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Assembly of vermiculite/SnO₂ composite membranes with high ion selectivity for enhancing osmotic energy conversion performance

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For osmotic energy harvesting based on nanofluidic membranes, aqueous instability, less-than-optimal ion selectivity, and moderately high internal resistance can somewhat restrict its performance advancement. This study develops a novel composite membrane combining 2D SnO₂ and vermiculite (VMT) nanosheets to balance permeability and ion selectivity, boosting power density. The optimized membrane achieves an output power density of 0.727 W m⁻² using simulated saltwater/river water, offering a promising solution for efficient osmotic energy conversion.

KEYWORDS

osmotic energy, energy conversion, nanofluidic membranes, ion selectivity, vermiculite nanosheets, SnO₂ nanosheets

1 Introduction

Notwithstanding significant advancements in renewable energy technology over the past few decades, conventional fossil fuels remain the foundation of the energy sector (Rahman, 2023). To meet growing energy demands and mitigate environmental issues stemming from the imprudent utilization of fossil fuels, it is essential to cultivate renewable and clean energy sources (Achakulwisu et al., 2023; Xie et al., 2023; Vedhanarayanan and Seetha Lakshmi, 2024).

Osmotic energy, predominantly located near the confluence of rivers and the ocean, arises from the chemical potential gradient between freshwater and saltwater or between varying salinities of seawater (Mohammadi Amin and Krühne, 2024; Ramon et al., 2011; Laucirica et al., 2021). Owing to its ecological sustainability, low daily variations, and considerable reserves, it is regarded as a very promising renewable and clean energy source with tremendous development potential (Yip et al., 2016). Research estimates indicate that the global total of accessible osmotic energy is twice the yearly consumption of hydroelectric power output (Zhang et al., 2021). This research highlights the potential significance of osmotic energy as a renewable energy source and illustrates its considerable contribution to the future energy portfolio. Nanofluidic membranes, composed of thin-membrane materials with nanoscale channels or pores, offer significant benefits in osmotic energy conversion due to the distinctive ability of nanoscale channels to regulate ion transport (Tonnah et al., 2023; Xin et al., 2021; Tong et al., 2021). The design and development of high-performance nanofluidic membrane assemblies will promote the

efficient capture of osmotic energy and establish a foundation for its substitution of fossil fuels. Researchers have recently reported rapid permeation and highly selective transport in two-dimensional (2D) nanofluidic membranes, presenting novel avenues for the acquisition of osmotic energy. These events reveal significant potential for transcending the restrictions of conventional membrane technologies. 2D nanofluidic membranes are typically made up of many exfoliated nanosheet layers stacked on top of one another (Mei et al., 2024; Qin et al., 2022). Ion diffusion over the interlayer space happens vertically, and this process can be done at a tunable nanoscale with control spanning from a few nanometers to sub-nanometer scales (Zhang et al., 2019; Cheng et al., 2018; Abraham et al., 2017; Ling et al., 2014; Raidongia and Huang, 2012). In recent years, researchers have investigated the potential of 2D materials such as boron nitride (BN) (Pendse et al., 2021), molybdenum disulfide (MoS_2) (Zhu et al., 2021), graphene oxide (GO) (Ma et al., 2024), and MXene (Ding et al., 2020) for osmotic energy conversion applications. Based on these 2D materials, researchers have produced a number of unique 2D nanofluidic membrane designs. In contrast to conventional one-dimensional (1D) nanofluidic membranes, two-dimensional (2D) nanofluidic membranes are easier to fabricate and possess a broader reference range (Ji et al., 2017; Park and Jung, 2014; Feng et al., 2016).

Composite membranes based on two different 2D nanosheets have consistently exhibited a diverse array of uses in osmotic energy conversion (Wang et al., 2023). Due to their distinctive structure and elevated surface charge density, 2D nanosheets can significantly enhance ionic transport, enabling nanofluidic membranes to realize efficient osmotic energy conversion (Cheng et al., 2019). Nevertheless, the majority of 2D nanosheets are produced through the use of potent acids and oxidizers, which might elevate expenses and result in considerable environmental pollution throughout the fabrication process (Wang and Mi, 2017). Vermiculite (VMT) is an economical natural clay mineral with a worldwide production of around 500,000 t (Xia et al., 2022). VMT possesses a negative structural charge resulting from the substitution of $\text{Si}^{4+}/\text{Al}^{3+}$ with low-valent cations. It is defined by the adsorption of Mg^{2+} , K^+ , and other interlayer cations to preserve electroneutrality, which substantially influences its ion exchange capacity and interfacial properties (Wang and Mi, 2017). Prior studies have shown that bulk VMT may be effectively exfoliated in aqueous solutions, resulting in the production of 2D VMT nanosheets of nanoscale thickness by more environmentally benign and gentle ion exchange methods (Ja et al., 2018). VMT nanosheets (Wang et al., 2024), similar to GO nanosheets (Nde et al., 2024), possess a lamellar structure, rendering them suitable for the formation of nanochannels for osmotic energy conversion. In comparison to other 2D nanosheets, VMT nanosheets exhibit a reduced cost and a more environmentally sustainable preparation method. SnO_2 is a prototypical n-type semiconducting metal oxide predominantly utilized in the fabrication of lithium batteries and the advancement of hydrogen sensors (Villarreal et al., 2020; Bhardwaj et al., 2016). Researchers have successfully synthesized and extensively examined SnO_2 nanostructures with various morphologies, including nanoparticles, nanotubes, nanosheets, and layered nanostructures (Tonezzer, 2019). Among these numerous forms, 2D SnO_2 nanosheets, synthesized using the hydrothermal method (Li et al., 2020), have garnered significant interest and

scrutiny in recent years due to their remarkable properties, including a high specific surface area (Zhao et al., 2018) and a distinct exposed crystalline surface (Wang et al., 2013). Due to the presence of a negative charge on the surface and varied carrier mobility in SnO_2 nanosheets (Pu et al., 2022), they possess great potential for applications in osmotic energy conversion. Nonetheless, no research has employed SnO_2 nanosheets in the domain of osmotic energy conversion. The composite membrane composed of SnO_2 and VMT nanosheets is cost-effective and effectively balances permeation current and diffusion voltage, facilitating energy collection and conversion to electrical energy. The composite membrane possesses substantial scientific importance in osmotic energy conversion.

