DMS (subscript  $d$ ) with the temperature dependent factors in  $k_b$ ,  $V_0$  and  $\alpha(20)$  combined into the single factors  $b_c$  and  $b_d$

$$k_{c \ 660} = 37.5 \ A \ u_{*v} + B \ b_c \ f_{wh} \quad (46a)$$

$$\begin{aligned} k_{d \ 660} &= 37.5 \ A \ u_{*v} + B \ b_d \ f_{wh} \\ &= 37.5 \ A \ u_{*v} + B \ r_{dc} \ b_c \ f_{wh} \end{aligned} \quad (46b)$$

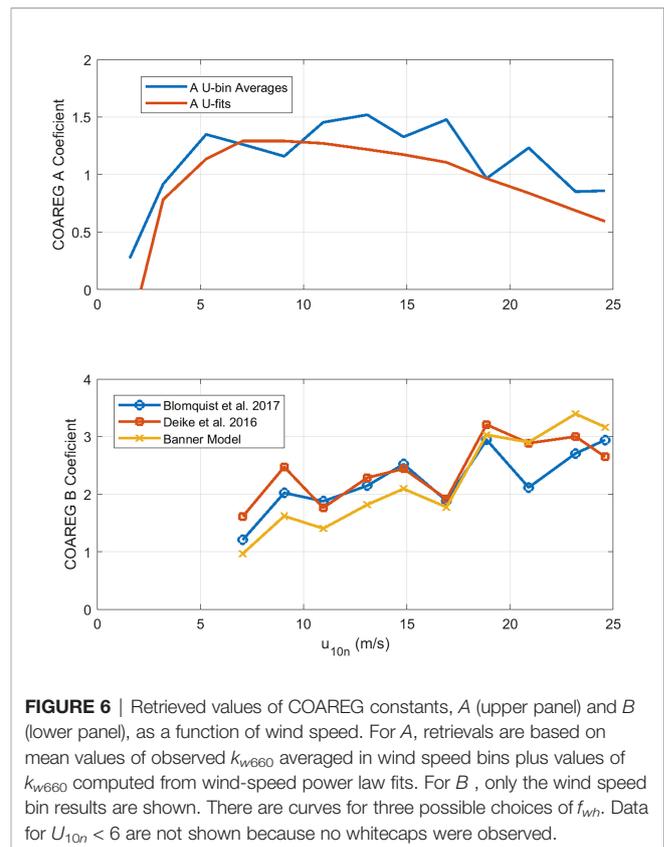
If  $k$  values are expressed in  $\text{cm hr}^{-1}$ , then the factor  $b_c \cong 830$ , while  $b_d = 130 + 2.6T$  where  $T$  is in  $^\circ\text{C}$ . Thus, the ratio between bubble-mediated gas exchange of DMS and that of  $\text{CO}_2$ ,  $r_{dc} = b_d/b_c$ , in (46b) varies from 0.16 to 0.22 with an average of 0.18 for HiWinGS. The relationships in (46) can be applied to observations of  $k$  for  $\text{CO}_2$  and DMS to estimate the constants  $A$  and  $B$ :

$$A = \frac{(k_{w660d} - r_{dc} k_{w660c})}{37.5 \ u_{*v} (1 - r_{dc})} \quad (47a)$$

$$B = \frac{(k_{w660c} - k_{w660d})}{830 \ f_{wh} (1 - r_{dc})} \quad (47b)$$

Note (47) is approximate because it uses mean values for T-dependent factors, but if (47) is applied to  $k_w$  values computed with the COAREG algorithm, then for a 10-m wind speed adjusted to neutral conditions,  $U_{10n} > 5 \text{ m s}^{-1}$ , the values for  $A$  and  $B$  assumed in the algorithm will be recovered within 10%. Also, note that the value of  $A$  depends on the form of the friction velocity factor and  $B$  depends on choice of whitecap formulation. If the model and the measurements are consistent, then the values of  $A$  and  $B$  should be independent of wind speed.

