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# Macroalga *Ulva prolifera* O.F. Müller: an efficient biofilter for nitrogen-enriched aquaculture effluents

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**Introduction:** *Ulva prolifera*, a dominant species in green tides, exhibits remarkable nitrogen absorption capacity, yet its kinetics as a biofilter in recirculating aquaculture systems (RAS) remain unquantified.

**Methods:** This study systematically characterized NH<sub>4</sub><sup>+</sup>-N, NO<sub>3</sub><sup>-</sup>-N, and NO<sub>2</sub><sup>-</sup>-N uptake kinetics in nitrogen-starved (7-day). *U. prolifera* across eight concentration gradients (NH<sub>4</sub><sup>+</sup>-N: 0.5–35  $\mu$ mol·L<sup>-1</sup>; NO<sub>3</sub><sup>-</sup>-N: 5–130  $\mu$ mol·L<sup>-1</sup>; NO<sub>2</sub><sup>-</sup>-N: 2.5–60  $\mu$ mol·L<sup>-1</sup>).

**Result:** Michaelis-Menten modeling revealed: NO $_3$ -N achieved the highest maximum uptake rate (V<sub>max</sub> = 161.29 µmol·g<sup>-1</sup>·h<sup>-1</sup>), but the greatest half-saturation constant (K<sub>m</sub> = 29.40 µmol·L<sup>-1</sup>); NH $_4$ +-N showed the strongest affinity (K<sub>m</sub> = 4.60 µmol·L<sup>-1</sup>); NO $_2$ -N absorption plummeted at >50 µmol·L<sup>-1</sup> (41% removal after 6h). When the initial concentrations were below 20 µmol·L<sup>-1</sup> for NH $_4$ +-N, or below 90 µmol·L<sup>-1</sup> NO $_3$ --N, or below 20 µmol·L<sup>-1</sup> for NO $_2$ --N, 1g of *Ulva prolifera* in 1 L of seawater completely achieving 100% removal efficiency for each within 6 hours. Critical inhibition thresholds were identified: NH $_4$ +-N >20 µmol·L<sup>-1</sup> reduced removal by 40–60%, NO $_3$ --N >110 µmol·L<sup>-1</sup> induced suppression, and NO $_2$ --N >30 µmol·L<sup>-1</sup> triggered acute inhibition.

**Conclusion:** We propose optimized RAS protocols: maintain NH<sub>4</sub><sup>+</sup>-N  $\leq$ 20  $\mu$ mol·L<sup>-1</sup> and NO<sub>2</sub><sup>-</sup>-N  $\leq$ 30  $\mu$ mol·L<sup>-1</sup>, with 1.5–2× increased algal biomass when high total inorganic nitrogen concentration to sustain >90% nitrogen removal. This work demonstrates *U. prolifera*'s nitrogen assimilation strategy—"high ammonium affinity, high nitrate capacity, nitrite sensitivity"—providing a mechanistic foundation for valorizing green-tide macroalgae in sustainable aquaculture.

KEYWORDS

RAS, Ulva prolifera, nitrogen absorption kinetics, eutrophication, biofilter, green tide

#### 1 Introduction

Despite rising food production, global hunger persists, affecting over 700 million people in 2023 (FAO, 2024). Meeting growing food demand sustainably is a critical challenge (Ahmed et al., 2019). Aquaculture has become vital, providing essential high-quality protein and trace elements to meet population needs, especially as capture fisheries decline due to overfishing and pollution (Li et al., 2023; Yan et al., 2021). Marine resources provide more extensive space, lower carbon footprints, stronger water currents, and faster pollutant dispersion than freshwater systems. With these advantages and the higher added value of marine aquaculture products, this sector has emerged as the dominant source of aquatic products (Shen et al., 2024). However, intensified highdensity practices, while productive, cause significant environmental impacts through extensive methods and poor feed management (Verdegem, 2013). China is a major aquaculture country, with its aquaculture output accounting for more than half of the global total, a trend that has raised concerns about water environmental safety (FAO, 2019). In fact, between 2006 and 2017, as China fish and shellfish production increased from 30 to 47 million tons (Mt), nitrogen (N) releases rose from 1.0 to 1.6 Mt/year, while phosphorus (P) releases increased from 0.1 to 0.2 Mt/year (Ahmed et al., 2019). The level of eutrophication in the coastal waters is gradually increasing, accompanied by algal blooms such as "red tides", "brown tides", "green tides" and "golden tide" (Kong et al., 2012; Song et al., 2022; Sun et al., 2024; Zhang et al., 2019). In conclusion, achieving sustainable expansion of aquaculture operations while ensuring environmentally friendly practices has emerged as a critical contemporary priority.

Intensive aquaculture operations currently require substantial inputs of chemical supplements such as feed and fertilizers. These substances are not fully utilized by farmed organisms, while metabolic processes of organisms generate additional waste, collectively contributing to environmental impacts (Turcios and Papenbrock, 2014). Aquaculture effluent contains elevated nitrogen and phosphorus concentrations that drive eutrophication and promote harmful algal blooms (Sun et al., 2024; Wang et al., 2018, Wang et al., 2020). Recently, recirculating aquaculture systems (RAS) have emerged as a validated solution for effective wastewater treatment (Cahill et al., 2010; van Rijn, 2013). Crucially, RAS operates independently of natural environmental constraints, enabling the cultivation of diverse species irrespective of their native distribution or habitat requirements (Ahmed and Turchini, 2021; Dalsgaard et al., 2013). However, the accumulation of nitrogenous waste represents a critical constraint affecting the sustained operation of RAS. Such waste primarily comprises nitrate, nitrite, and ammonium nitrogen (Nelson et al., 2001). Notably, ammonium nitrogen exhibits both acute and chronic toxicity to aquatic species and constitutes a primary constraint on system functionality (Cahill et al., 2010; Randall and Tsui, 2002). Implementing effective filtration or purification methods is therefore essential for ensuring the long-term viability of RAS. Macroalgae are proposed as biofilters in RAS due to their superior nitrogen uptake efficiency compared to conventional filter membranes (Mangott et al., 2020),

while offering significant potential for carbon dioxide sequestration to support climate change mitigation (Ahmed and Turchini, 2021; Goddek et al., 2015). In addition, cultivated macroalgae in RAS can be harvested as valuable aquaculture products (e.g., food or bioresources), thereby improving overall RAS profitability.