Herein, we report a novel composite membrane consisting of SnO_2 nanosheets and VMT nanosheets, characterized by increased ion selectivity, little internal resistance, and excellent aqueous stability. In testing conditions involving artificial river water and artificial saltwater, nanofluidic devices constructed from this composite membrane generated an output power density of 0.727 W m^{-2} . It is worth noting that the 50-fold NaCl concentration gradient employed here mimics the salinity difference between seawater and river water at natural estuaries, a critical target environment for osmotic energy harvesting. This configuration establishes a robust benchmark for evaluating the membrane's performance under realistic estuarine conditions, where NaCl constitutes the primary electrolyte. Meanwhile, this work provides significant insights and novel research concepts about osmotic energy conversion.

2 Materials and methods

2.1 Materials

Cetyltrimethylammonium bromide (CTAB) and sodium hydroxide (NaOH) were purchased from Titan Technology Discovery Platform; stannous chloride dihydrate ($\text{SnCl}_2 \cdot 2\text{H}_2\text{O}$) was purchased from Yatai United Chemical Co. Ltd. 2D VMT nanosheet dispersion (50 mg mL^{-1}) was purchased from Nano Functional Materials Co. Ltd.; and organic-based nylon microporous filter membranes were purchased from Derfiltration Technology. All chemicals, including sodium chloride (NaCl), potassium chloride (KCl), and lithium chloride (LiCl), were analytically pure.

2.2 Preparation of SnO_2 nanosheets

As depicted in Supplementary Figure S1a, 4.52 g of $\text{SnCl}_2 \cdot 2\text{H}_2\text{O}$, 1.28 g of CTAB, and 2.4 g of NaOH were introduced to 70 mL of deionized water, magnetically stirred for 1.5 h to ensure complete dissolution, and thereafter subjected to ultrasonic agitation for 1 h. The ultrasonicated solution was subsequently transferred to a 100 mL hydrothermal reactor, where it experienced a 12-h hydrothermal reaction at 180°C . The product was extracted and then rinsed multiple times with deionized water and anhydrous ethanol once it reached room temperature. Upon cooling the hydrothermal reactor to ambient temperature, the product

was extracted and subjected to numerous cross-washings with anhydrous ethanol and deionized water, respectively. The cleaned product was further annealed at 500 °C for 3 h at a rate of 5 °C min⁻¹ to yield SnO₂ nanosheets.

2.3 Preparation of VMT-X%SnO₂ composite membranes

As illustrated in [Supplementary Figure S1b](#), a dispersion of VMT nanosheets at a concentration of 5 mg mL⁻¹ was initially generated. Subsequently, 3 mL of VMT nanosheet dispersion was combined with 10%, 30%, and 40% of SnO₂ nanosheets, respectively. The two components were meticulously combined using continuous magnetic stirring for 8 h, followed by ultrasonication for 1 h. Following that, using vacuum filtration, the VMT nanosheet dispersion was amalgamated with 3 mL of VMT nanosheet dispersion. After ultrasound treatment, the VMT-10%SnO₂, VMT-30%SnO₂, and VMT-40%SnO₂ mixed dispersions were sequentially deposited via vacuum filtration onto the nylon microporous filter membrane of the organic system and then dried for 8 h at 60 °C, resulting in VMT-X%SnO₂ membranes, where X% indicates the mass percentage of SnO₂ nanosheets relative to VMT nanosheets in the membrane.

2.4 Characterization

Scanning electron microscopy (SEM, FEI Quanta 200FEG, Netherlands, and Zeiss Sigma 300, Germany) was used to examine the membranes' microstructure. A dynamic light scattering device (Brookhaven, NanoBrook Omni, United States) was used to test the dispersions' zeta potential at a concentration of 0.5 mg mL⁻¹. Using Cu K α irradiation and a scan rate of 5 min⁻¹, X-ray diffraction spectroscopy (XRD) was performed on a Rigaku D/MAX-2200PC X-ray diffractometer.

2.5 Electrochemical workstation testing

Using an electrochemical workstation (CS301M, Wuhan Kotai Instrument Co., Ltd.), the produced devices' ion transport characteristics and osmotic energy conversion ability were assessed and tested. Ag/AgCl electrodes were utilized for the testing unless otherwise noted. Schematically depicted in [Figure 2a](#), the test apparatus was composed of a composite membrane encased in epoxy resin. The composite membrane was inserted into the epoxy resin plate that separated the device's two chambers.

2.6 Measurement of power density

Current-voltage (*I-V*) curves, open-circuit voltage (V_{OC}), and short-circuit current (I_{SC}) were measured across a voltage range of -0.2 V–0.2 V at a 50-fold KCl concentration gradient (0.5 M for high concentration and 0.01 M for low concentration) to ascertain the maximum power density.

To determine the output power density, external resistors with diverse resistance values were applied to the current-time (*I-T*) curves at 50-fold concentration gradients of KCl, NaCl, and LiCl (0.5 M for high concentration and 0.01 M for low concentration). Throughout the scanning procedure, the voltage was established at 0 V.

2.7 Ion selectivity test

The *I-V* curves documenting salinity gradients of 10, 50, 100, 500, and 1,000 times were evaluated to determine ion selectivity utilizing Ag/AgCl electrodes with saturated salt bridges within a voltage measurement range of -0.2–0.2 V and a scan rate range of 10 mV s⁻¹.

2.8 Conductivity test

The conductivity of KCl solutions, ranging from 10⁻⁶ M–1 M without a concentration gradient, was assessed by scanning the *I-V* curves at a rate of 10 mV s⁻¹ across a voltage range of -0.2–0.2 V.