**Figure 6** shows values of  $A$  and  $B$  extracted from HiWinGS observations averaged in wind speed bins. To reduce the effects of flux sampling uncertainty, values of  $\text{CO}_2$  transfer velocities were only used if the absolute value of sea-air partial pressure difference  $\Delta p_{\text{CO}_2}$  exceeded  $20 \ \mu\text{atm}$ . Two retrievals have been done: 1) with bin averages of measured  $k_{w660}$  and 2) using power-law fits of  $k_{w660}$  to wind speed in the form



**FIGURE 6** | Retrieved values of COAREG constants,  $A$  (upper panel) and  $B$  (lower panel), as a function of wind speed. For  $A$ , retrievals are based on mean values of observed  $k_{w660}$  averaged in wind speed bins plus values of  $k_{w660}$  computed from wind-speed power law fits. For  $B$ , only the wind speed bin results are shown. There are curves for three possible choices of  $f_{wh}$ . Data for  $U_{10n} < 6$  are not shown because no whitecaps were observed.

$$k_{w \ 660} = c_0 + c_1 \ U_{10n}^m \quad (48)$$

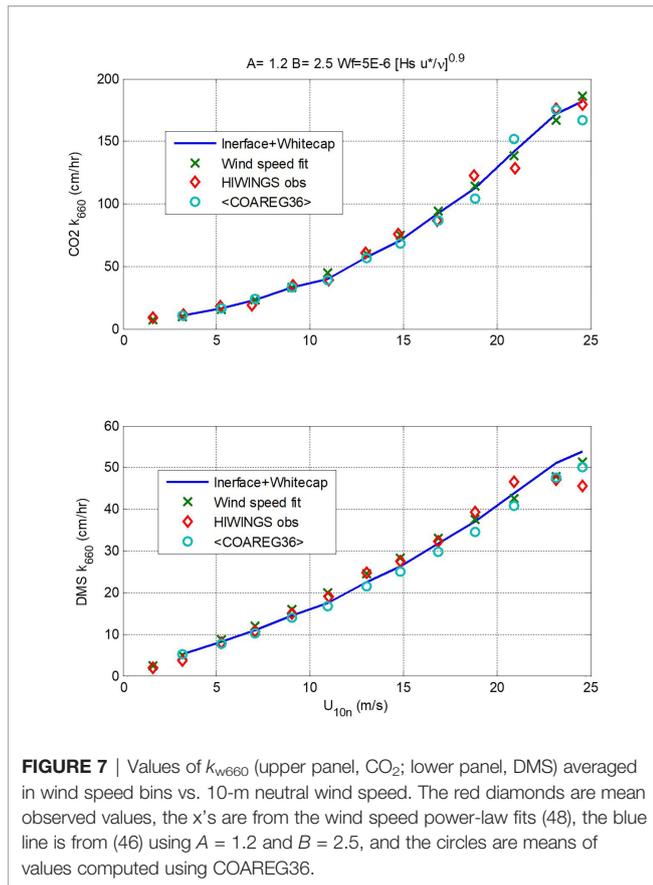
We have used  $c_0 = 6.0$ ,  $c_1 = 0.41$ , and  $m = 1.9$  for  $\text{CO}_2$ ;  $c_0 = 0.6$ ,  $c_1 = 1.09$ , and  $m = 1.2$  for DMS. To compute  $B$  (47b), both retrievals used bin-averaged estimates of whitecap fraction computed from Brumer et al. (2017b)

$$f_{wh} = 5.0 \times 10^{-6} \left[ \frac{H_s u_{*a}}{V_w} \right]^{0.9} \quad (49)$$

Averaging both retrieval methods yields  $A = 1.25$  and  $B = 2.3$ , using (49) for whitecap fraction. We have also used bin-averaged values of observed  $f_{wh}$ ; that yields noisier results but does not significantly change the final estimates of  $A$  and  $B$ .