Macroalgae perform well in the process of aquaculture wastewater treatment, especially species of Ulva and Gracilaria, which are the most commonly used genera in RAS biological filtration (Lavania-Baloo et al., 2014). Specific species such as Ulva lactuca, Ulva rigida, Ulva fasciata, Gracilaria conferta, Gracilaria vermiculophylla, Gracilaria chilensis, Gracilaria bursapastoris have been applied in offshore or land-based Multi-Trophic Aquaculture (IMTA) systems (Lothmann and Sewilam, 2023). Moreover, Kappaphycus alvarezii (Hayashi et al., 2008), Gracilariopsis longissima (He et al., 2014), Caulerpa lentillifera (Bambaranda et al., 2019), kelps (e.g., Nereocystis luetkeana; (Supratya and Martone, 2024), Sargassum siliquosum (Edwards et al., 2024) have received increasing attention. In recent years, Ulva prolifera (U. prolifera) has garnered significant research interest due to its exceptional capacity for nitrogen and phosphorus assimilation, combined with its frequent bloom events (Xia et al., 2024). Since 2008, recurrent green tide events in the Southern Yellow Sea of China have necessitated substantial resource allocation for shoreline cleanup of macroalgal deposits (Sun et al., 2022). The accumulation of drifting algae along coastlines (driven by ocean currents and tidal dynamics) has disrupted local aquaculture operations, resulting in significant economic losses (Liu et al., 2022). As the dominant species in green tide events, U. prolifera demonstrates significantly superior nitrogen and phosphorus absorption, enrichment, and assimilation capabilities compared to other macroalgae (Wu et al., 2025a). This proven physiological capacity qualifies it as a promising biofilter material for treating aquaculture wastewater, particularly in RAS. However, the research on the effects of different initial concentrations of nitrogen and different forms of nitrogen on the absorption rate of *U. prolifera* is still insufficient. This study aims to (1) analyze the adsorption kinetics and nitrogen source preference (NH<sub>4</sub>, NO<sub>2</sub> and NO<sub>3</sub>) of *U. prolifera* at varying initial concentrations, (2) quantify its nitrogen removal capacity from aquaculture effluents, and (3) provide foundational data to advance IMTA systems.

#### 2 Materials and methods

#### 2.1 Material sources and pretreatment

The green algae (*U. prolifera*) was obtained from the Algal Laboratory of the Water Environment & Ecology Engineering Research Center of Shanghai Institution of Higher Education at Shanghai Ocean University. It was collected during the green tide outbreak in 2021 from the coastal waters near Qingdao, Shandong Province (36°3′48″N, 120°23′34″E), preserved in ice boxes, and transported to the laboratory within 48 hours for processing. After isolation and purification, the strain was preserved in the

laboratory. Subsequently, molecular identification was conducted on the algae. Internal transcribed spacer (ITS) sequences and 5S ribosomal deoxyribonucleic acid (5S rDNA) spacer sequences were chosen for species identification, and the algal species was identified as *Ulva prolifera* (sequencing data can be found in the Supplementary Materials).

For large-scale cultivation, *U. prolifera* was pre-cultured in 1 L custom-made round glass containers. The culture medium consisted of artificial seawater prepared using sea salt crystals (Lanhongxing brand, Haiding Technology, Shanghai), which was filtered, sterilized, and supplemented with VSE nutrients, with a salinity of 24  $\pm$  0.2 psu. Cultivation conditions were as follows: temperature 22  $\pm$  1°C, light intensity 90  $\mu$ mol·m $^{-2}$ ·s $^{-1}$ , 12-hour light:12-hour dark photoperiod, and continuous aeration. These parameters ensured optimal growth conditions for *U. prolifera* (Huo et al., 2021; Bao et al., 2023; Glauco et al., 2024). The algae were cultured for 30 days prior to the experiment to ensure availability for experimental use.

#### 2.2 Experimental design

The inorganic nitrogen content in seawater of routinely cultured *U. prolifera* was measured daily until it reached zero (below the detection limit). No additional nitrogen nutrients were supplemented thereafter, and the algae were maintained under nitrogen starvation for 7 days before nitrogen uptake kinetics experiments.

Using artificial seawater without additional nitrogen sources as the baseline (NH<sub>4</sub><sup>+</sup>-N: 0.25  $\mu$ mol·L<sup>-1</sup>, NO<sub>3</sub><sup>-</sup>-N: 4.9  $\mu$ mol·L<sup>-1</sup>, NO<sub>2</sub><sup>-</sup>-N: 0.07  $\mu$ mol·L<sup>-1</sup>, PO<sub>4</sub><sup>3-</sup>-P: 0.02  $\mu$ mol·L<sup>-1</sup>), seawater with varying initial nitrogen concentrations was prepared by adding high-concentration NH<sub>4</sub>Cl, NaNO<sub>3</sub>, and NaNO<sub>2</sub> solutions. Both the artificial seawater and all nitrogen stock solutions (NH<sub>4</sub>Cl, NaNO<sub>3</sub>, and NaNO<sub>2</sub> prepared to target concentrations) were autoclaved to prevent microbial interference with nitrogen transformation processes. Three nitrogen species were tested at eight gradient concentrations:

NH<sub>4</sub><sup>+</sup>-N: 0.5, 5, 10, 15, 20, 25, 30, 35  $\mu$ mol·L<sup>-1</sup>; NO<sub>3</sub><sup>-</sup>-N: 5, 10, 20, 30, 60, 90, 110, 130  $\mu$ mol·L<sup>-1</sup>; NO<sub>2</sub><sup>-</sup>-N: 2.5, 5, 10, 15, 20, 30, 50, 60  $\mu$ mol·L<sup>-1</sup>.