2.9 Ion transport stability test

Using a 0.1 M KCl solution in both chambers, external bias voltages of +1 V and -1 V were sequentially applied to the device, and the *I-T* curves were recorded every 3,000 s in a cycle to assess the ion transfer stability of the device.

3 Results and discussions

3.1 Microanalysis of nanosheets and composite membranes

[Figure 1](#) shows the microscopic characterization of VMT nanosheets, SnO₂ nanosheets and VMT-X%SnO₂ composite membranes. VMT nanosheets and SnO₂ nanosheets were initially analyzed microscopically. As shown in TEM images ([Figures 1a,b](#)), the VMT and SnO₂ nanosheets exhibit a distinct lamellar structure at the nanometer scale, with the diameters of the VMT nanosheets surpassing those of the SnO₂ nanosheets. The zeta potentials of the VMT and SnO₂ nanosheets are -27.47 mV and -23.45 mV, respectively ([Figure 1c](#)). The higher zeta potential of VMT (-27.47 mV) establishes a robust electrostatic driving force for cation attraction and anion repulsion, while the moderate zeta potential of SnO₂ (-23.45 mV) prevents excessive local charge accumulation that might otherwise impede cation transport through overcrowding. This balance prevents "charge saturation" in nanochannels, ensuring efficient cation migration while maintaining anion exclusion. Subsequently, we can calculate the surface charge density of VMT nanosheets and SnO₂ nanosheets by the value of zeta potential as -2.12 mC m⁻² and -1.81 mC m⁻², respectively ([Supporting Note1](#)). Thereafter, we microscopically analyzed the VMT-X%SnO₂ composite membrane. The XRD spectra ([Figure 1d](#)) indicate that the VMT-30%SnO₂ composite

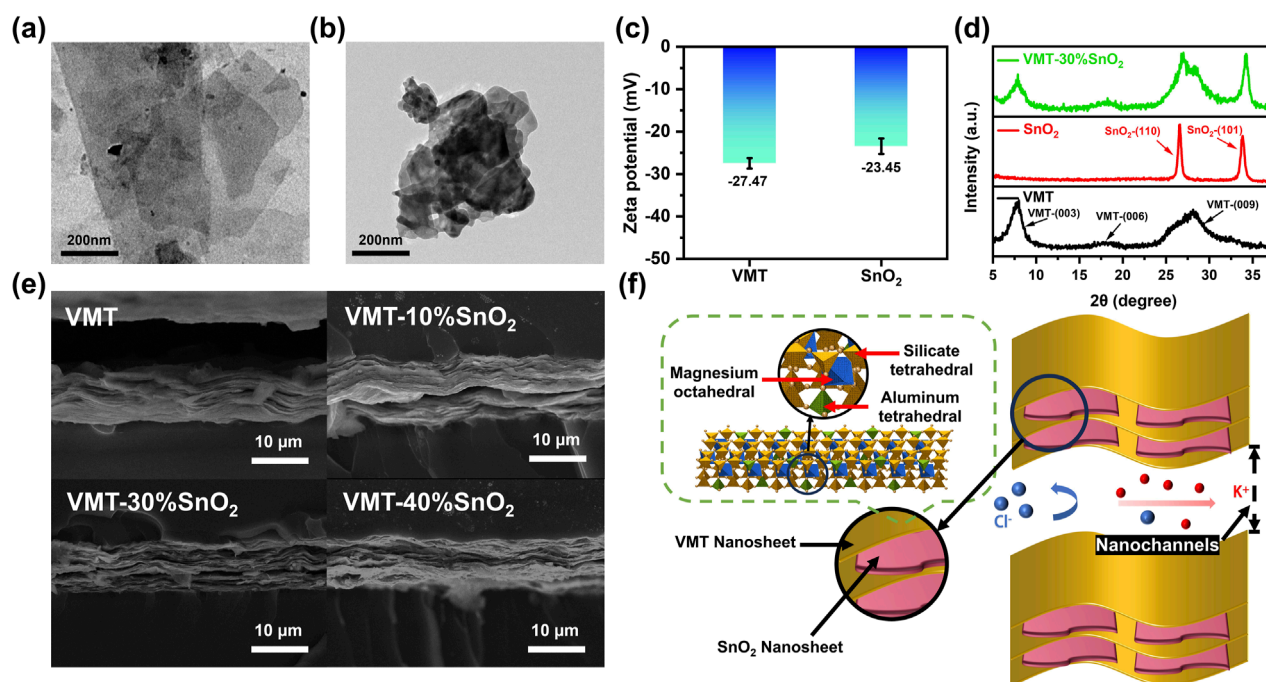


FIGURE 1 Characterization of VMT nanosheets, SnO_2 nanosheets and VMT-X% SnO_2 composite membranes. TEM images of (a) VMT nanosheets and (b) SnO_2 nanosheets. (c) Zeta potential values of VMT nanosheets and SnO_2 nanosheets. (d) XRD spectra of VMT-30% SnO_2 composite membrane. (e) Cross-sectional SEM images of VMT membranes and VMT-X% SnO_2 composite membranes. (f) Schematic diagram of VMT-X% SnO_2 composite membrane nano-channels.