In **Figure 7** we show a comparison of transfer velocities averaged in wind speed bins from the three calculation methods: linear+bubble (46); wind speed power law (48); and a new version of COAREG using these values of  $A$  and  $B$  and the Brumer et al. (2017b) whitecap formulation – we are referring to this as COAREG36. A summary of the mean and RMS statistics is given in **Table 2**. Since the power law is fit directly to the mean observations, it gives the best overall fit.

So far our specification of total gas transfer velocity (46) requires the turbo-molecular term to scale with  $u_{*v}$  and the bubble-mediated term to scale with  $f_{wh}$ . It is insightful to reevaluate the turbo-molecular and bubble terms separately without specifying the nature of the forcing. So we recast (47) without the  $u_{*v}$  and  $f_{wh}$  factors but assume the forcing will have some wind speed dependence:



**FIGURE 7** | Values of  $k_{w660}$  (upper panel,  $\text{CO}_2$ ; lower panel, DMS) averaged in wind speed bins vs. 10-m neutral wind speed. The red diamonds are mean observed values, the x's are from the wind speed power-law fits (48), the blue line is from (46) using  $A = 1.2$  and  $B = 2.5$ , and the circles are means of values computed using COAREG36.

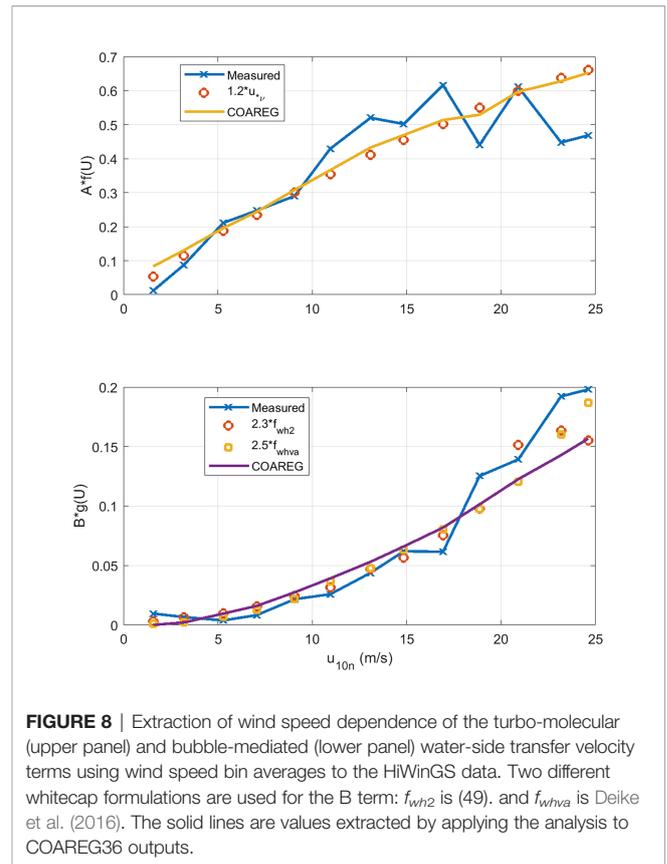
$$A \ f(U) = \frac{(k_{w660d} - r_{dc} \ k_{w660c})}{37.5 \ (1 - r_{dc})} \quad (50a)$$

$$B \ g(U) = \frac{(k_{w660c} - k_{w660d})}{830 \ (1 - r_{dc})} \quad (50b)$$

The results are shown in **Figure 8** as a function of 10-m wind speed. Also shown on the graphs are the COAREG forms for the forcing:  $f(U) = u_{*v}$  and  $g(U) = f_{wh}$ . We can see that the turbo-molecular term is nearly linear with the viscous stress and showing a hint of saturation at higher winds speeds. This could imply that our parametrization of viscous stress is too high and our parameterization underestimates the importance of the wave stress component at high winds speeds. The bubble-mediated term has a much stronger wind speed dependence and is well represented by the whitecap parameterization.