Each concentration had three replicates, totaling 72 samples. Each sample contained 1 L of seawater and  $2.0 \pm 0.05$  g of nitrogenstarved *U. prolifera*, with other cultivation conditions consistent with prior protocols.

Water samples (5 mL) were collected at 0 h, 1 h, 2 h, 4 h, and 6 h after the experiment initiation. The removed volume was immediately replenished with artificial seawater to maintain a constant total volume. The concentrations of different nitrogen species in the seawater were measured at each time point. After the experiment, the *U. prolifera* was collected, dried at 60 °C to constant weight, and its dry weight was determined.

#### 2.3 Data and statistical analysis

The formulas for calculating the absorption rate (V), maximum absorption rate  $(V_{max})$ , and Michaelis constant  $(K_m)$  of U. proliferator inorganic nitrogen components are as follows:

$$V = \frac{(C_{t-1} - C_t) \cdot V_{t-1}}{t \cdot W} \tag{1}$$

Where V means absorption rate ( $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>),  $C_{t-1}$  and  $C_t$  means initial and final nutrient concentrations ( $\mu$ mol·L<sup>-1</sup>) during the sampling interval,  $V_{t-1}$  means initial culture volume (L) during the interval, t means time interval (h), and W means dry weight of algae (g).

Michaelis-Menten kinetics equation is as follows:

$$V = \frac{V_{\text{max}} \times C}{K_{\text{max}} + C} \tag{2}$$

Where V means absorption rate ( $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>),  $V_{max}$  means maximum absorption rate ( $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>),  $K_m$  means Michaelis constant ( $\mu$ mol·L<sup>-1</sup>), C means initial nutrient concentration ( $\mu$ mol·L<sup>-1</sup>) during the sampling interval.

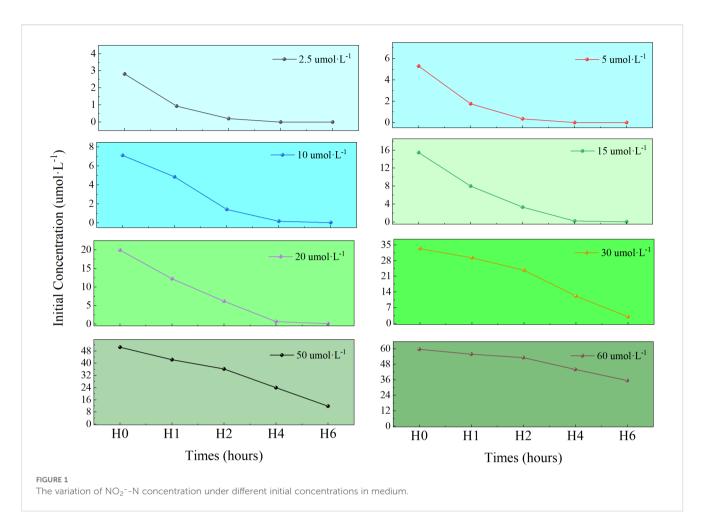
Experimental data were preprocessed using Excel, analyzed via one-way ANOVA and variance tests in SPSS 26.0 with a significance level of P< 0.05, and visualized using Origin 2022.

#### 3 Results

## 3.1 The influence of different initial concentrations on the adsorption of $NO_2^-$ -N by *U. prolifera*

Changes in NO $_2$ <sup>-</sup>-N concentration within the culture media across treatment groups are shown in Figure 1. *U. prolifera* exhibited significant absorption of NO $_2$ <sup>-</sup>-N. In low-concentration groups (2.5 and 5  $\mu$ mol·L<sup>-1</sup>), NO $_2$ <sup>-</sup>-N was completely depleted within 2 h. In contrast, high-concentration groups (30, 50, 60  $\mu$ mol·L<sup>-1</sup>) showed a gradual decline in NO $_2$ <sup>-</sup>-N concentration over time. After 6 h, the cumulative NO $_2$ <sup>-</sup>-N removal capacity ranked as follows: 50 > 30 > 60 > 20 > 15 > 10 > 5 > 2.5  $\mu$ mol·L<sup>-1</sup> groups. The highest total removal occurred in the 50  $\mu$ mol/L group (38.72  $\mu$ mol), followed by the 30  $\mu$ mol/L group (30.31  $\mu$ mol).

The  $NO_2^--N$  absorption rate per unit algal biomass (Calculated by Equation 1;  $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>) is presented in Figure 2. In 0–1 h, all groups reached peak absorption rates, indicating rapid initial uptake by nitrogen-starved *U. prolifera*. Absorption rates increased with initial concentration but were suppressed at concentrations >50  $\mu$ mol·L<sup>-1</sup> (Figure 2a). In 1–2 h, high-concentration groups (60  $\mu$ mol·L<sup>-1</sup>) continued to inhibit absorption rates (Figure 2b). Notably, during the initial absorption phase (1–2 h), the  $NO_2^--N$  uptake rates demonstrated sufficient normality across concentration gradients (2.5-60



μmol·L<sup>-1</sup>), validating their applicability for kinetic modeling via the Michaelis-Menten equation (Figure 2b). In 2–6 h, absorption rates dropped to 0 μmol·g<sup>-1</sup>·h<sup>-1</sup> in low-concentration groups (2.5-20 μmol·L<sup>-1</sup>) due to substrate depletion (Figures 2c, d). After 6 h, NO<sub>2</sub><sup>-</sup>-N removal efficiencies (%) for each initial concentration group (2.5-60 μmol·L<sup>-1</sup>) were: 99%, 100%, 99%, 99%, 99%, 91%, 77%, and 41%. These results demonstrate that NO<sub>2</sub><sup>-</sup>-N concentrations exceeding 50 μmol·L<sup>-1</sup> significantly suppress the absorption capacity of *U. prolifera*.