membrane preserves the (003) and (009) crystalline absorption peaks characteristic of VMT nanosheets (Zhang et al., 2023) and also exhibits the (110) and (101) crystalline absorption peaks related to SnO_2 nanosheets (Chen et al., 2014). The aforementioned phenomenon demonstrated that the VMT-X% SnO_2 composite membrane preserved the original lattice structure of both VMT and SnO_2 nanosheets. Analysis of the cross-sectional SEM images of the VMT membrane and the VMT-X% SnO_2 composite membrane (Figure 1e) reveals that both exhibit a somewhat regular laminar structure, with components organized in close proximity. This structure creates favorable conditions for the development of nano-channels, as well as nanofluidic ion transport (Zhang et al., 2022). The nanochannel dimensions of VMT-X% SnO_2 composite membranes exhibit a non-monotonic variation with increasing SnO_2 nanosheet additive ratio, demonstrating initial expansion followed by subsequent contraction. The VMT-X% SnO_2 composite membranes exhibit a relatively uniform laminar structure, as illustrated in Figure 1f, facilitating the development of nano-channels. The SnO_2 nanosheets are deposited and adhere to the planar framework formed by VMT nanosheets. This structure comprises aluminum tetrahedra, silicate tetrahedra, and magnesium octahedra in an orderly arrangement (Wang et al., 2024). Multiple nano-channels for ion transport were established between the SnO_2 nanosheets and the VMT nanosheets. In these nano-channels, the surface charges of the walls attract counterions of opposite charge, resulting in the formation of electric double layer (EDL) structures. When the channel dimensions are comparable to the Debye length, the electric double layers, comprising the Stern and diffusion

layers, overlap within the channel (Supplementary Figure S2). In this situation, ions with identical surface charges within the channel experience repulsion, whereas counterions can traverse the channel (Chang et al., 2022).

3.2 Relationship between power density and additive ratio

The ion transport properties and osmotic energy conversion performance of the fabricated devices were assessed using an electrochemical workstation (CS301M, Wuhan Kotai Instrument Co., Ltd.). Unless stated otherwise, Ag/AgCl electrodes were employed for all experiments in this investigation. As illustrated in Supplementary Figure S3, the test device was constructed from a composite membrane encased in epoxy resin. The device comprises two chambers: the left chamber contains a low concentration salt solution, while the right chamber contains a high concentration salt solution. The composite membrane is situated within an epoxy resin plate utilized to partition the two chambers. Significantly, given that the test area of the VMT-X% SnO_2 composite membranes with varying additive ratios was 0.03 mm^2 (Figure 1d), and then enclosed them in devices using epoxy resin for further testing.

In the absence of an external electric field, ions diffuse spontaneously from regions of high concentration to low concentration due to the concentration gradient (Mohammadi Amin and Krühne, 2024). The VMT-X% SnO_2 composite membrane possesses a negative surface charge, and its

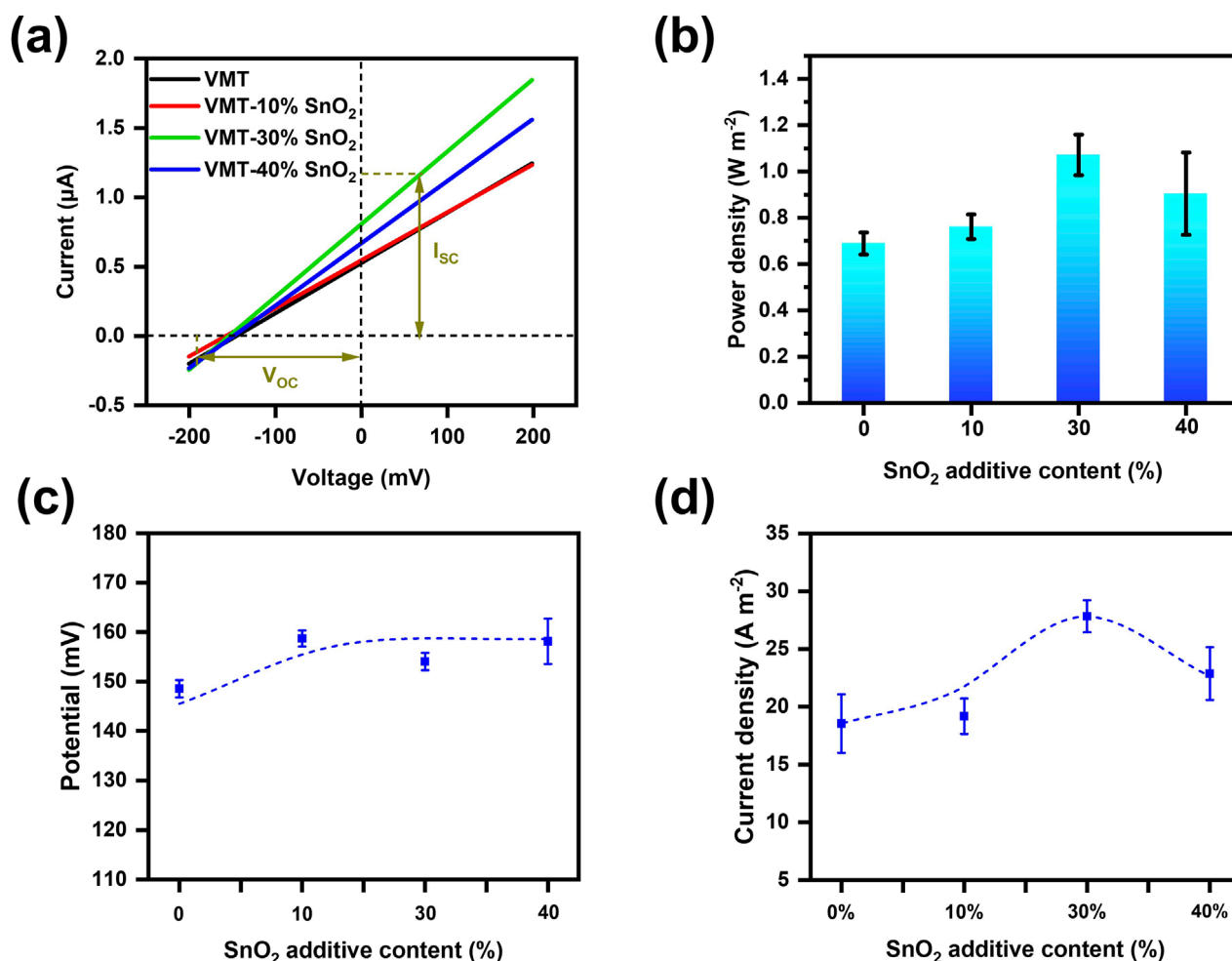


FIGURE 2
Study on the relationship between power density and additive ratio of VMT-X%SnO₂ composite membranes. (a) *I-V* curves, (b) power density comparison, (c) V_{OC} and (d) current density of VMT-X%SnO₂ composite membranes with different additive ratios under 50-fold KCl concentration gradient.