**TABLE 2** | Summary of mean  $k_{660}$  ( $\text{cm hr}^{-1}$ ) and RMS difference from mean HIWINGS measurements.

	$\text{CO}_2$		DMS	
	Mean	RMS	Mean	RMS
Observation	73.9	0	24.7	0
Interface + Whitecap	80.6	6.2	28.2	3.3
Power-law	74.4	6.5	25.3	2.2
COAREG36	75.2	10.1	24.8	2.8



**FIGURE 8** | Extraction of wind speed dependence of the turbo-molecular (upper panel) and bubble-mediated (lower panel) water-side transfer velocity terms using wind speed bin averages to the HIWINGS data. Two different whitecap formulations are used for the B term:  $f_{wh2}$  is (49), and  $f_{whva}$  is Deike et al. (2016). The solid lines are values extracted by applying the analysis to COAREG36 outputs.

## 4.2 Chemical Enhancement

We can use observations of  $\text{CO}_2$  and DMS transfer velocity to estimate CE if the difference between  $\text{CO}_2$  and dual tracer is due to chemical enhancement only by adding a term to (46)

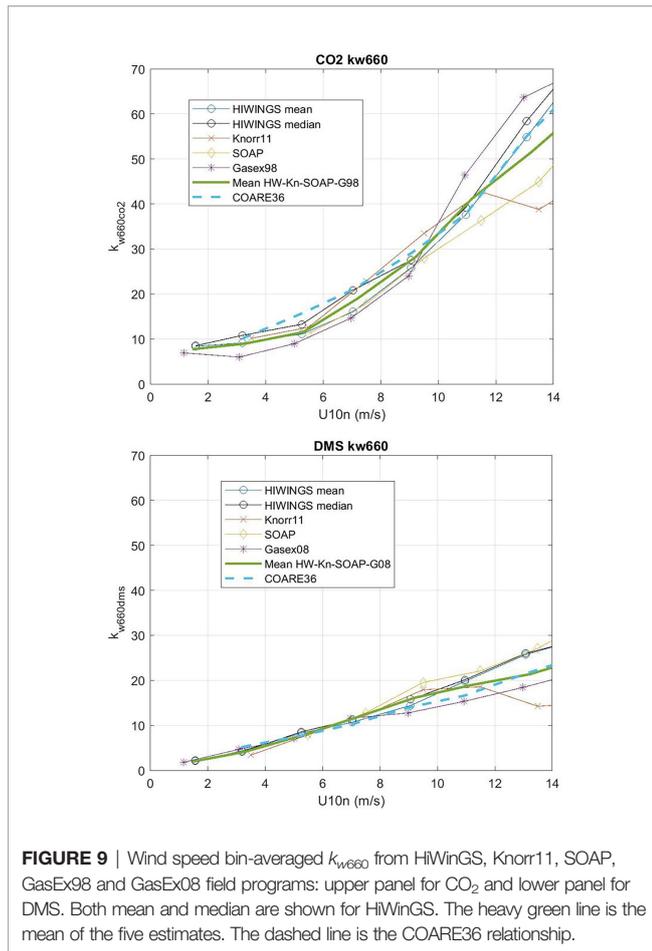
$$k_{c660} = \text{CE} + 37.5A u_{*v} + B b_c f_{wh} \quad (51)$$

$$k_{d660} = 37.5A u_{*v} + B r_{dc} b_c f_{wh} \quad (52)$$

Taking the difference gives

$$k_{c660} - k_{d660} = \Delta k = \text{CE} + B \ (1 - r_{dc}) \ b_c f_{wh} \quad (53)$$