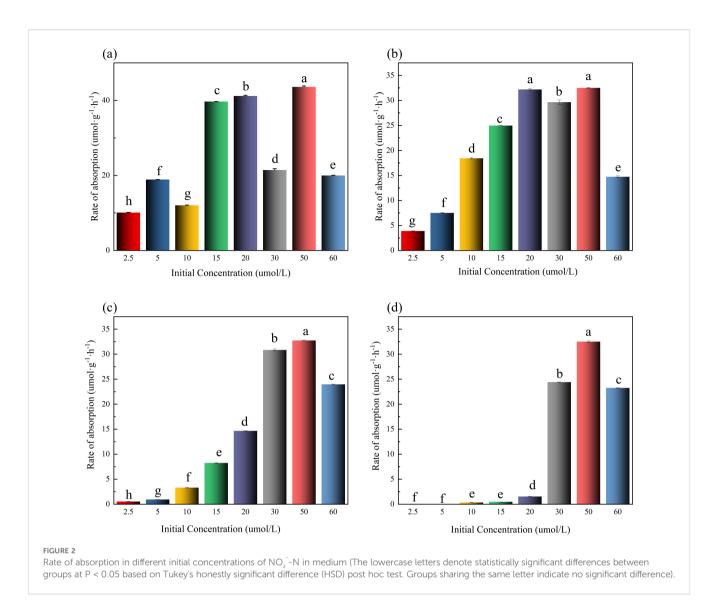
# 3.2 The influence of different initial concentrations on the adsorption of $NO_3^-$ -N by *U. prolifera*

Changes in NO<sub>3</sub><sup>-</sup>-N concentration within the culture media across treatment groups are shown in Figure 3. *U. prolifera* exhibited significant absorption capacity for nitrate nitrogen (NO<sub>3</sub><sup>-</sup>-N). In low-concentration groups (5-30  $\mu mol \cdot L^{-1}$ ), NO<sub>3</sub><sup>-</sup>-N was almost completely depleted within 1–2 h. High-concentration groups (110-130  $\mu mol \cdot L^{-1}$ ) showed gradual declines in NO<sub>3</sub><sup>-</sup>-N concentration over time. After 6 h, the cumulative NO<sub>3</sub><sup>-</sup>-N removal ranked as: 130 > 110 > 90 > 60 > 30 > 20 > 10 > 5  $\mu mol \cdot L^{-1}$  groups, with the highest total removal in the 130  $\mu mol \cdot L^{-1}$  group (100.25  $\mu mol$ ) followed by the 110  $\mu mol/L$  group (96.15  $\mu mol$ ).

Time-dependent absorption rates (μmol·g<sup>-1</sup>·h<sup>-1</sup>) are shown in Figure 4. In 0–1 h, all groups except 130 μmol·L<sup>-1</sup> reached peak absorption rates, and absorption suppression occurred in high-concentration groups (≥110 μμmol·L<sup>-1</sup>) (Figure 4a). In 2–4 and 4–6 h, rates dropped to 0 μmol·g<sup>-1</sup>·h<sup>-1</sup> in low-concentration groups (5-30 μmol·L<sup>-1</sup>) due to substrate exhaustion (Figures 4c, d). Final NO<sub>3</sub><sup>-</sup>-N removal efficiencies (%) per group (5-130 μmol·L<sup>-1</sup>) were: 31%, 100%,100%, 100%, 100%, 100%, 87% and 77%. It is worth noting that the NO<sub>3</sub><sup>-</sup>-N removal rate in the lowest concentration group (5 μmol·L<sup>-1</sup>) did not reach 100%, which indicates that in addition to the high concentration inhibition of NO<sub>3</sub><sup>-</sup>-N absorption by *U. prolifera*, there may also be a low concentration absorption threshold.

### 3.3 The influence of different initial concentrations on the adsorption of NH<sub>4</sub><sup>+</sup>-N by *U. prolifera*

Changes in NH<sub>4</sub><sup>+</sup>-N concentration within the culture media across treatment groups are shown in Figure 5. *U. prolifera* demonstrated significant assimilation capacity for ammonium nitrogen (NH<sub>4</sub><sup>+</sup>-N). In low concentration groups (0.5-15  $\mu$ mol·L<sup>-1</sup>), NH<sub>4</sub><sup>+</sup>-N was fully depleted within 2 h. High-concentration groups (20-35  $\mu$ mol·L<sup>-1</sup>) exhibited gradual concentration declines throughout the experiment. After 6 h, cumulative NH<sub>4</sub><sup>+</sup>-N removal



ranked per group (0.5-35  $\mu$ mol·L<sup>-1</sup>) as: 30 > 20 > 25 > 35 > 15 > 10 > 5 > 0.5  $\mu$ mol·L<sup>-1</sup> groups, with maximum removal in the 30  $\mu$ mol·L<sup>-1</sup> group (18.08  $\mu$ mol) followed by the 20  $\mu$ mol/L group (17.04  $\mu$ mol).

Figure 6 illustrates time-dependent  $\mathrm{NH_4}^+$ -N absorption kinetics in U. prolifera. In 0–1 h, all treatment groups exhibited peak absorption rates (Figure 6a), indicating rapid initial uptake of  $\mathrm{NH_4}^+$ -N by nitrogen-starved algae. In 1–2 h, high concentrations ( $\geq 15~\mu\mathrm{mol\cdot L^{-1}}$ ) suppressed absorption rates (Figure 6b). In 2–4 and 4–6 h, absorption dropped to 0  $\mu\mathrm{mol\cdot g^{-1}\cdot h^{-1}}$  in low-concentration groups (0.5-15  $\mu\mathrm{mol\cdot L^{-1}}$ ) due to substrate depletion (Figures 6c, d). After 6 h,  $\mathrm{NH_4}^+$ -N removal efficiencies were: 100%, 100%, 100%, 100%, 79%, 88% and 64%.