internal nano-channels preferentially allow the passage of cations while repelling anions. The differential ion migration behavior, influenced by the nanolimited domain effect and the material's surface chemistry, results in cation-preferential transport, leading to charge separation and a net current across both sides of the membrane (Feng et al., 2016). Initially, we should ascertain the optimal additive ratio for the composite membrane. An aqueous KCl solution has been introduced into the chambers on both sides of the device as an electrolyte salt solution. The membrane-forming properties of the VMT-X%SnO₂ composite membrane deteriorate as the mass percentage of added SnO₂ nanosheets increases. The composite membrane becomes brittle and hence challenging to test when the additive ratio of SnO₂ nanosheets exceeds 40%. Consequently, the additive ratio of SnO₂ nanosheets incorporated is limited to 40% or below. The values of V_{OC} and I_{SC} are derived by analyzing the *I-V* curves of VMT-X%SnO₂ composite membranes with differing additive ratios under a 50-fold KCl concentration gradient (high concentration of 0.5 M, low concentration of 0.01 M) across a voltage range of -0.2 – 0.2 V, as illustrated in Figure 2a. Supplementary Equation S3 can be

employed to ascertain the power densities of the VMT-X%SnO₂ composite membranes with differing additive ratios under a 50-fold KCl concentration gradient subsequent to the deduction of the redox potential (Figure 2b). As the additive ratio of SnO₂ nanosheets increases, the power density initially ascends and thereafter declines. The power density reaches its maximum at a 30% additive ratio of SnO₂ nanosheets (1.07 W m^{-2}), representing a 55.3% improvement over the power density of pure VMT membrane (0.69 W m^{-2}). As the additive ratio of SnO₂ nanosheets grew, V_{OC} also exhibited an upward trend (Figure 2c). Nonetheless, as the additive ratio of SnO₂ nanosheets grew, the current density initially ascended and then declined. It reached a maximum additive ratio of 30%, surpassing that of the pure VMT membrane, consequently enhancing the power density (Figure 2d). The observed trend can be attributed to the following mechanism: Initially, with increasing additive ratio of SnO₂ nanosheet, the interlayer spacing of nanochannels expands, thereby facilitating enhanced cation transport through the nanochannels and consequently leading to increased current density. However, when the additive ratio reaches a critical threshold, SnO₂ nanosheet begin to aggregate

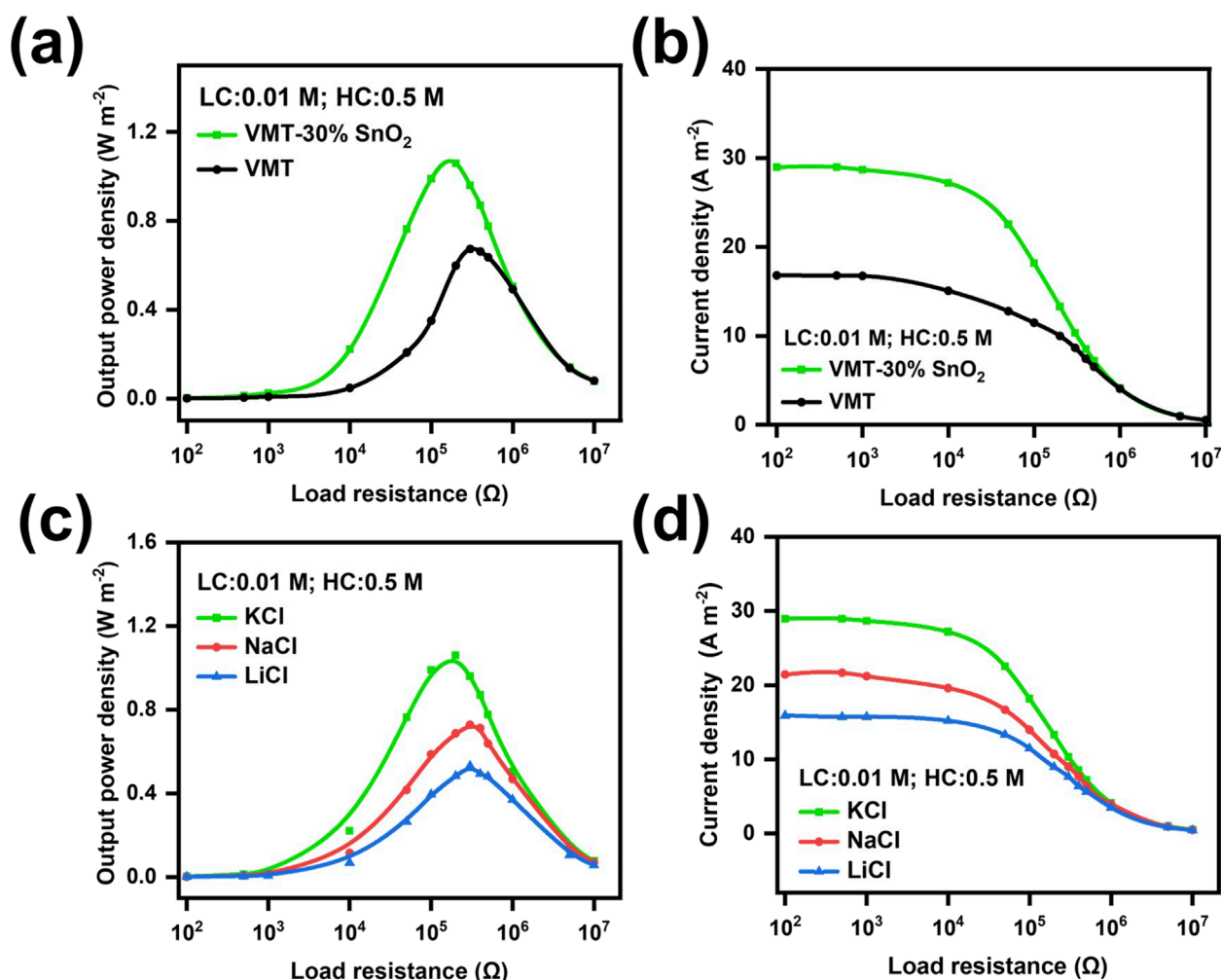


FIGURE 3 Output power density test of VMT-X%SnO₂ composite membrane. Comparison of (a) output power density and (b) output current density of VMT composite membrane as well as VMT-30%SnO₂ composite membrane under 50 times KCl concentration gradient (0.01 M/0.5 M) in the selected load range. (c) Output power density and (d) Output current density of VMT-30%SnO₂ composite membrane under 50-fold concentration gradient (0.01 M/0.5 M) of different electrolytes in the selected loading range.