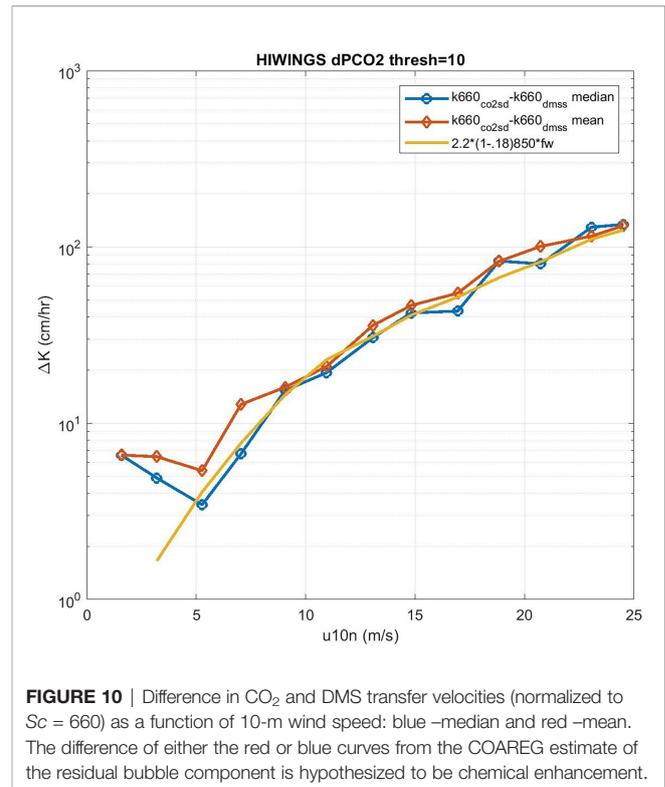
We can solve (53) for CE but we expect the values of CE will be the difference between two large numbers except at low wind speeds. In order to reduce the effect of sampling uncertainty, we have added data from four additional field programs –  $\text{CO}_2$  from GasEx98, SOAP, and Knorr11 and DMS from SO-GasEx, SOAP, and Knorr11 – to the ensemble of data and produced a grand average for  $\text{CO}_2$  and DMS transfer velocities (see **Figure 9**). In the case of GasEx98,  $\text{CO}_2$  fluxes were determined with a closed path system that lacked a drier but used a long inlet. This tends to eliminate water vapor concentration variance and may be less affected by flux cross-talk than open path sensors. For  $U_{10} < 10 \text{ m s}^{-1}$ , the uncertainty in these averages is  $\pm 2.0 \text{ cm hr}^{-1}$  for  $\text{CO}_2$  and  $\pm 0.4 \text{ cm hr}^{-1}$  for DMS. The uncertainty in  $\Delta k$  is essentially that of  $\text{CO}_2$ . In **Figure 10** we show  $\Delta k$  as a function of  $U_{10}$  with separate curves for mean and medians of the four-experiment ensemble;



we also show the bubble driven component [second term on RHS of (53)]. The data clearly imply values of CE on the order  $4\text{--}6\text{ cm hr}^{-1}$  at the lowest wind speeds but even at  $U_{10} = 5\text{ ms}^{-1}$  it is doubtful the difference between observations of  $\Delta k$  and the estimates of the bubble component are significant. This result is similar to (Yang et al., 2022) who computed a grand-averaged  $k_{c660}$  from eight field programs (including the ones used here) and estimate CE by differencing their average with dual tracer estimates of  $k_{c660}$  (Ho et al., 2006). Because the dual tracer studies are done with non-reactive gases, the argument is that they do not include  $\text{CO}_2$  CE. Yang et al. (2022) found CE values of about  $4\text{ cm hr}^{-1}$  for  $U_{10} < 10\text{ m s}^{-1}$ . These results suggest  $\tau_r$  on the order of  $3\text{ s}$  ( $a_r = 0.33$ ) should be used in (38) to estimate CE if the difference between  $\text{CO}_2$  and dual tracer is due to chemical enhancement only.