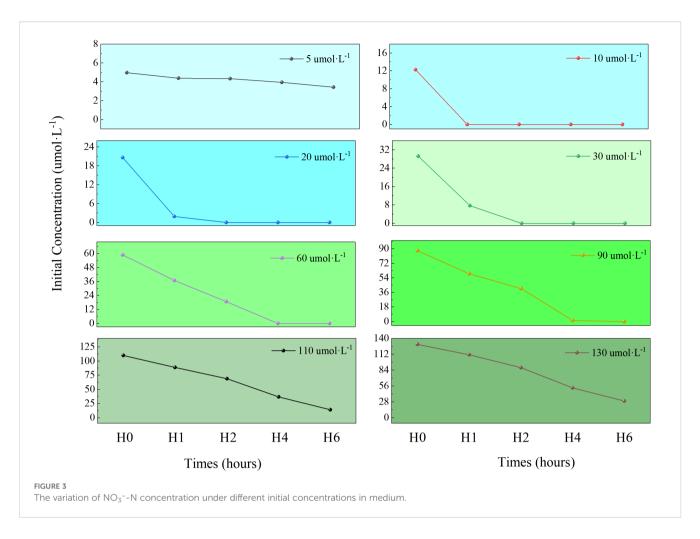
### 3.4 The absorption kinetics characteristics of *U. prolifera* under different nitrogen forms

The 1–2 h interval was selected for Michaelis-Menten modeling (Calculated by Equation 2 due to its strong linear correlation and

homogeneous data distribution across nitrogen species. Fitted kinetic parameters for  $NO_2^--N$ ,  $NO_3^--N$ , and  $NH_4^+-N$  assimilation are summarized in Table 1.

Kinetic analysis revealed distinct nitrogen assimilation patterns in *U. prolifera*: The maximum uptake velocity ( $V_{max}$ ) followed  $NO_3^-N$  (161.29  $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>) >  $NO_2^-N$  (39.06  $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>) >  $NH_4^+N$  (27.17  $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>), demonstrating superior nitrate removal capacity, while half-saturation constants ( $K_m$ ) exhibited  $NH_4^+N$  (4.60  $\mu$ mol·L<sup>-1</sup>) <  $NO_2^-N$  (8.31  $\mu$ mol·L<sup>-1</sup>) <  $NO_3^-N$  (29.40  $\mu$ mol·L<sup>-1</sup>), indicating highest transporter affinity for ammonium. This inverse relationship between  $V_{max}$  and  $K_m$  values elucidates a competitive assimilation priority: the minimal  $K_m$  for  $NH_4^+-N$  drives preferential uptake during multi-nitrogen coexposure, aligning with energy conservation strategies in algal metabolism where ammonium assimilation consumes less energy than nitrate assimilation.

 $\mathrm{NH_4}^+$ -N can be directly absorbed by algae and incorporated into amino acids such as glutamine, a process catalyzed by glutamine synthetase (GS) and glutamate synthase (GOGAT) (Guo et al., 2024). Because  $\mathrm{NH_4}^+$ -N is already in a reduced state, algae do not



need additional energy for reduction, making NH<sub>4</sub><sup>+</sup>-N assimilation the most energetically economical (Pereira and Cushman, 2019). NO<sub>3</sub><sup>-</sup>-N must first be reduced to nitrite by nitrate reductase (NR) and then to NH<sub>4</sub><sup>+</sup>-N by nitrite reductase (NiR) (Xu et al., 2024). Both reduction steps require energy input, usually provided in the form of NAD(P)H or reduced ferredoxin. Therefore, NO3-N assimilation requires more energy than NH<sub>4</sub><sup>+</sup>-N assimilation. NO<sub>2</sub><sup>-</sup>-N is an intermediate product in the reduction of NO<sub>3</sub>-N to NH<sub>4</sub>+-N. Therefore, algae absorbing NO2-N only require one reduction step (converting to NH<sub>4</sub><sup>+</sup>-N via NO<sub>2</sub><sup>-</sup>-N reductase), making it more efficient than NO<sub>3</sub>-N assimilation but still requiring more energy than directly absorbing NH<sub>4</sub><sup>+</sup>-N (Córdoba et al., 1986). Energy conservation strategies explain the differences among the three K<sub>m</sub> to some extent. The energy conservation strategy partially explains the differences in K<sub>m</sub> among the uptake of the three nitrogen forms.

# 3.5 The optimal applicable conditions for *U. prolifera* to absorb different forms of nitrogen

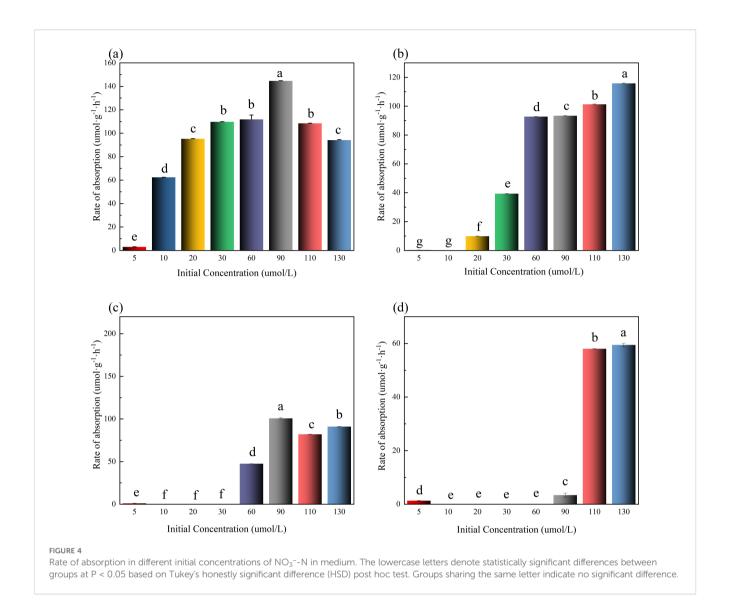
U. prolifera cannot sustain rapid nitrogen assimilation indefinitely as a biofilter, justifying our kinetic modeling focus on