within the nanochannels. This aggregation can lead to the blockage of the nanochannels, resulting in a decrease in effective nanochannels and a reduction in cation flux. Consequently, the current density shows a downward trend. The VMT-30%SnO₂ composite membranes was chosen for further testing, as the optimal power density was attained with a 30% additive ratio of SnO₂ nanosheets.

3.3 Output power density test

Nanofluidic membranes can provide electrical energy to externally powered devices. (Wang et al., 2021). [Supplementary Equation S4](#) can be utilized to ascertain the output power densities of the VMT membrane and the VMT-30%SnO₂ composite membrane. At a 50-fold KCl concentration gradient (0.01 M/0.5 M), the output power density of the VMT-30%SnO₂ composite membrane was 1.059 W m⁻², surpassing that of the VMT membrane (Figure 3a). This can be attributed to the superior

output current density of the VMT-30% SnO₂ composite membrane compared to the VMT membrane (Figure 3b). However, the output power density of the VMT membrane and the VMT-30%SnO₂ composite membrane reached their peak values under different external resistance values. The reason for this phenomenon can be attributed to the fact that the internal resistance of the VMT-30%SnO₂ composite membrane is lower than that of the VMT membrane. Subsequently, we evaluated the output power density of the VMT-30%SnO₂ composite membrane using various electrolytes. The output power density was 0.727 W m⁻² with NaCl as the electrolyte and 0.531 W m⁻² with LiCl, both under a 50-fold electrolyte concentration gradient (0.01 M/0.5 M) (Figure 3c). The addition of KCl, NaCl, and LiCl as electrolytes resulted in output current densities of 28.9 A m⁻², 21.4 A m⁻², and 15.9 A m⁻², respectively, while sustaining a 50-fold electrolyte concentration gradient (0.01 M/0.5 M) (Figure 3d). The 50-fold NaCl concentration gradient (0.01 M/0.5 M) can be regarded as representative of the concentration gradient between artificial river water and artificial seawater. This discrepancy arises from variations