## 5 DISCUSSION AND CONCLUSIONS

In this paper we analyze concurrent observations of  $\text{CO}_2$  and DMS fluxes and ocean-side transfer velocity from three recent field programs. We emphasize the HiWinGS program because it has the broadest range of wind speeds and multiple systems of high quality covariance flux instrumentation. We frame our



analysis in terms of the COAREG gas flux algorithm, which treats the ocean-side transfer as the sum of direct interfacial and bubble-mediated transfer mechanisms. We assume the interfacial transfer component scales as the square root of the Schmidt number and is driven linearly by the viscous friction velocity. The total surface stress is partitioned into viscous and wave contributions with the fraction going to viscous stress decreasing with increasing wind speed. COAREG scales the bubble-mediated component with whitecap fraction (Woolf, 1993) with additional temperature-dependent sensitivity to Schmidt number and solubility. Whitecap fraction is difficult to measure so parametrizations are uncertain, but whitecap fraction is only one of several possible choices to characterize the wave breaking contribution to bubble-mediated exchange (other possibilities include air entrainment rate or wave energy dissipated by breaking).

The analysis focuses on determination of the tuning constants  $A$  and  $B$ , which scale with the viscous and bubble-mediated terms. We use (47) to compute values of  $A$  and  $B$  in wind-speed bins. Note the value of  $A$  obtained from (47a) is independent of the formulation of whitecap scaling and  $B$  obtained via (47b) is independent of the formulation of the forcing of the viscous term. The wind speed dependence of  $A$  and  $B$  depends on the wind speed dependence of the forcing terms. The values of  $A$  and  $B$  determined from these data are essentially independent of wind speed for the chosen forcing: linear with  $u_{*v}$  and with a particular whitecap formulation. At low wind speeds, there are departures for both  $A$  and  $B$  that we associate with the effects of chemical enhancement of  $\text{CO}_2$  transfer, which are not captured in (47). CE is discussed theoretically in section 2.4 and a

parameterization is presented. In section 4.2 we exploit the difference in CO<sub>2</sub> and DMS transfer velocities to estimate CE – the result is noisy (**Figure 10**) but values are comparable to Wanninkhof (1992) and (Zheng et al., 2021).

The product of this effort is version 3.6 of the COARE flux algorithm – COAREG 3.6 which is available at [https://downloads.psl.noaa.gov/BLO/Air-Sea/bulkalg/cor3\\_6/gasflux36/](https://downloads.psl.noaa.gov/BLO/Air-Sea/bulkalg/cor3_6/gasflux36/) (See the Supplement to this paper for more detail on the update). The algorithm incorporates a modern whitecap formulation that allows either pure wind speed or wave-dependent scaling. Chemical enhancement for CO<sub>2</sub> *via* (38) is included as an option. Wave dependence of the stress has also been updated.

## DATA AVAILABILITY STATEMENT

Publicly available datasets were analyzed in this study. This data can be found here: [https://downloads.psl.noaa.gov/psd3/cruises/HiWINGS\\_2013/Fairall\\_etal\\_2022\\_Frontiers\\_Paper/](https://downloads.psl.noaa.gov/psd3/cruises/HiWINGS_2013/Fairall_etal_2022_Frontiers_Paper/). Version 3.6 of the COARE flux algorithm (COAREG 3.6) is available at: [https://downloads.psl.noaa.gov/BLO/Air-Sea/bulkalg/cor3\\_6/gasflux36/](https://downloads.psl.noaa.gov/BLO/Air-Sea/bulkalg/cor3_6/gasflux36/).

## AUTHOR CONTRIBUTIONS

CWF wrote the first draft of the manuscript, MY and SEB each contributed a subsection. CWF, BWB, and MY revised the manuscript following the peer review process. JBE, CJZ, TGB, ESS, and SEB participated in discussions and provided edits. CWF, BWB, MY, SEB, LB, and CJZ participated in the HiWinGS experiment. TGB and ESS participated in the Knorr11 and SOAP experiment. JBE, CWF, and CJZ participated in the GasEx98 experiment. BB, LB, JBE, and CJZ participated in the SO-GasEx experiment. LB performed the numerical simulations with DE equation solver. SP and LB provided technical support

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## SUPPLEMENTARY MATERIAL

The Supplementary Material for this article can be found online at: <https://www.frontiersin.org/articles/10.3389/fmars.2022.826606/full#supplementary-material>

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