the 1–2 h window where initial surge uptake reflects nitrogen starvation pretreatment while phase-II steady-state absorption aligns with practical operations. Nitrogen assimilation dynamics—modulated by temperature, pH, irradiance, salinity, phosphorus limitation, and initial N concentration—were evaluated under optimized conditions (24°C, 90 µmol photons·m²-s-¹, salinity 22 PSU), revealing two critical operational thresholds including non-inhibitory optimal concentrations (50 µmol·L¹ NO₂¹-N, 90 µmol·L¹ NO₃¹-N, 20 µmol·L¹ NH₄¹-N) and V<sub>max</sub>-sustaining concentrations derived from K<sub>m</sub> values (NO₂¹-N =8.3 µmol·L¹, NO₃¹-N =29.4 µmol·L¹, NH₄¹-N =4.6 µmol·L¹). For recirculating aquaculture systems experiencing dynamic nitrogen fluctuations, adaptive biomass deployment becomes essential requiring a 1.5-2× increase in *U. prolifera* biomass when total inorganic nitrogen exceeds 20 mg/L to sustain >90% removal efficiency.

#### 4 Discussion

### 4.1 The absorption kinetics characteristics of *U. prolifera* for different nitrogen forms

This study provides the systematic characterization of NH<sub>4</sub><sup>+</sup>-N, NO<sub>3</sub><sup>-</sup>-N, and NO<sub>2</sub><sup>-</sup>-N uptake kinetics in *U. prolifera* using

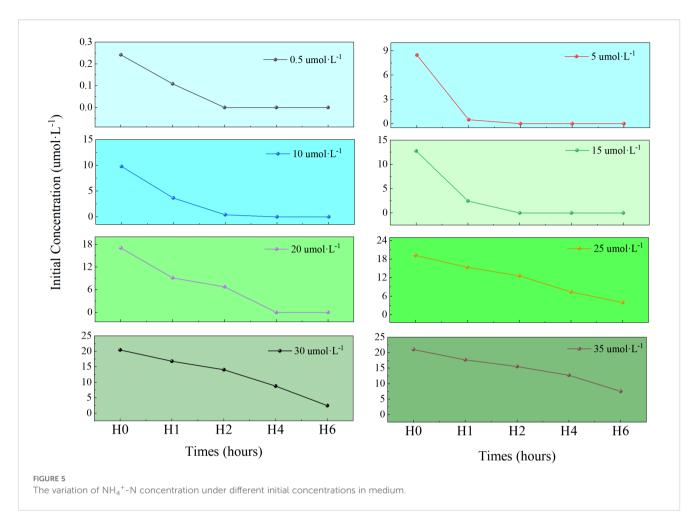


Michaelis-Menten modeling. The relationship between the N absorption rate of large seaweeds and the concentration of nutrients generally follows the deformation formula of the Michaelis-Menten equation:  $V=V_{max}\cdot C/(K_m+C)$ . *U. prolifera* as a species of large seaweed, also follows this rule (Luo et al., 2012; Zhang et al., 2019). The differential kinetic parameters reveal profound physiological adaptations of *U. prolifera* to environmental nitrogen regimes. *U. prolifera* exhibits robust uptake capacity for all three inorganic nitrogen forms. Notably, its maximum  $NO_3^--N$  absorption velocity reaches 161.29  $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>. This high  $NO_3^--N$  assimilation efficiency aligns with nitrate's dominance in natural marine environments, likely reflecting long-term evolutionary adaptation between coastal macroalgae and  $NO_3^--N$  dominated seawater.

 ${
m NH_4}^+$ -N exhibited the highest substrate affinity ( ${
m K_m}=4.60$   ${
m \mu mol \cdot L^{-1}}$ ,  ${
m R}^2=0.99$ ). This preference likely stems from the lower energy cost of  ${
m NH_4}^+$ -N assimilation compared to other nitrogen sources, as  ${
m NO_2}^-$ -N or  ${
m NO_3}^-$ -N are more oxidized forms of nitrogen that need to be reduced to  ${
m NH_4}^+$ -N (Abreu et al., 2011; Li et al., 2016; Ross et al., 2018).  ${
m NH_4}^+$ -N is commonly taken up through

passive diffusion. As nitrogen is presented in a reduced state that can be easily assimilated, the uptake rate rises in proportion to the substrate concentration. In contrast, NO<sub>3</sub>-N must first undergo reduction to NO<sub>2</sub>-N and then to NH<sub>4</sub>+N before algae can utilize this nitrogen source. This makes nitrogen uptake an energy dependent process (Fan et al., 2014). In practice, high substrate affinity enables sustained high absorption efficiency (100% removal within 6 h) at ammonium concentrations  $\leq 20 \, \mu \text{mol} \cdot \text{L}^{-1}$ . Notably, field measurements confirm that NH<sub>4</sub><sup>+</sup>-N levels in both the green tide origin site (Subei Shoal: about 10.79 μmol·L<sup>-1</sup>) and landing area (Qingdao coast: about 2.87 µmol·L<sup>-1</sup>) remain consistently<20 μmol·L<sup>-1</sup> (Wu et al., 2025b; Xiu et al., 2019). Consequently, U. prolifera experiences no NH4+-N inhibition during floating dispersal, as ambient concentrations remain below the suppression threshold identified in kinetic assays. This might also be one of the reasons for the rapid growth of *U. prolifera* biomass during the outbreak of the green tide.

 $NO_3$ <sup>-</sup>-N dominates the dissolved nitrogen pool in seawater, and the high uptake capacity of *U. prolifera* for  $NO_3$ <sup>-</sup>-N ( $V_{max}$ = 161.29  $\mu$ mol·g<sup>-1</sup>·h<sup>-1</sup>, R2=0.99) represents a significant ecological



adaptation. This confers competitive advantage in nutrient acquisition within complex nitrogen matrices. Evidence suggests  $NO_3^-$  may be the preferred nitrogen form for U. prolifera growth (Li et al., 2019), with uptake rates increasing proportionally to ambient nitrate concentrations (Zhang et al., 2021). According to the dual-compartment model established by Heimer and Filner (Heimer and Filner, 1971), nitrate is stored primarily in vacuoles (occupying  $\approx 90\%$  of cell volume), while metabolic nitrate resides in the cytoplasm. This explains the high absorption and enrichment capacity of  $NO_3^-$ -N by U. prolifera. In addition, U. prolifera still maintained a removal rate of 77% - 87% at a concentration of 90-110  $\mu$ mol·L<sup>-1</sup> (Figure 4), confirming its potential as a RAS biological filter.