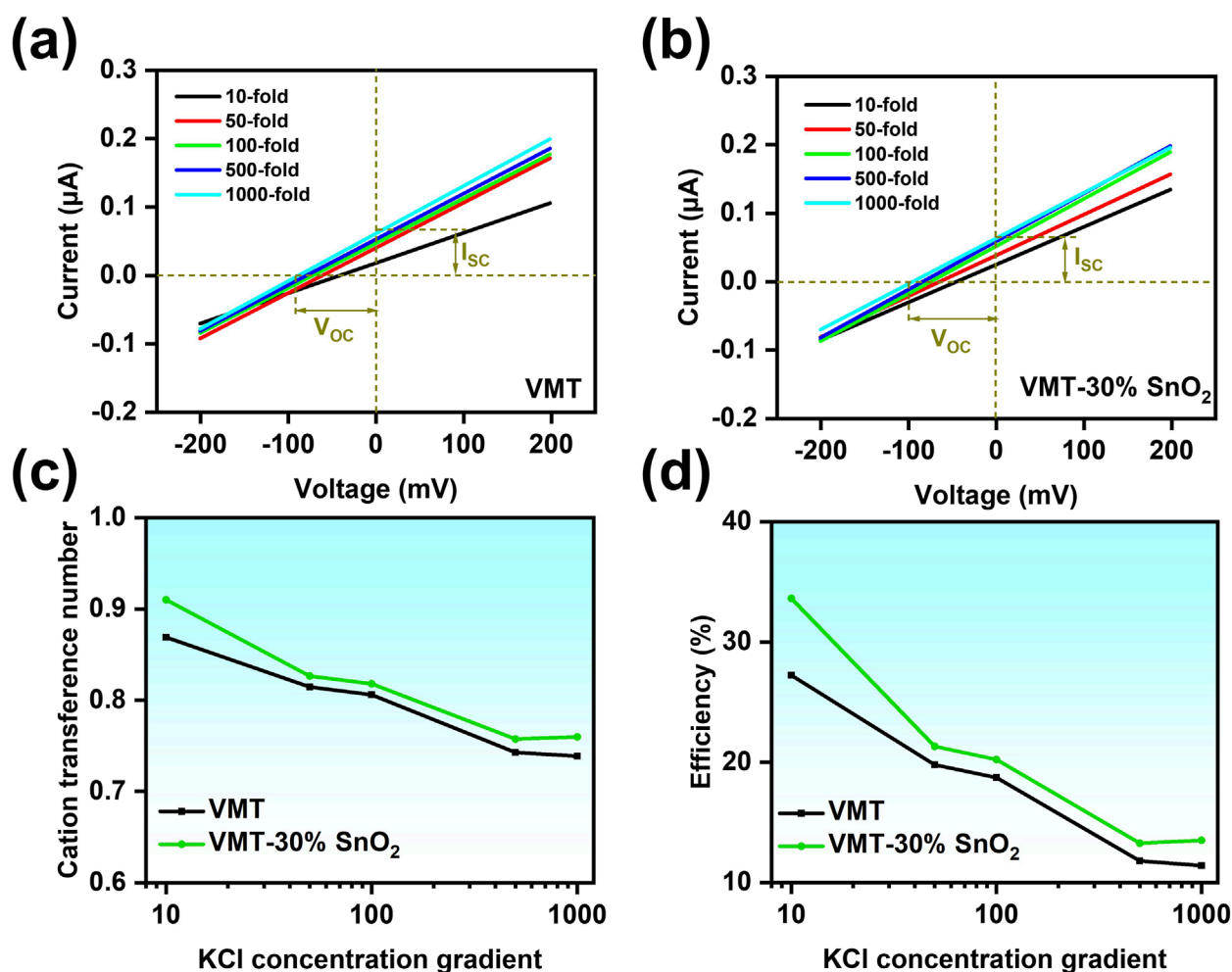


FIGURE 4
Transmembrane ion transport in VMT-30%SnO₂ composite membranes. I-V curves of (a) VMT-30%SnO₂ composite membrane and (b) VMT membrane in different concentration gradients of KCl solution. (c) Cation transfer number (t_+) and (d) energy conversion efficiency plots of VMT-30%SnO₂ composite membrane and VMT membrane at different KCl solution concentration gradients.

in the cation diffusion coefficients of the electrolytes. The hierarchy of cation diffusion coefficients for the three selected electrolytes is $K^+ > Na^+ > Li^+$. Elevated cation diffusion coefficients yield increased output current densities, thereby enhancing output power densities (Wu et al., 2020).

3.4 Transmembrane ion transport performance testing

Upon establishing the optimal additive ratio of the composite membrane, we utilized Ag/AgCl electrodes with saturated salt bridges to further examine the transmembrane ion transport performance. Maintaining the concentration of the low side KCl solution at a constant 10^{-3} M, the I-V curves of the VMT-30%SnO₂ composite membrane and the VMT membrane were examined over various KCl solution concentration gradients within the voltage range of -0.2 V– 0.2 V (Figures 4a,b). Consequently, the V_{OC} values of VMT-30%SnO₂ composite membrane and

VMT composite membrane were derived from the I-V curves at varying concentration gradients of KCl solutions, respectively. The absolute values of V_{OC} for the VMT-30%SnO₂ composite membrane and VMT membrane escalated with the concentration gradient. The V_{OC} of the VMT-30%SnO₂ composite membrane was approximately -50 mV at a concentration gradient of 10 times, and around -98 mV when the gradient increased to 1,000 times. Furthermore, the absolute values of the V_{OC} for the VMT membrane at varying concentration gradients were lower than those of the VMT-30%SnO₂ composite membrane, corroborating previous test results (Supplementary Figures S4a,b). Cation transfer number (t_+) and energy conversion efficiency are critical metrics for assessing the ion-selective performance of the devices (Ji et al., 2017; Zhou and Jiang, 2020). When the value of t_+ equals 1, it signifies that the composite membrane exhibits complete cation selectivity. The t_+ values of the VMT-30%SnO₂ composite and VMT membranes can be ascertained using Supplementary Equation S5. The maximum value of t_+ for the VMT-30%SnO₂ device is 0.910, surpassing the maximum value of t_+ for the VMT device, which is 0.869. The

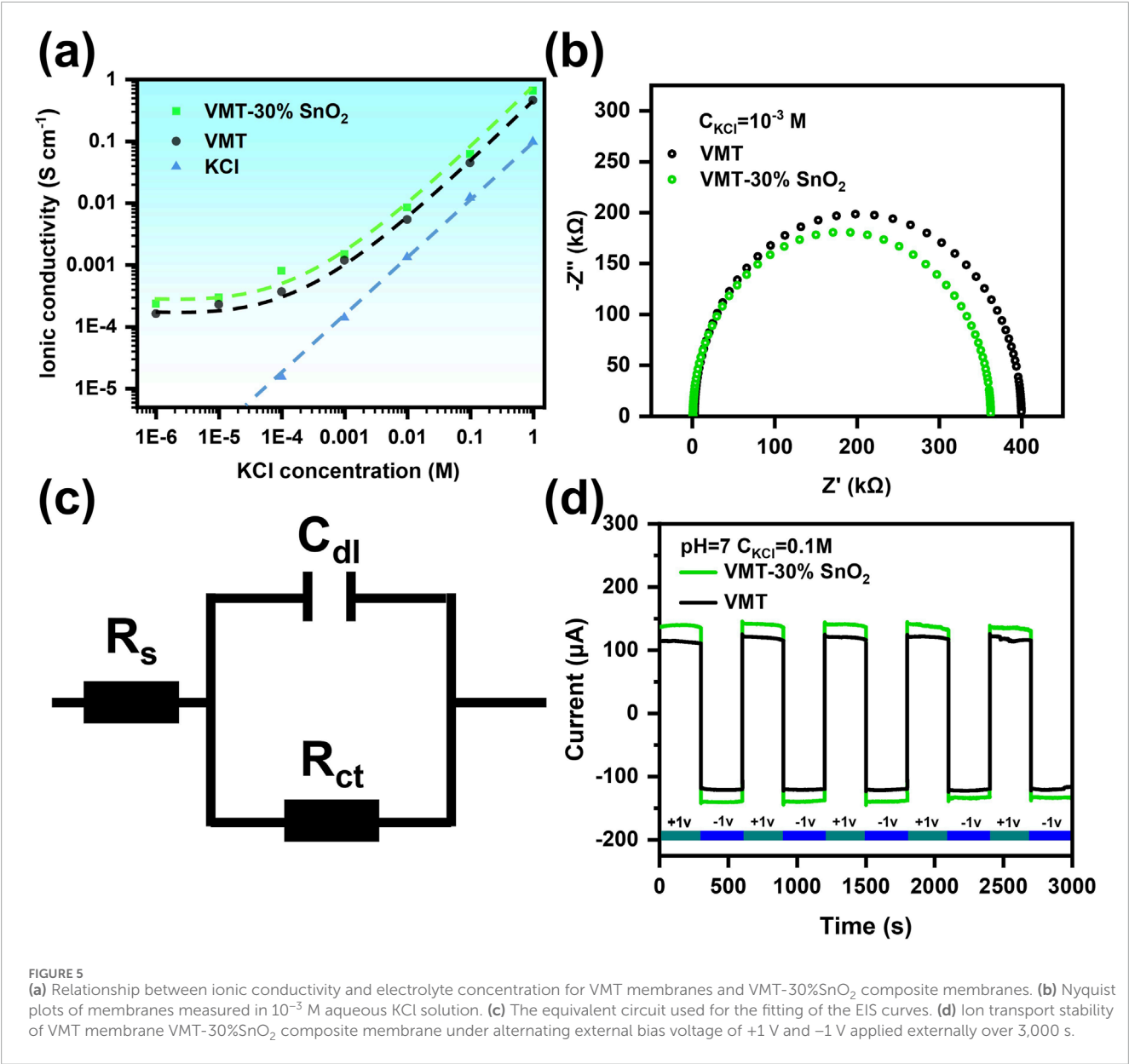


TABLE 1 Computations subsequent to curve fitting for EIS equivalent circuits.

Sample	$R_s(\Omega)$	$R_{ct}(\Omega)$	$C_{dl}(F)$
VMT	2,471.7	3.971×10^5	8.744×10^{-10}
30% SnO ₂	587.06	3.618×10^5	7.074×10^{-10}

forementioned conclusion demonstrates that the ion selectivity of the composite membrane improved with the incorporation of SnO₂ nanosheets, while VMT-30%SnO₂ exhibited commendable cation selectivity. As the KCl concentration gradient intensifies, the t_+ values exhibit a declining trend, attributable to the reduction in the Debye length and concentration polarization at elevated

concentrations (Figure 4c). The energy conversion efficiencies of the VMT-30%SnO₂ composite membrane and VMT membrane can be obtained from Supplementary Equation S6. The energy conversion efficiency of the VMT-30%SnO₂ composite membrane (33.63%) surpasses that of the VMT membrane (27.23%), and the efficiency diminishes with an increasing concentration gradient (Figure 4d).

3.5 Conductivity test

The ion transport characteristics of VMT-30%SnO₂ composite membrane and VMT membrane were further examined by assessing their conductivity. During the conductivity test, the concentration of KCl solution in the chambers on either side of the testing apparatus had to be uniform. The precise value of the nano-channel conductivity was ascertained using Supplementary Equation S7.

As the concentration of KCl solution increased, conductivity rose, and the conductivity of the VMT-30%SnO₂ composite membrane surpassed that of the VMT membrane (Figure 5a). This phenomenon can be mechanistically ascribed to the expansion of interlayer spacing in nanochannels induced by the introduction of SnO₂ nanosheets. Such structural evolution effectively mitigates the steric hindrance during ion transport, thereby facilitating the permeation kinetics of ions through the nanochannel network. The conductance (S), as indicated by Supplementary Equations S7, 8, was predominantly influenced by the surface charge density at low electrolyte solution concentrations. Consequently, when the concentration of the KCl solution was in the low concentration range (below 10⁻³ M) the conductivity tended to stabilize on a logarithmic scale. The phenomenon was typical of nanofluidic ion transport behavior. The S of KCl solutions in the high concentration range (higher than 10⁻³ M) was predominantly influenced by the S of the aqueous KCl solution at varying concentrations. Therefore, the conductance trend in this region, when represented on a logarithmic scale, aligned with the linear variation of the intrinsic conductance of KCl.

Simultaneously, we acquired the Nyquist plots of the VMT membrane compared to the VMT-30%SnO₂ membrane by measuring with a KCl solution concentration of 10⁻³ M on both sides of the chamber (Figure 5b). We subsequently fitted the Nyquist curves using an EIS equivalent circuit (Figure 5c) to get the internal resistance values of the VMT membrane and the VMT-30%SnO₂ composite membrane (Table 1). The charge transfer resistance (R_{ct}) of the VMT-30% SnO₂ composite membrane was around 361.8 k Ω , marginally lower than the R_{ct} of the VMT membrane at 397.1 k Ω . SnO₂ nanosheets reduce R_{ct} through synergistic surface charge effects and optimized channel structures, minimizing energy loss and improving ion transport efficiency. The comparatively lower internal resistance was advantageous for output power density, resulting in the VMT-30%SnO₂ composite membrane exhibiting a greater output power density than the VMT membrane.

Ultimately, we assessed the ion transport stability of the composite membranes over 3,000 s by alternately applying +1 V and -1 V external bias voltages outside the testing apparatus. As illustrated in Figure 5d, both the VMT membrane and the VMT-30%SnO₂ composite membrane exhibited minimal fluctuations throughout the 3,000 s, indicating that they both demonstrated relatively robust ion transport stability.

4 Conclusion

In summary, this work demonstrated the preparation of VMT/SnO₂ nanofluidic membranes and their application in osmotic energy conversion. The composite membrane effectively balanced permeability and ion selectivity due to the synergistic effect of two negatively charged surface nanosheets, resulting in enhanced performance for osmotic energy conversion. The composite membrane's output power density attained 0.727 W m⁻² at a 50-fold NaCl concentration gradient (artificial seawater versus river water). This study provides a novel approach for osmotic energy conversion and energy sustainability, and offers a theoretical basis for the application of VMT/SnO₂ nanofluidic membranes in real-life scenarios.

Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material, further inquiries can be directed to the corresponding authors.

Author contributions

YF: Funding acquisition, Conceptualization, Project administration, Formal Analysis, Writing – review and editing, Data curation, Methodology, Writing – original draft, Resources, Investigation. ZC: Visualization, Methodology, Data curation, Validation, Investigation, Conceptualization, Writing – review and editing. YZ: Visualization, Validation, Investigation, Methodology, Writing – review and editing, Conceptualization. BX: Writing – review and editing, Investigation, Conceptualization, Methodology, Resources, Project administration, Visualization.

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Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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Supplementary material

The Supplementary Material for this article can be found online at: <https://www.frontiersin.org/articles/10.3389/fmats.2025.1648638/full#supplementary-material>

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