NO<sub>2</sub><sup>-</sup>-N uptake kinetics exhibited a distinct unimodal curve: removal efficiency exceeded ≥99% at ≤20 μmol·L<sup>-1</sup> but plummeted to 41% at >50 μmol·L<sup>-1</sup> within 6 h (Figure 2). Although its  $K_m$  (8.31 μmol·L<sup>-1</sup>) was lower than that of NO<sub>3</sub><sup>-</sup>-N, the inhibition under elevated concentrations was more pronounced. For a long time, NO<sub>2</sub><sup>-</sup>-N has been ignored, although it is toxic to aquatic organisms. Interestingly, *U. prolifera* has a strong absorption capacity for NO<sub>2</sub><sup>-</sup>-N, which will effectively alleviate the toxicity caused by the accumulation of NO<sub>2</sub><sup>-</sup>-N in RAS.

The process of nitrogen within the cell mainly involves  $NO_3^--N$  accumulating in the vacuole and cytoplasm.  $NO_3^--N$  is reduced to  $NO_2^--N$  through nitrate reductase (NR). Then,  $NO_2^--N$  diffuses onto the cell membrane in a molecular form. Subsequently, under the action of nitrite reductase (NiR), it is converted into  $NH_4^+-N$ , serving as the substrate for amino acid synthesis (Zhang et al., 2021). Therefore, when the concentration of  $NO_2^--N$  is too high, the nitrite reduction process in the cell is inhibited, and the absorption of  $NO_2^--N$  by algae slows down. In summary, the kinetic characteristics of "low  $NH_4^+-N$  affinity - high  $NO_3^--N$  capacity -  $NO_2^--N$  sensitivity" of *Ulva* are the core of its green tide competitive advantage and provide a basis for nitrogen form regulation in RAS. That is, prioritizing the control of  $NH_4^+-N$  can alleviate the nitrification load, but the toxic threshold of  $NO_2^--N$  needs to be avoided.

### 4.2 The influence of initial concentration and time on absorption kinetics

Initial concentration gradient experiments have exposed *Ulva*'s nonlinear nitrogen uptake response. NH<sub>4</sub><sup>+</sup>-N uptake was

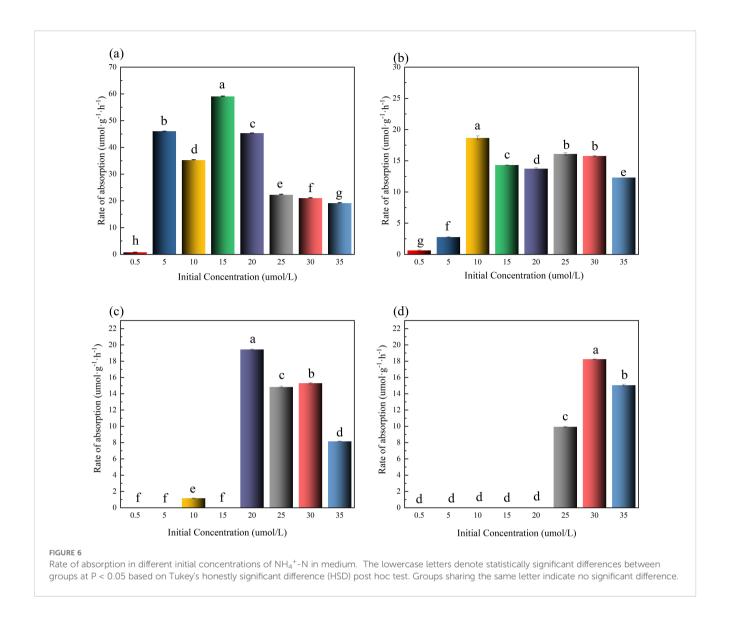


TABLE 1 Estimated kinetic parameters for NO2-N, NO3-N, NH4+-N uptaking.

Inorganic nitrogen form	Interval (h)	V <sub>max</sub> (μmol·g <sup>-1</sup> ·h <sup>-1</sup> )	K <sub>m</sub> (μmol·L <sup>-1</sup> )	R <sup>2</sup>
NO2 <sup>-</sup> -N	1-2h	39.06	8.31	0.95
NO3 <sup>-</sup> -N	1-2h	161.29	29.40	0.99
NH <sub>4</sub> <sup>+</sup> -N	1-2h	27.17	4.60	0.99

proportional to concentration from 0.5 to 20  $\mu$ mol·L<sup>-1</sup>, but the removal rate dropped 40%–60% when levels exceeded 20  $\mu$ mol·L<sup>-1</sup>. NO<sub>3</sub><sup>-</sup>-N uptake kept high absorption rate from 5 to 90  $\mu$ mol·L<sup>-1</sup>, yet was restrained once concentrations surpassed 110  $\mu$ mol·L<sup>-1</sup>. For NO<sub>2</sub><sup>-</sup>-N, remarkable inhibition occurred above 30  $\mu$ mol·L<sup>-1</sup>, with the 60  $\mu$ mol·L<sup>-1</sup> group achieving merely a 41% removal rate after 6 hours. This reflects *Ulva*'s varied response to different nitrogen concentrations and confirms the high ecological risk of elevated NO<sub>2</sub><sup>-</sup>-N levels.

The absorption process displayed a three phase evolution. During the rapid absorption phase (0–1 hour), nitrogen - starved transporters reacted swiftly, enabling all groups to reach peak absorption rates. In the steady - state phase (1–2 hours), absorption neared  $V_{\rm max}$  aligning with the Michaelis - Menten model, which made it the ideal window for kinetic modeling. During the attenuation phase (2–6 hours), low concentration groups (NO<sub>3</sub><sup>-</sup>-N  $\leq$ 15, NO<sub>3</sub><sup>-</sup>-N  $\leq$ 30, NO<sub>2</sub><sup>-</sup>-N  $\leq$ 20  $\mu$ mol·L $^{-1}$ ) plateaued due to substrate depletion, while high concentration groups were governed by inhibitory effects.

TABLE 2 Reference for the removal rate during the actual operation of RAS.

Biomass	Nitrogen form	Time interval	Velocity at different initial concentrations							
			2.5	5	10	15	20	30	50	60
1g	NO <sub>2</sub> -	0-1	10.08	18.87	12.02	39.69	41.17	21.42	43.61	19.98
		1-2	3.88	7.50	18.42	24.96	32.19	29.64	32.49	14.73
		2-4	0.53	0.93	3.31	8.24	14.65	30.84	32.74	23.95
		4-6	0.00	0.00	0.34	0.46	1.54	24.41	32.51	23.25
Final removal rate			99%	100%	99%	99%	99%	91%	77%	41%
1g	NO <sub>3</sub>		5	10	20	30	60	90	110	130
		0-1	2.99	62.38	95.21	109.71	111.76	144.61	108.43	94.10
		1-2	0.26	0.00	9.83	39.35	92.74	93.33	101.27	115.77
		2-4	0.98	0.00	0.00	0.00	47.44	100.71	81.99	90.95
		4-6	1.32	0.00	0.00	0.00	0.00	3.38	58.01	59.42
Final removal rate			31%	100%	100%	100%	100%	100%	87%	77%
1g	NH <sub>4</sub> <sup>+</sup>		0.5	5	10	15	20	25	30	35
		0-1	0.77	46.02	35.24	59.04	45.30	22.27	21.01	19.15
		1-2	0.62	2.76	18.66	14.30	13.73	16.09	15.76	12.31
		2-4	0.00	0.00	1.16	0.00	19.43	14.83	15.29	8.15
		4-6	0.00	0.00	0.00	0.00	0.00	9.93	18.25	15.05
Final removal rate			100%	100%	100%	100%	100%	79%	88%	64%

we consider the initial concentration at which a high removal efficiency is maintained (over 90% for 6 hours) as the upper limit of the concentration of the tail water from algae filtration. As show in Table 2, based on these findings, the following RAS application strategy is proposed: limiting NH<sub>4</sub><sup>+</sup>-N to  $\leq$ 20  $\mu$ mol·L<sup>-1</sup>, NO<sub>3</sub><sup>-</sup>-N to  $\leq$ 90  $\mu$ mol·L<sup>-1</sup>, and NO<sub>2</sub><sup>-</sup>-N to  $\leq$ 30  $\mu$ mol·L<sup>-1</sup> to prevent inhibition; boosting *Ulva* biomass by 1.5–2 times when TIN is high; and using pulsed feeding or continuous - flow reactors to avoid efficiency loss from algal nitrogen saturation.

#### 4.3 Limitations and future perspectives

The limitations of this study are as follows:  $PO_4^{\ 3-}$  -P was fixed at 0.02 µmol·L<sup>-1</sup> (Real seawater levels), so the impact of N:P ratio fluctuations on kinetics wasn't investigated; urea and other organic nitrogen, which account for 15% – 30% of aquaculture wastewater, weren't covered; and the single nitrogen source experiments failed to reflect the real environment with multiple coexisting nitrogen sources.

Future research should focus on the following aspects: integrating RAS nitrogen emission temporal data to build dynamic models; leveraging the high  $V_{max}$  characteristics of green - tide strains (e.g.,  $NO_3^-$ -N  $V_{max}=161.29~\mu mol\cdot g^{-1}\cdot h^{-1}$ ) and CRISPR technology to

enhance nitrogen transporter genes; developing a "negative - emission" RAS system that integrates *Ulva* carbon fixation with nitrogen removal; and using transcriptomics to analyze NO<sub>2</sub><sup>-</sup>-N inhibition mechanisms for designing resistant algal strains.

#### 5 Conclusion

The nitrogen uptake kinetics of U. prolifera constitute a fundamental mechanism underpinning both its ecological competitive advantage and bioremediation potential. This study quantified species-specific nitrogen uptake kinetics, revealing a physiological strategy characterized by: (i) optimal substrate affinity for  $NH_4^+$ -N ( $K_m = 4.60 \mu mol \cdot L^{-1}$ ), (ii) high uptake capacity for  $NO_3^-\text{--}N$  (V  $_{max}$  = 161.29  $\mu mol\cdot g^{-1}\cdot h^{-1}),$  and (iii) sensitive yet efficient  $NO_2$ -N absorption ( $V_{max} = 39.06 \mu mol \cdot g^{-1} \cdot h^{-1}$ ). Optimizing concentration thresholds and biomass allocation enables synergistic aquaculture wastewater denitrification and biomass valorization. Future research should prioritize elucidating multi-nitrogen interaction mechanisms and integrated process engineering. This dual functionality positions *U. prolifera* as a nature based solution for sustainable aquaculture, specifically contributing to SDG 6 (Clean Water) and SDG 14 (Life Below Water) through nitrogen bioremediation and biomass valorization in RAS.

#### Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material. Further inquiries can be directed to the corresponding authors or the first author.

#### **Author contributions**

WL: Investigation, Conceptualization, Resources, Writing – original draft. MZ: Investigation, Writing – original draft, Resources, Conceptualization. XX: Validation, Writing – original draft, Methodology. CH: Supervision, Funding acquisition, Writing – review & editing, Project administration. JL: Project administration, Writing – review & editing, Supervision, Funding acquisition. PH: Supervision, Writing – original draft, Writing – review & editing, Project administration, Funding acquisition.

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#### Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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#### Supplementary material

The Supplementary Material for this article can be found online at: https://www.frontiersin.org/articles/10.3389/fmars.2025. 1654677/full#supplementary-material

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